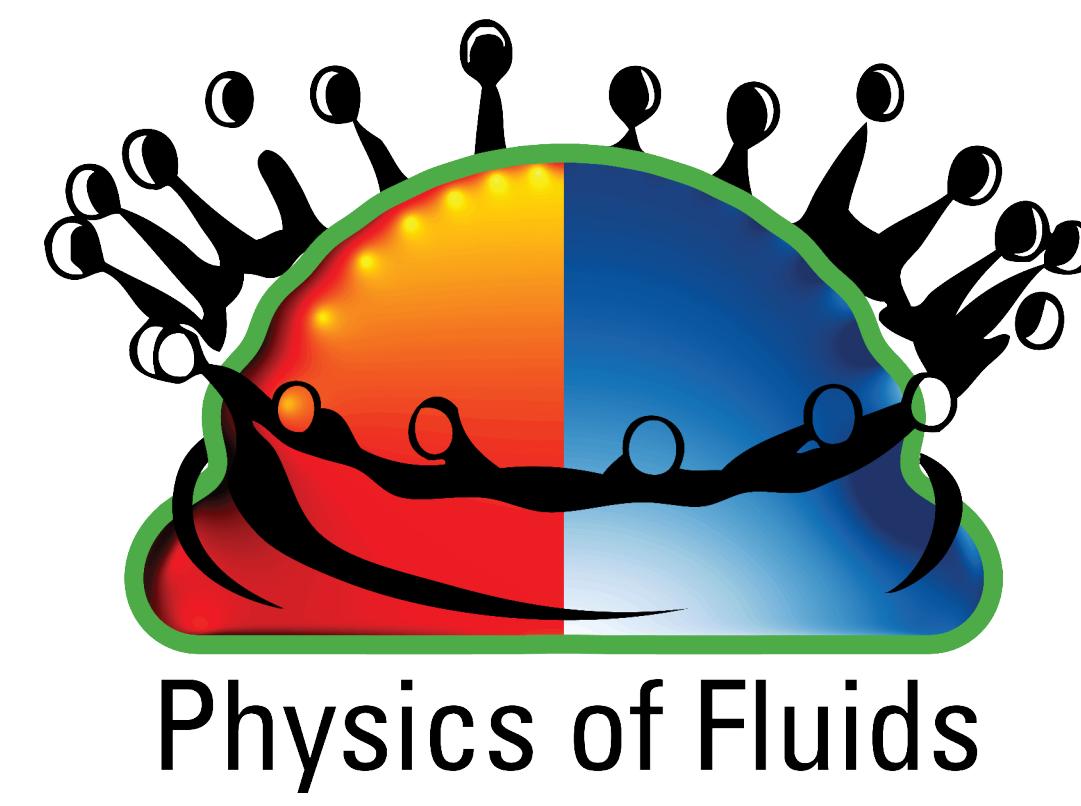


Viscous Free-Surface Flows

Vatsal Sanjay



European Research Council
Established by the European Commission



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Link: <https://youtu.be/3FZPkWxprDM>

Collaborators & Acknowledgements

- **Detlef Lohse**
- Pierre Chantelot (Institut Langevin)
- Mazi Jalaal (UvA, Amsterdam)
- **Uddalok Sen (WUR, Wageningen)**
- **Jacco Snoeijer**
- **Cunjing Lv (Tsinghua Univ.)**
- **Alexandros Oratis**
- **Vincent Bertin**
- Youssef Saade (Canon)*
- Mandeep Saini*
- **Pallav Kant (Univ. of Cambridge)**
- Jonathan Pham (Univ. of Kentucky)
- Doris Vollmer (MPI-Mainz)

Canon

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European Research Council

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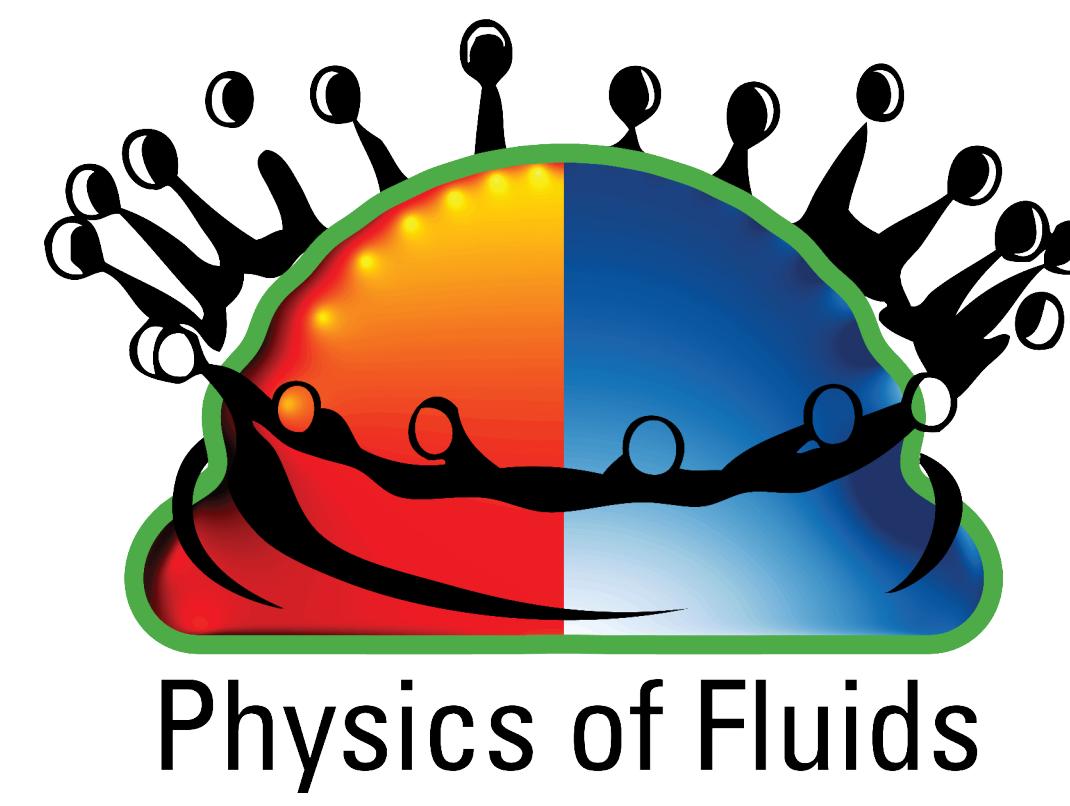


Viscous Free-Surface Flows

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European Research Council
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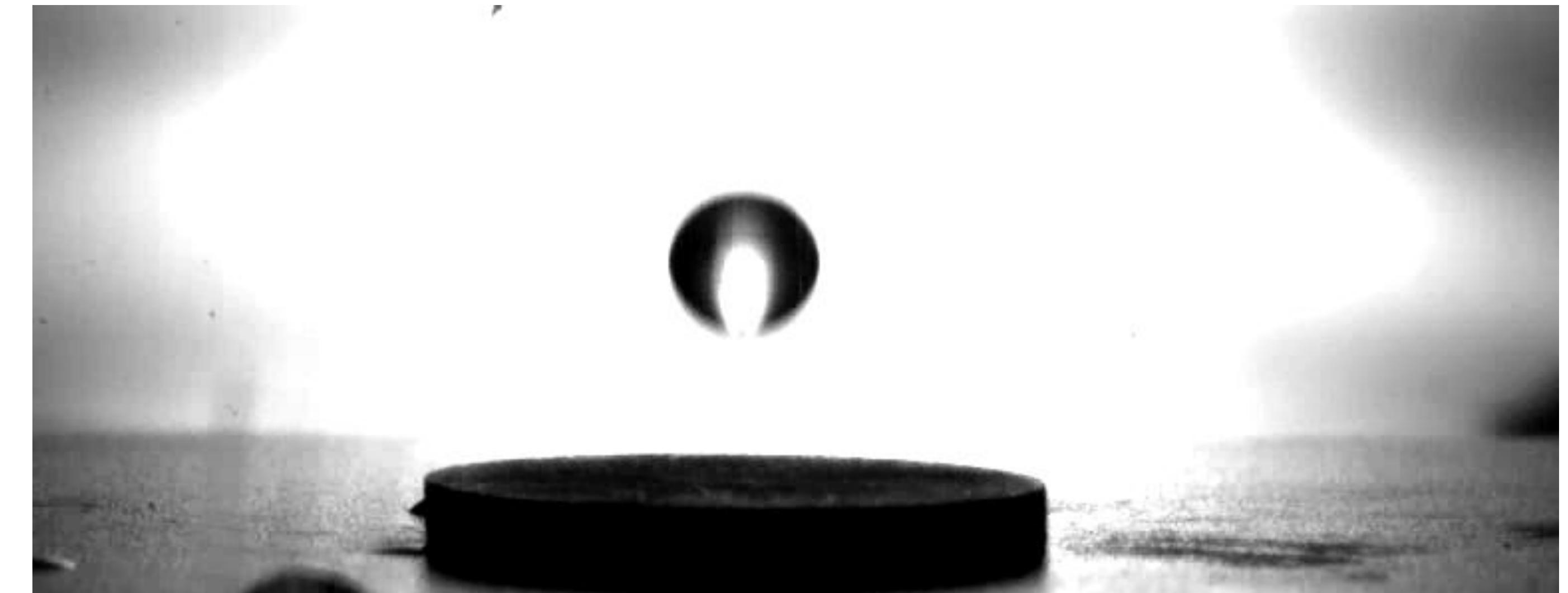
UNIVERSITY
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Drop impact on a superhydrophobic surface: What are the forces exerted on the substrate?



low velocity

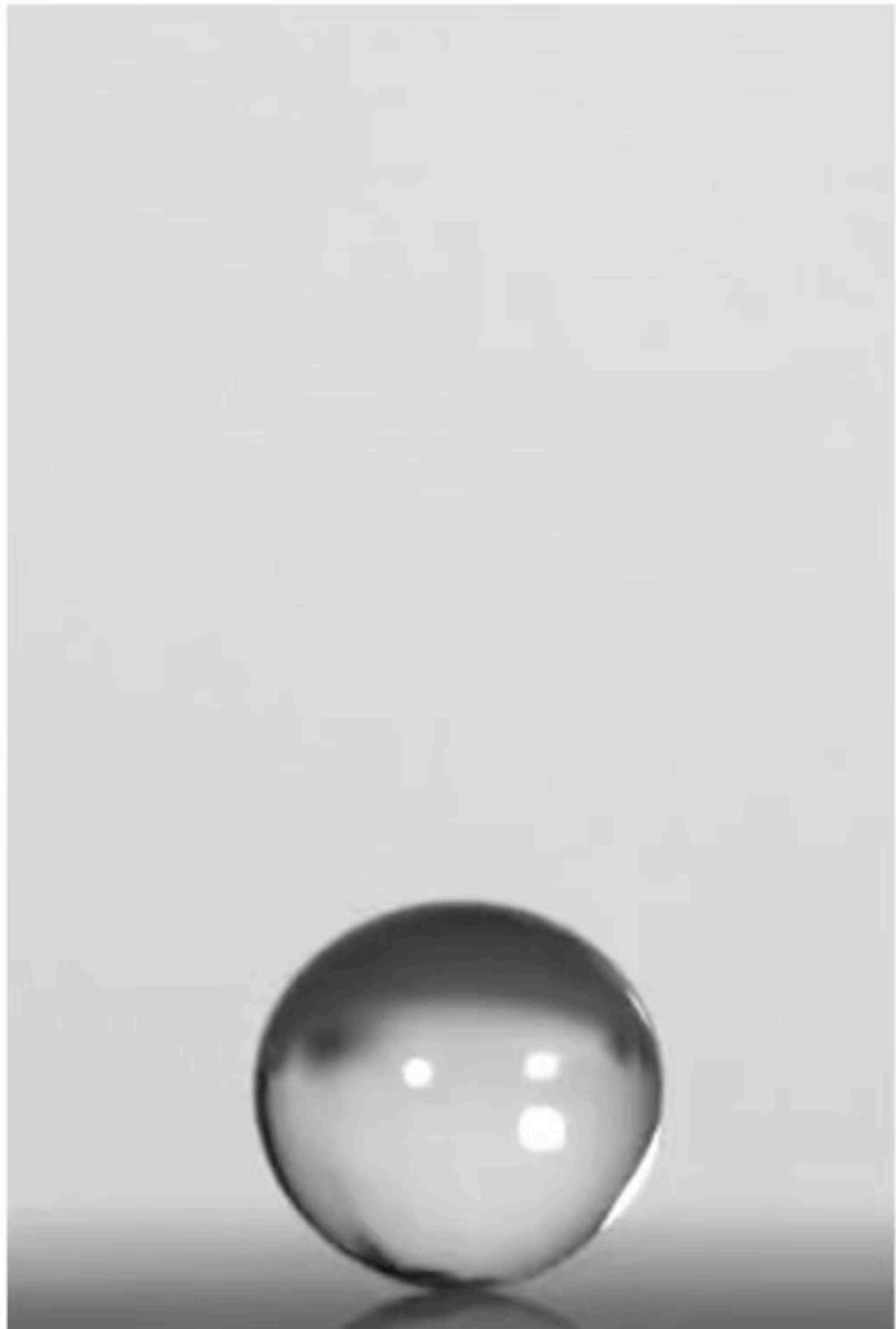


high velocity

Tsai, Pacheco, Pirat, Lefferts, Lohse,
Langmuir 25, 12293 (2009)

Parameter space of drop impact

- Velocity
- Diameter
- Viscosity
- Density
- Surface tension
- Surface roughness
- Temperatures
- Ambient air pressure
- ...



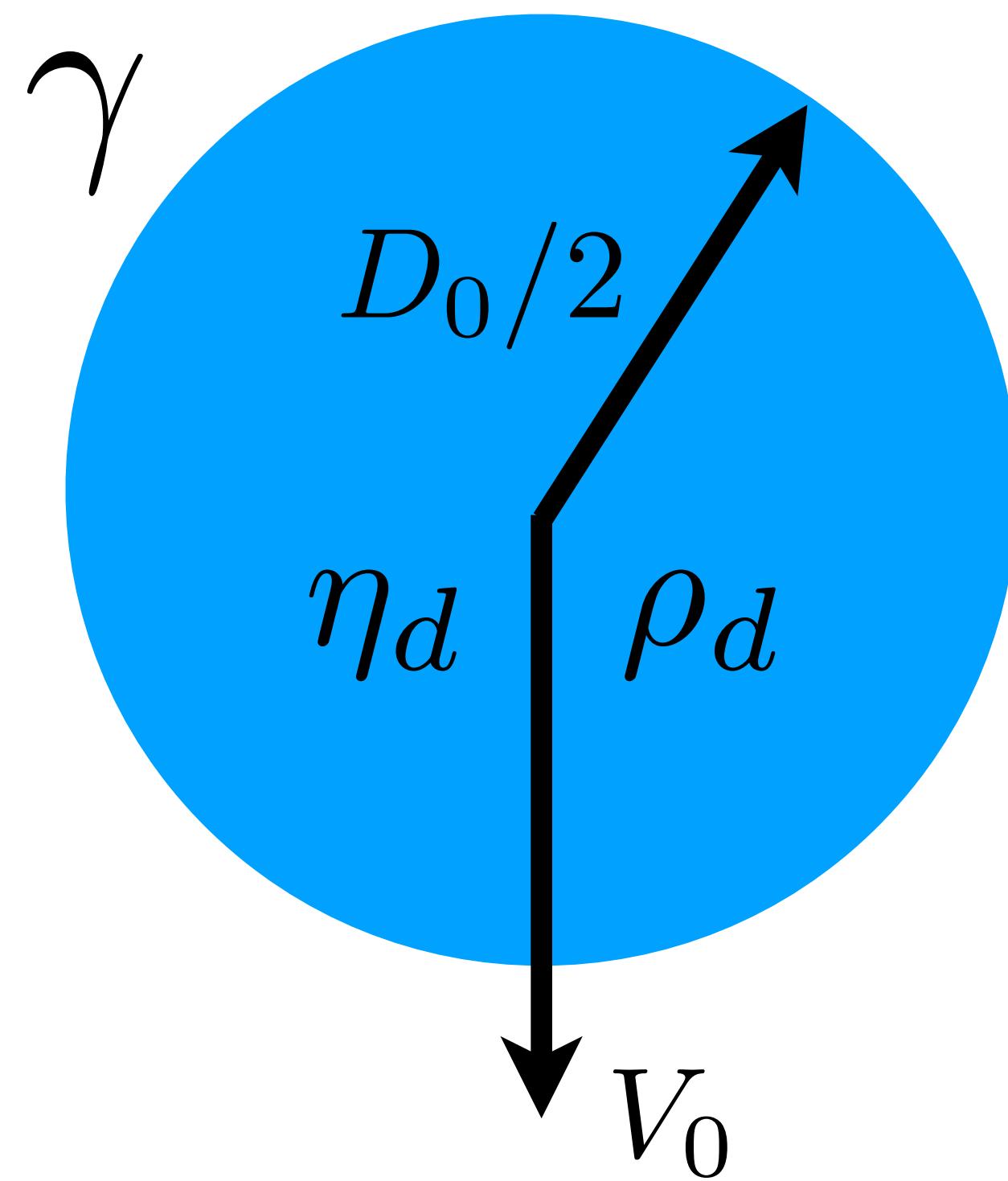


Viscous Free-Surface Flows

Drop Impact onto a solid surface

$$We = \frac{\rho_d V_0^2 D_0}{\gamma}$$

$$Oh = \frac{\eta_d}{\sqrt{\rho_d \gamma D_0}}$$



$$Oh_s = \frac{\eta_s}{\sqrt{\rho_d \gamma D_0}} = 10^{-5}$$

$$\rho_s / \rho_d = 10^{-3}$$

C. Lv B. Zhang D. Lohse

Superhydrophobic substrate



How does it look like?

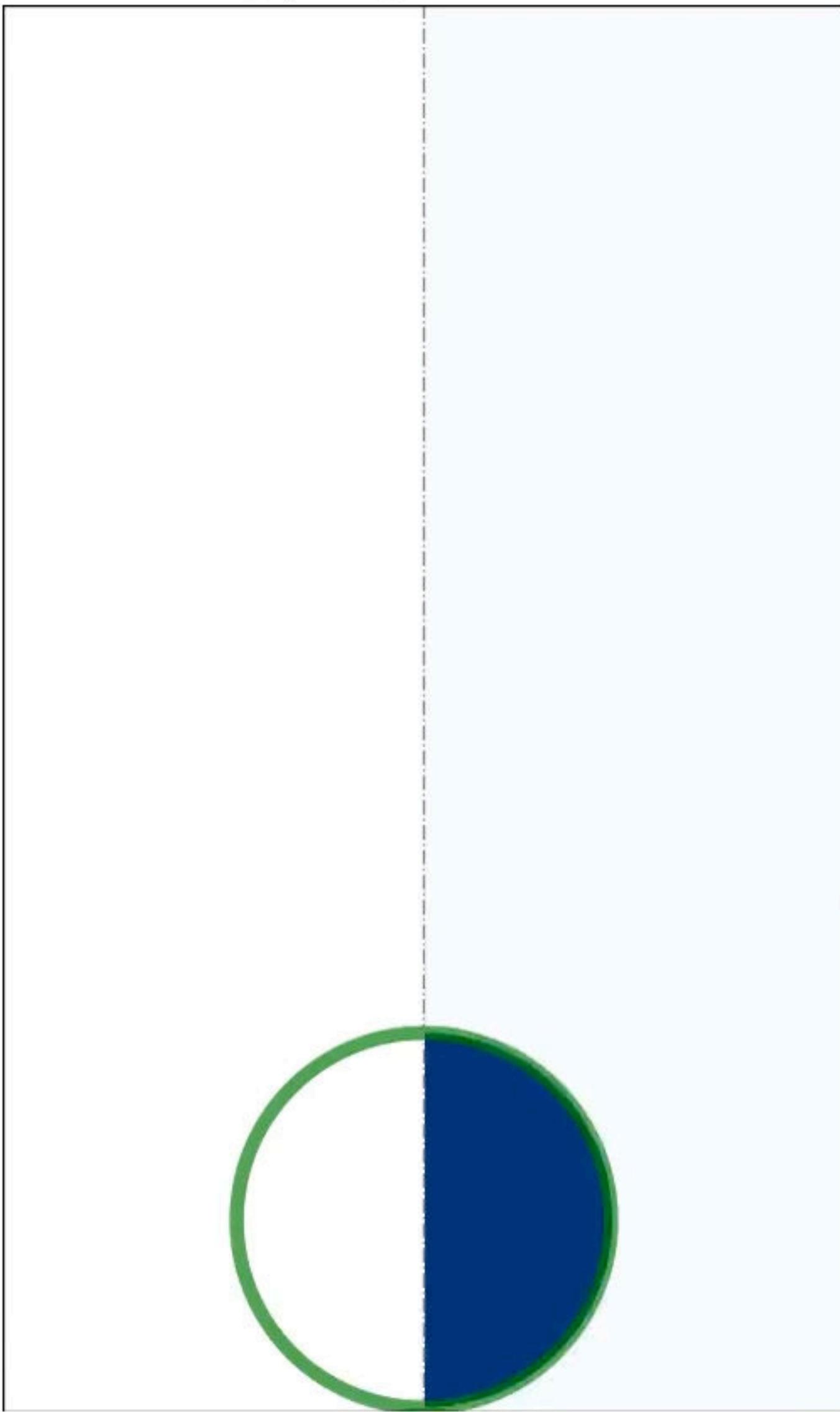
Volume of Fluid Method:
Basilisk-Code



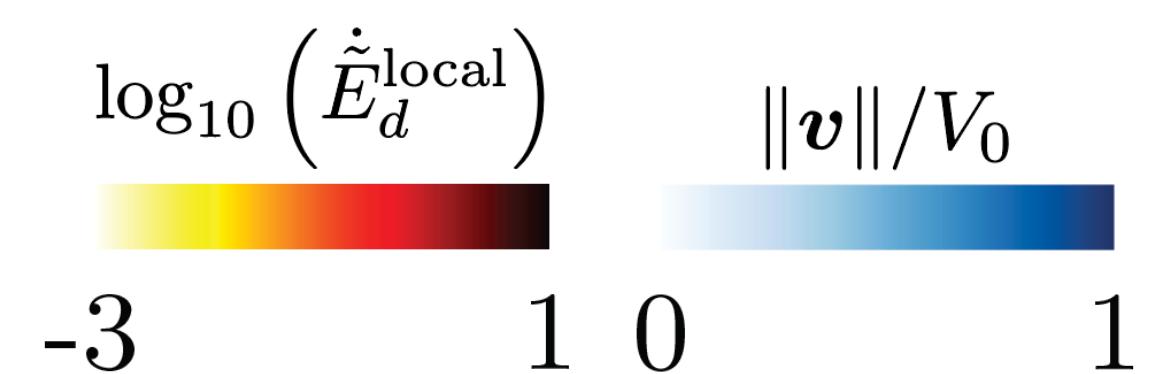
Stéphane Popinet *et al.*

$We = 40$

$$V_0 t / D_0 = 0.000$$



- Impact
- Spreading
- Recoil
- Take-off

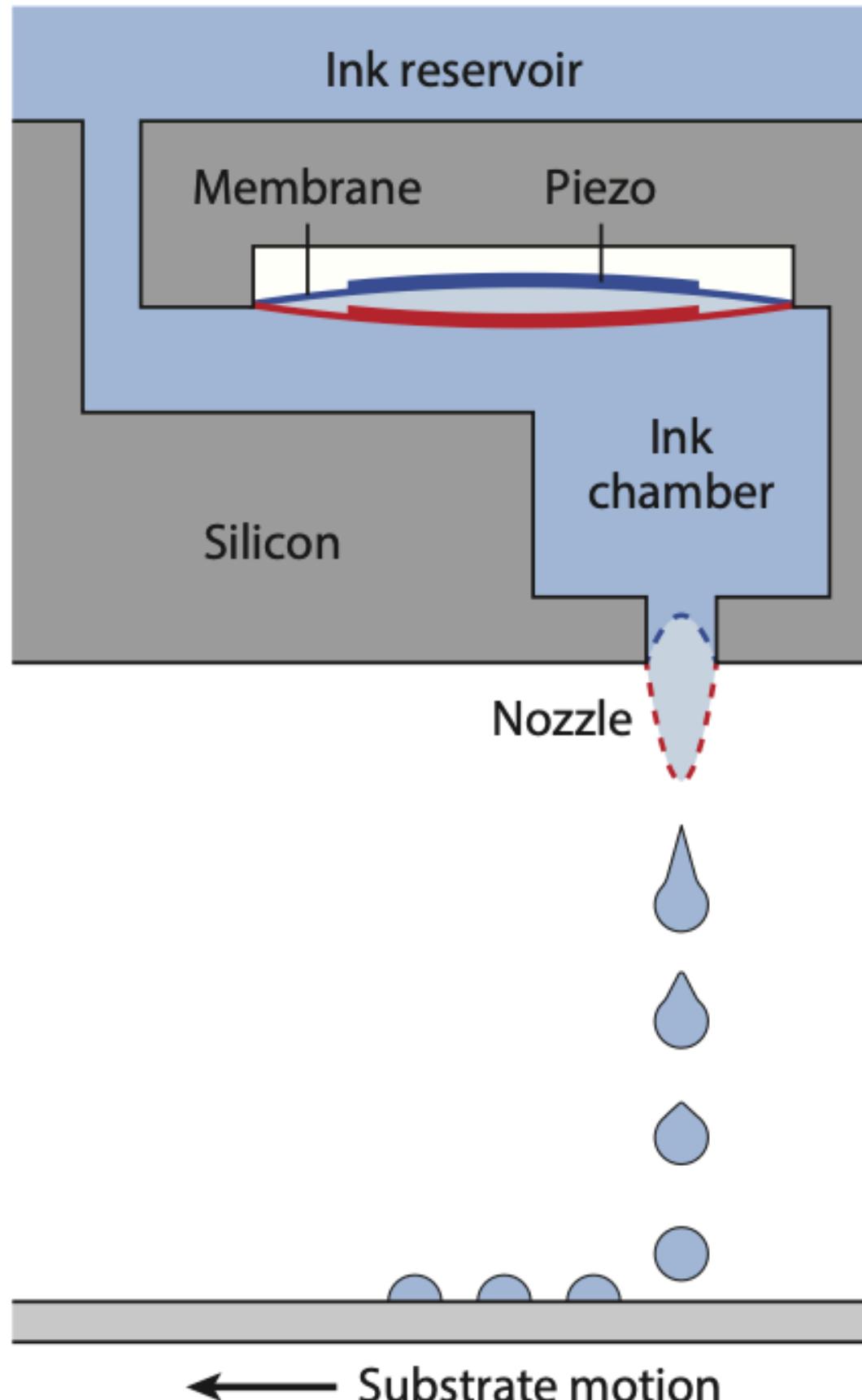


$$\dot{\tilde{E}}_d^{\text{local}} = 2\eta(\mathcal{D} : \mathcal{D})$$
$$\mathcal{D} = (\nabla \mathbf{v} + (\nabla \mathbf{v})^T) / 2$$

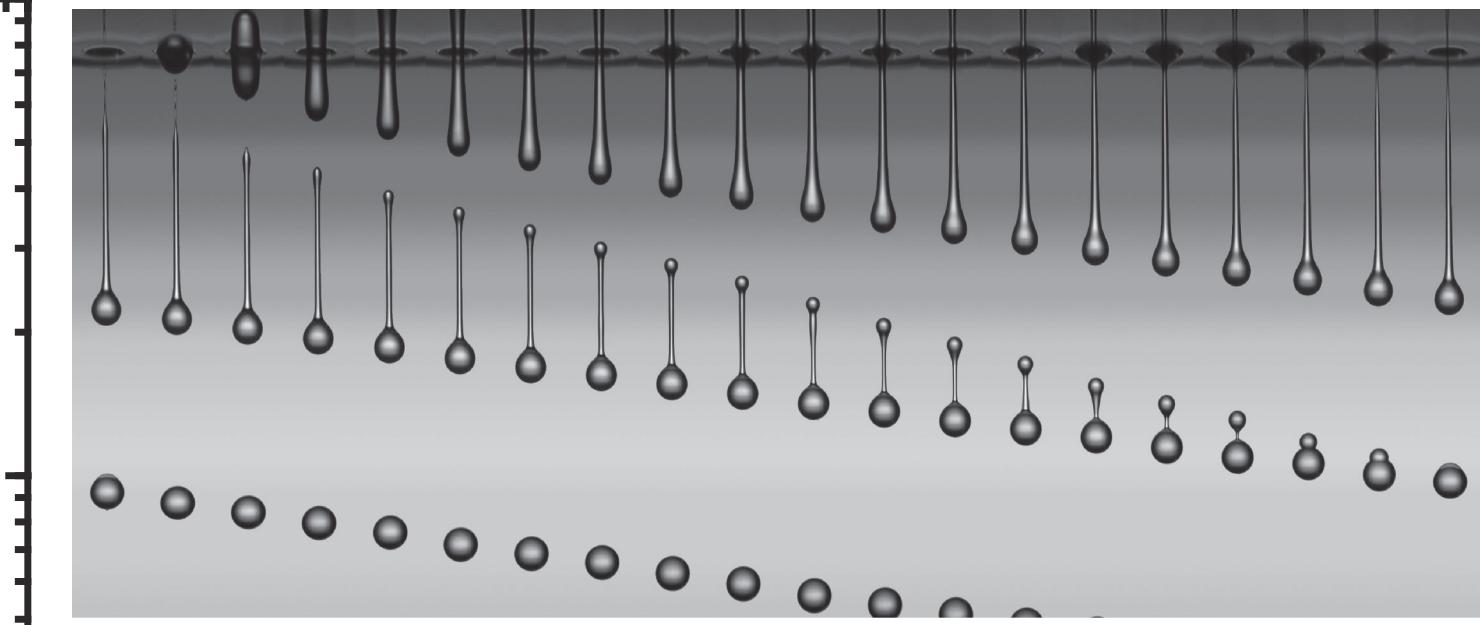
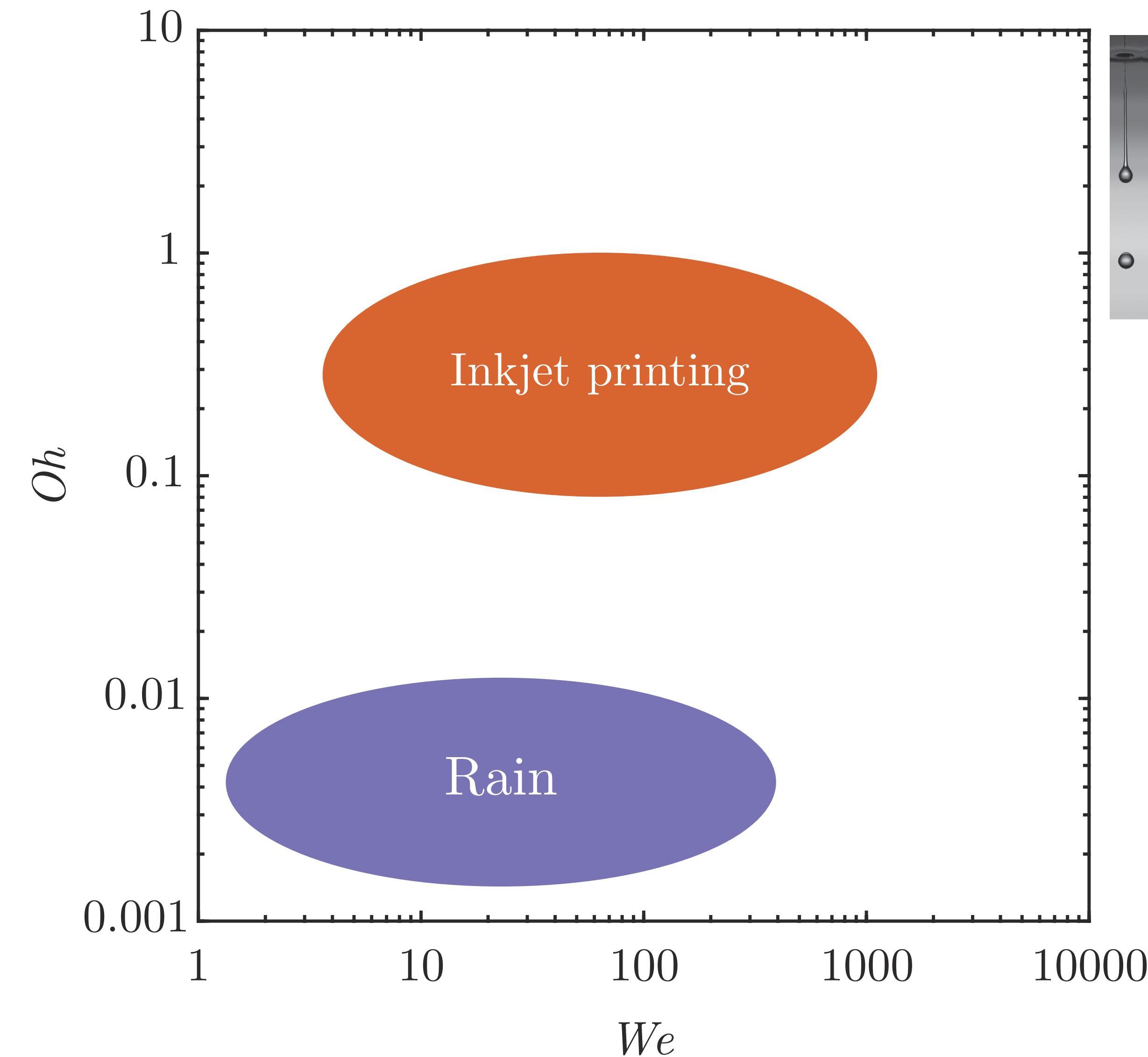


Viscous Free-Surface Flows

Oh vs We parameter space



Lohse, Annu. Rev. Fluid Mech.
2022. 54:349–82

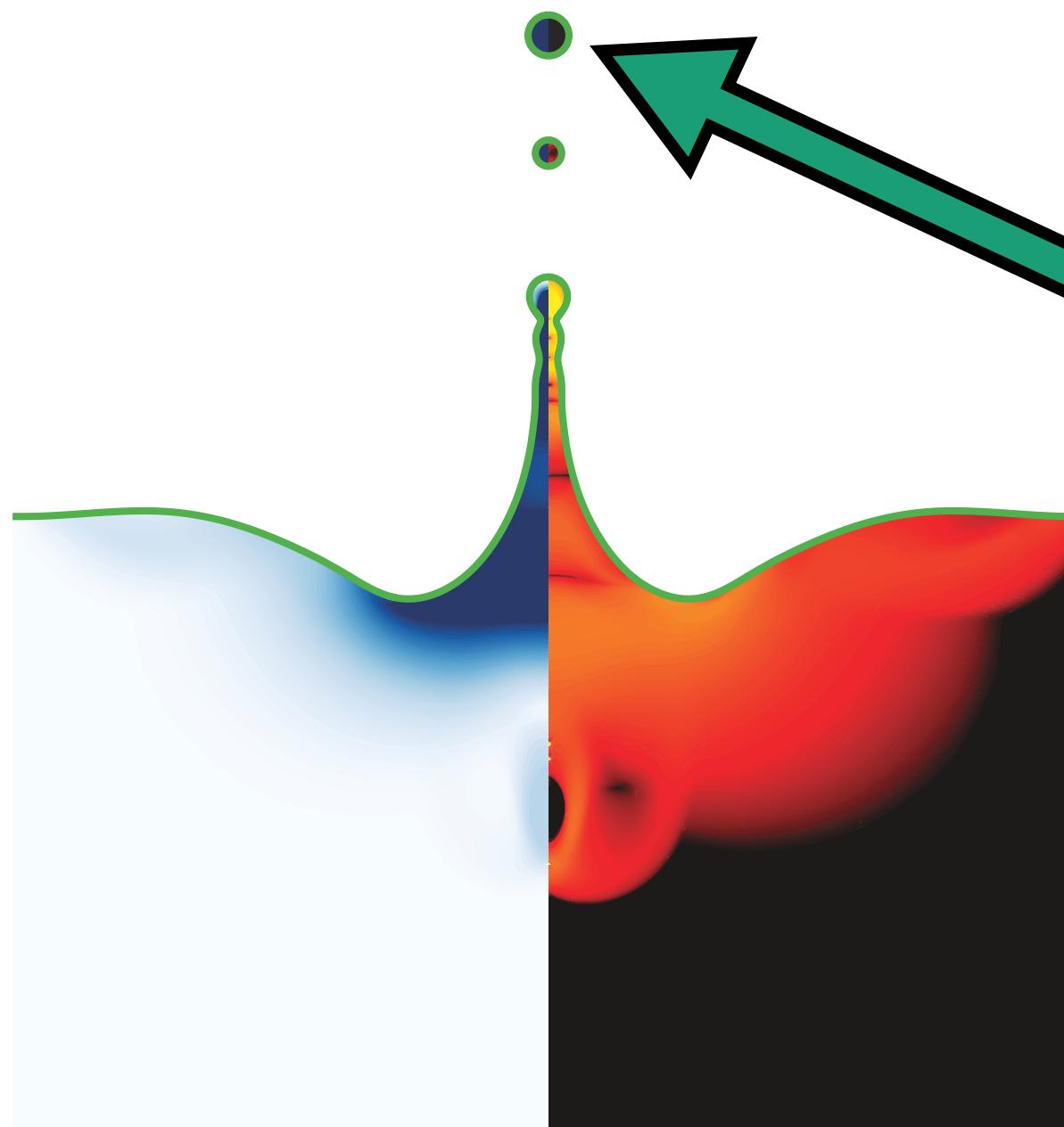


$$Oh = \frac{\eta_d}{\sqrt{\rho_d \gamma D_0}}$$
$$We = \frac{\rho_d V_0^2 D_0}{\gamma}$$



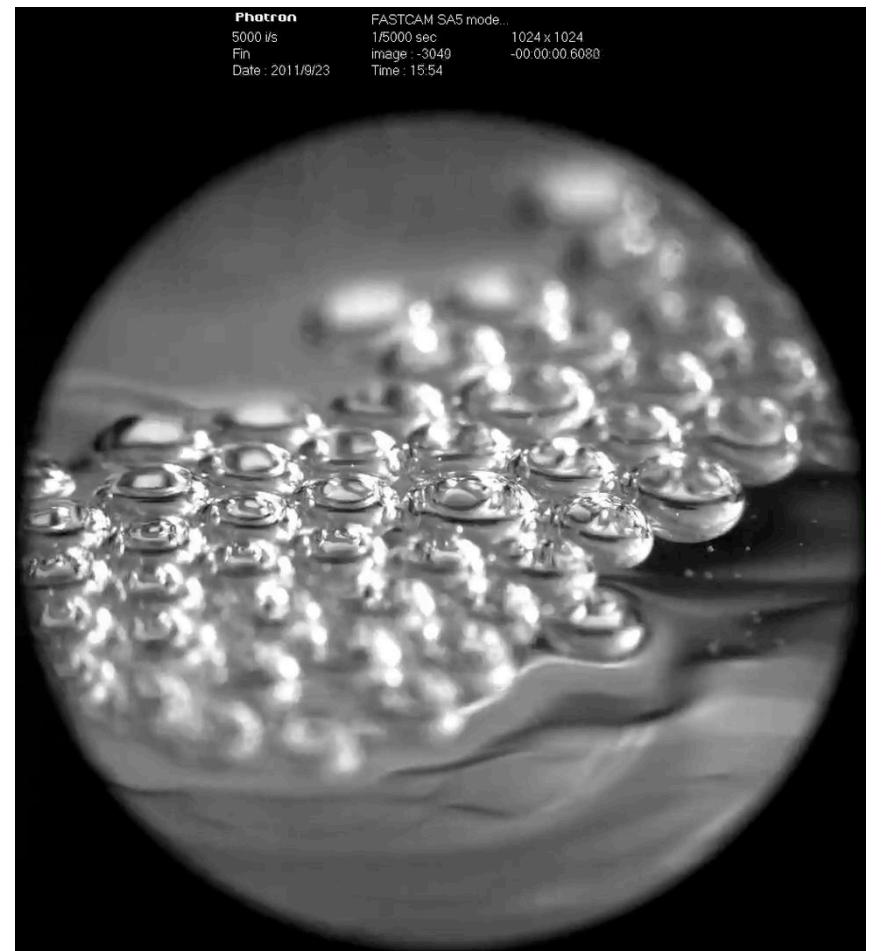
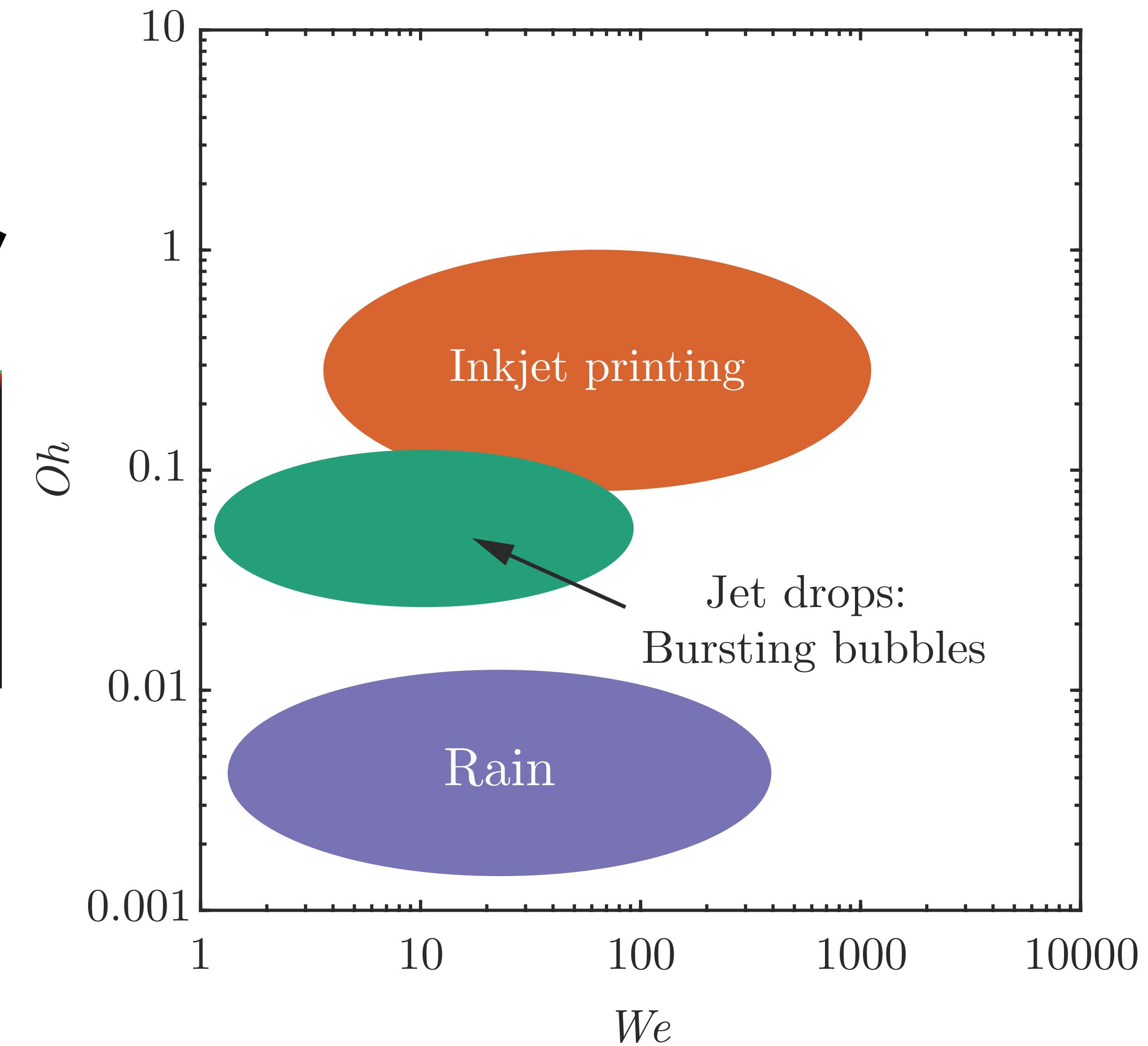
Viscous Free-Surface Flows

Oh vs We parameter space



Sanjay, Lohse, & Jalaal,
J. Fluid Mech. (2021), vol. 922, A2

Néel & Deike,
Phys. Rev. Fluids 7, 103603



Video:
Thomas Séon & Arup Kumar Das

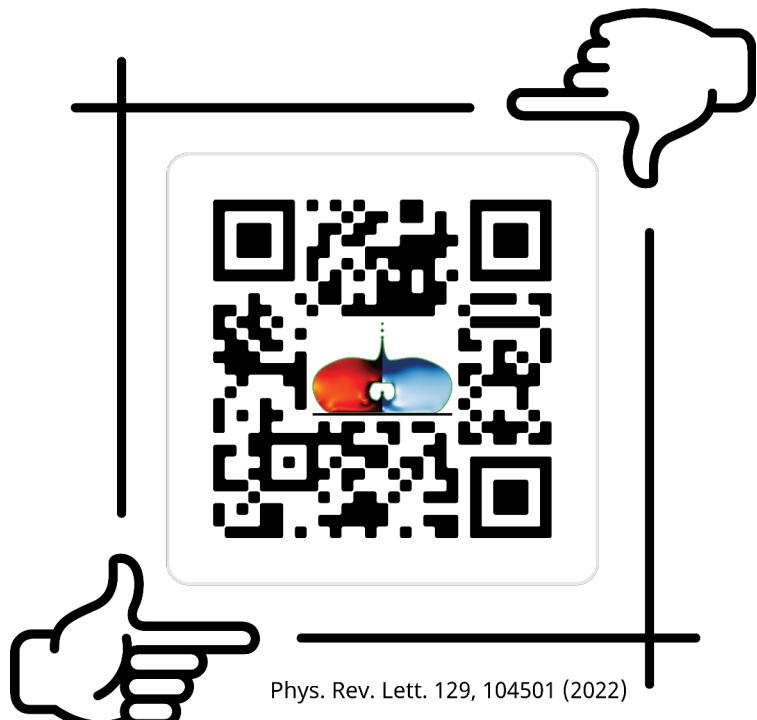
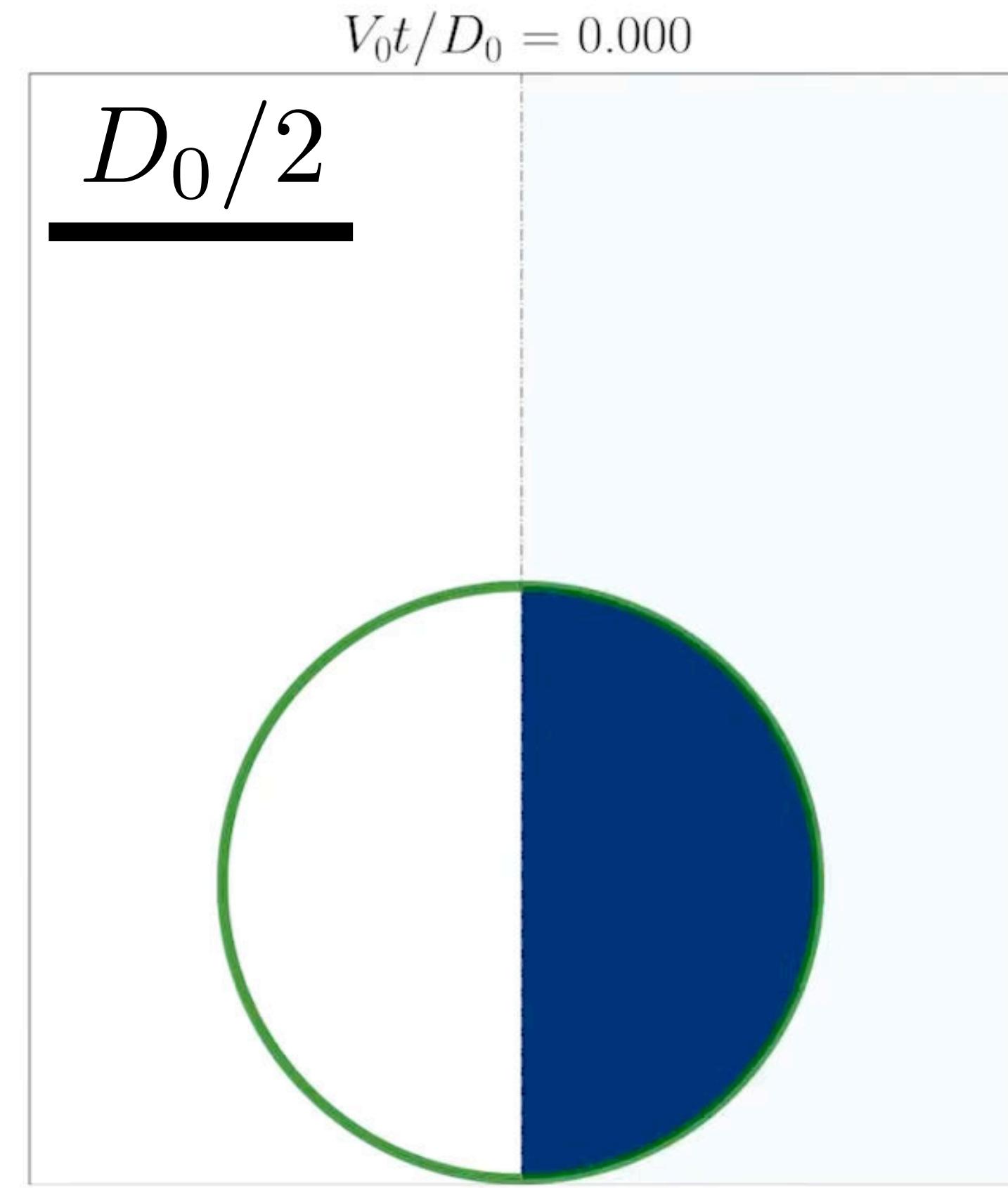
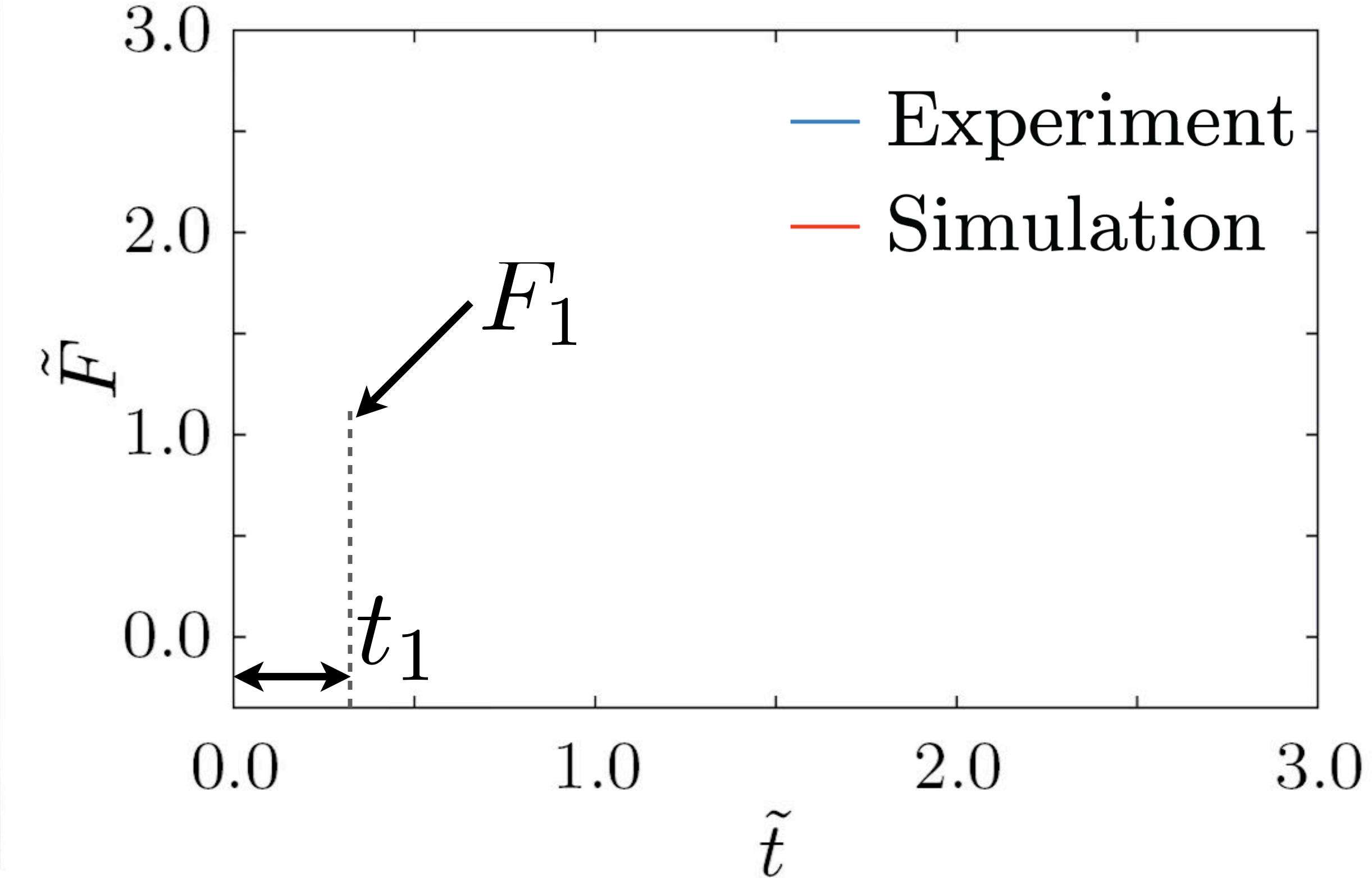
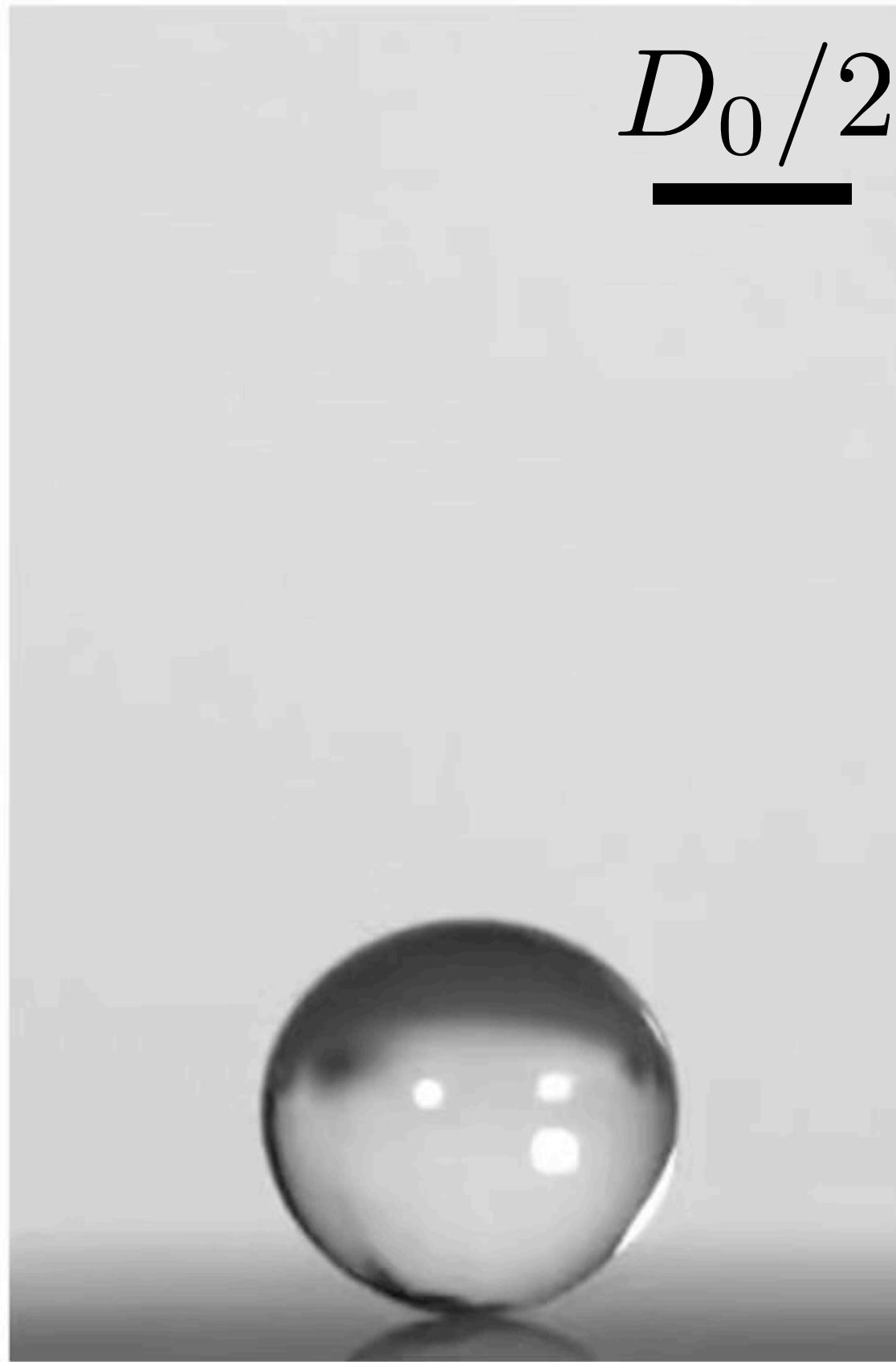
$$Oh = \frac{\eta_d}{\sqrt{\rho_d \gamma D_0}}$$

$$We = \frac{\rho_d V_0^2 D_0}{\gamma}$$

$We = 9$

$Oh = 0.0025$

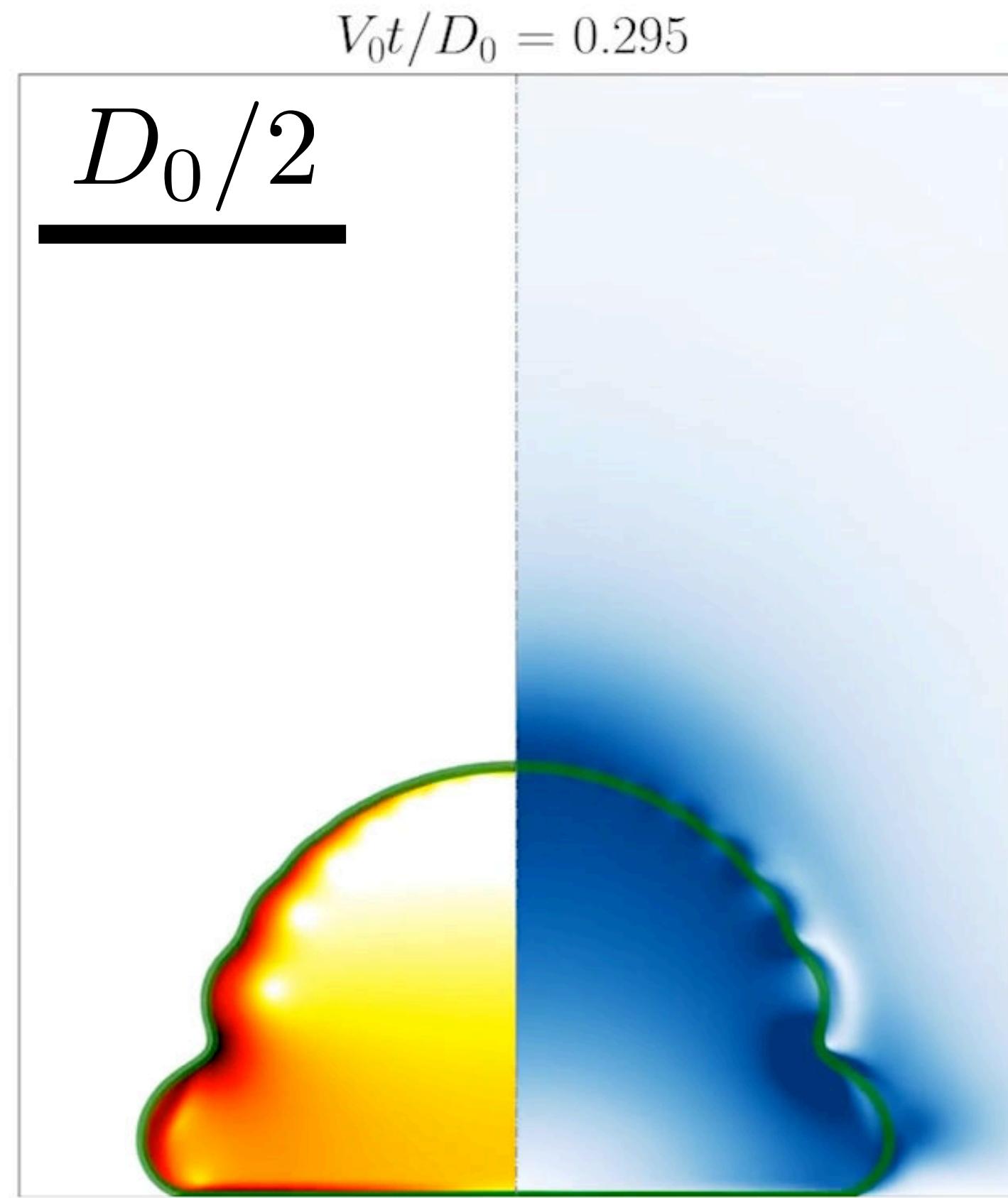
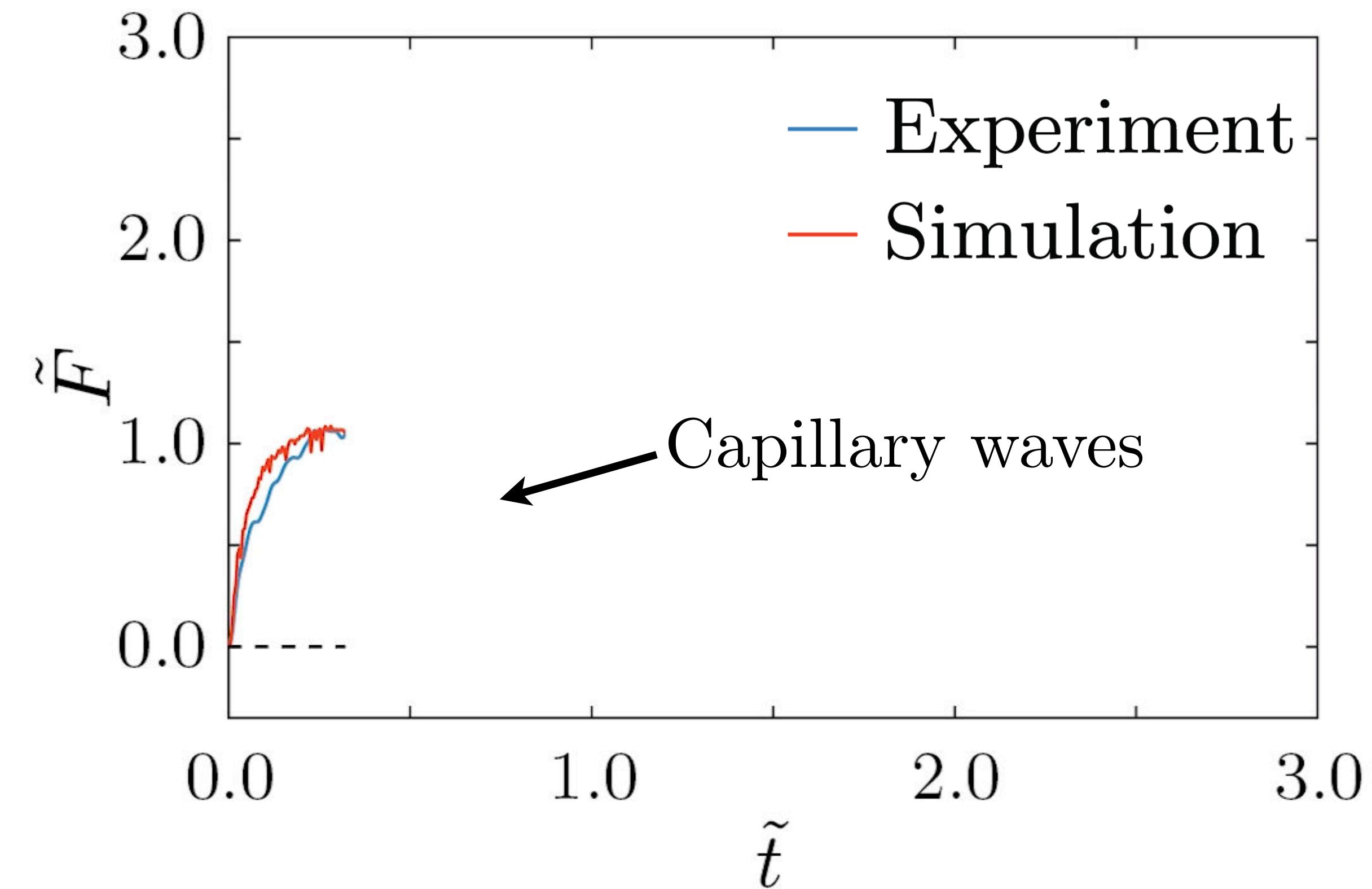
$D_0/2$



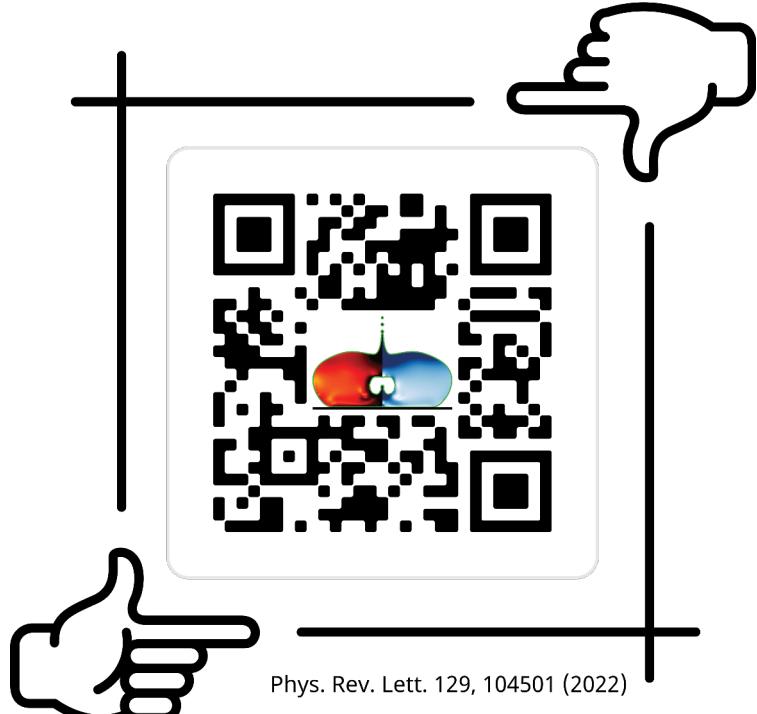
$We = 9$

$Oh = 0.0025$

$\underline{D_0/2}$



Renardy, **Popinet**, Duchemin, Renardy, Zaleski, Josserand,
Drumright-Clarke, Richard, Clanet, Quéré
J. Fluid Mech. 484, 69 (2003)



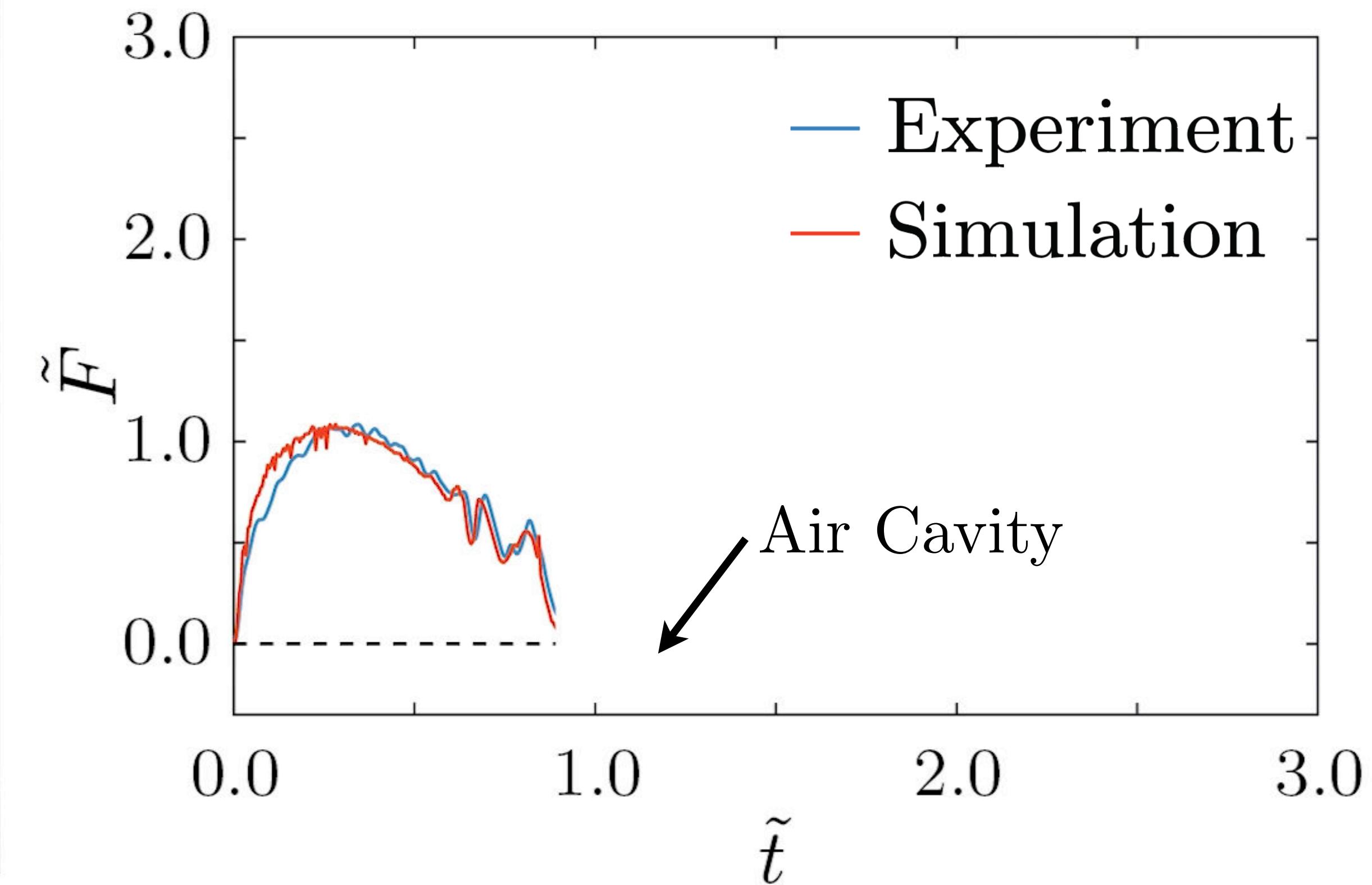
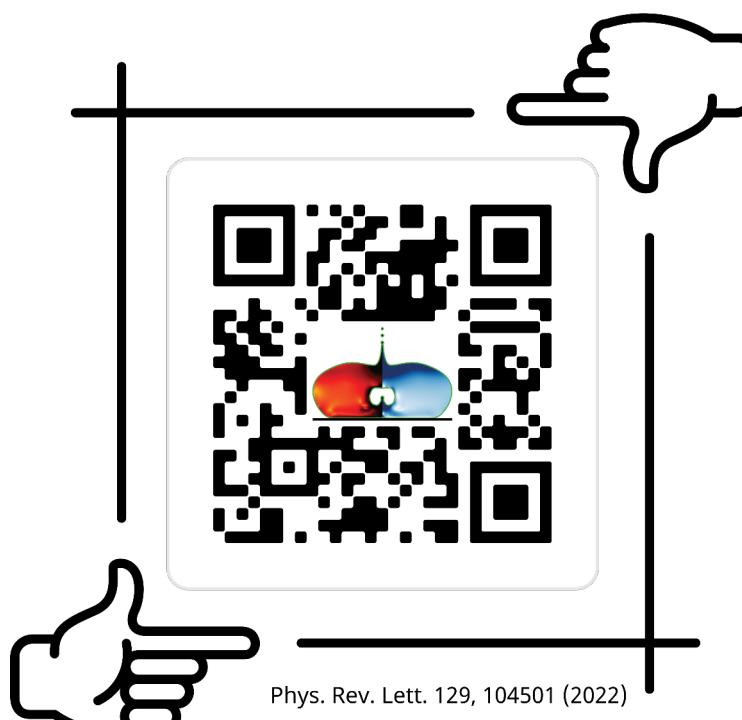
$\log_{10} (\dot{\tilde{E}}_d^{\text{local}})$ $\|\mathbf{v}\|/V_0$
-3 1 0 1

$We = 9$

$Oh = 0.0025$

$D_0/2$

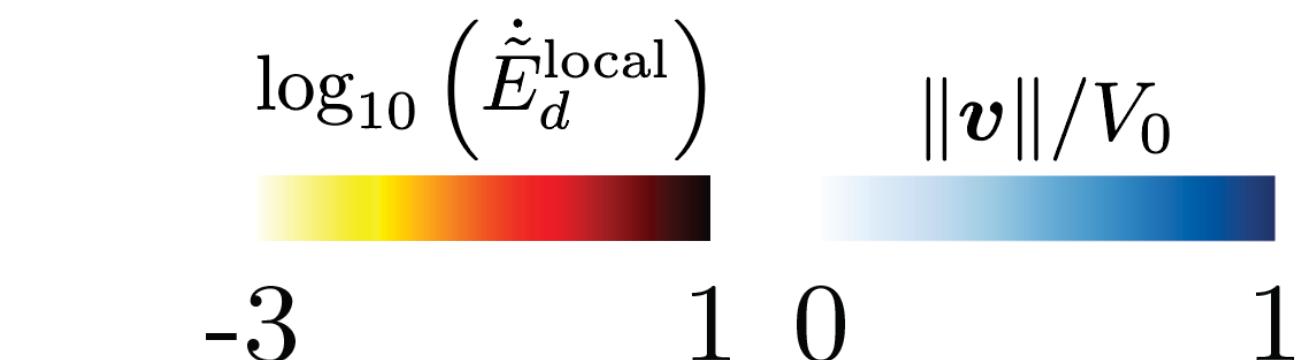
Air Cavity



$V_0 t / D_0 = 0.855$

$D_0/2$

Air Cavity



Air bubble entrainment !

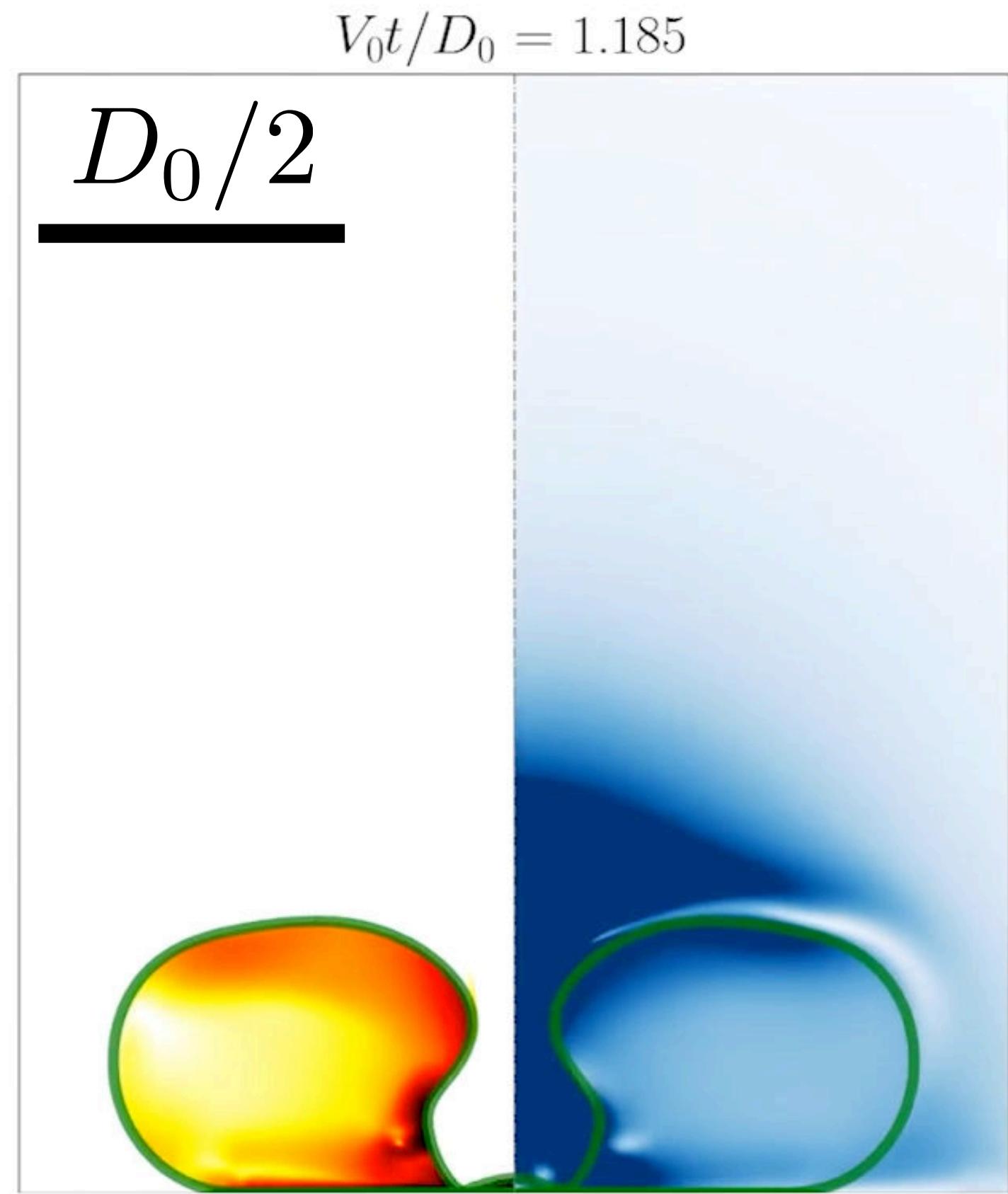
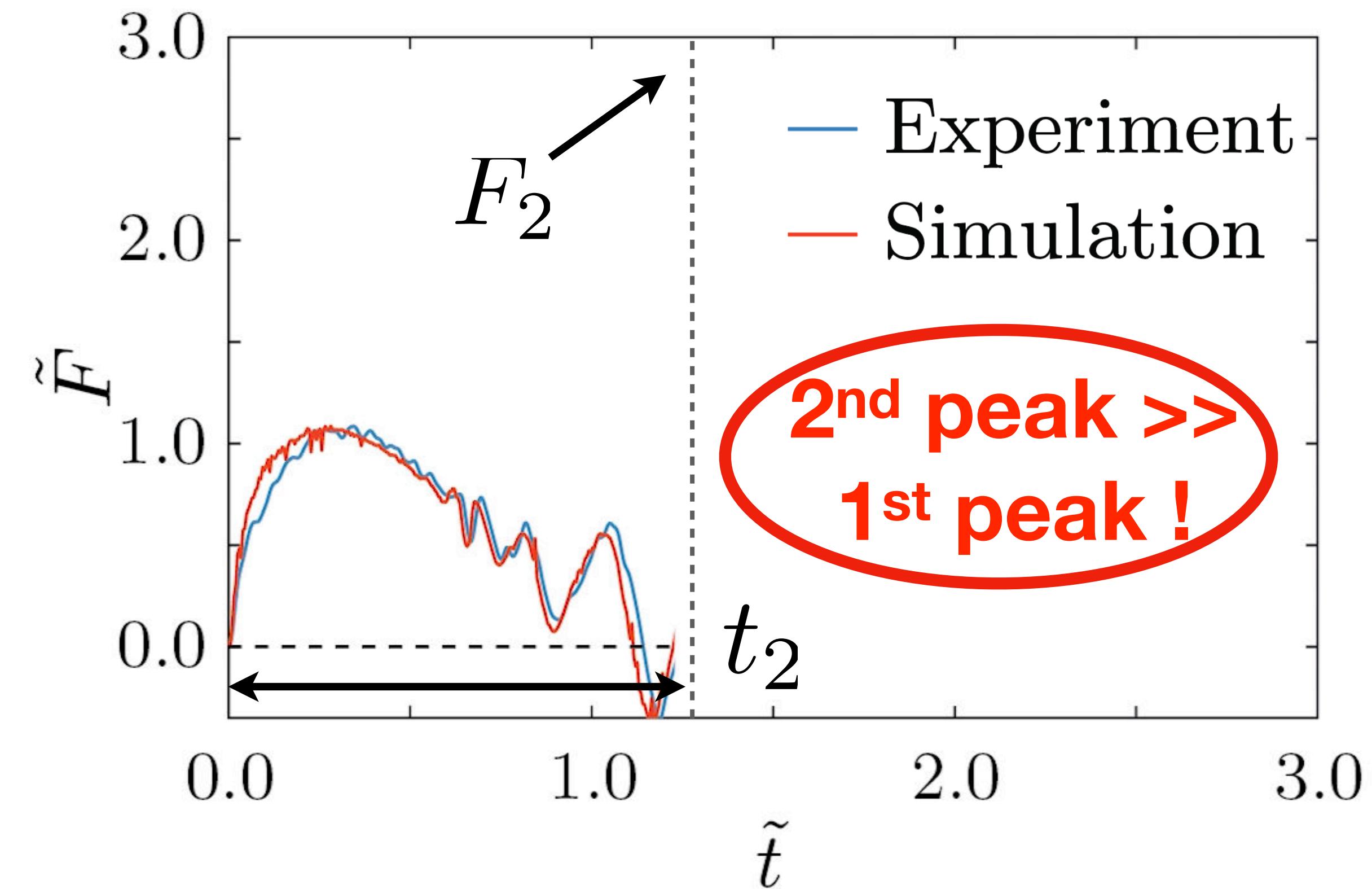
Bartolo, Josserand, & Bonn

Phys. Rev. Lett. 96, 124501 (2006)

$We = 9$

$Oh = 0.0025$

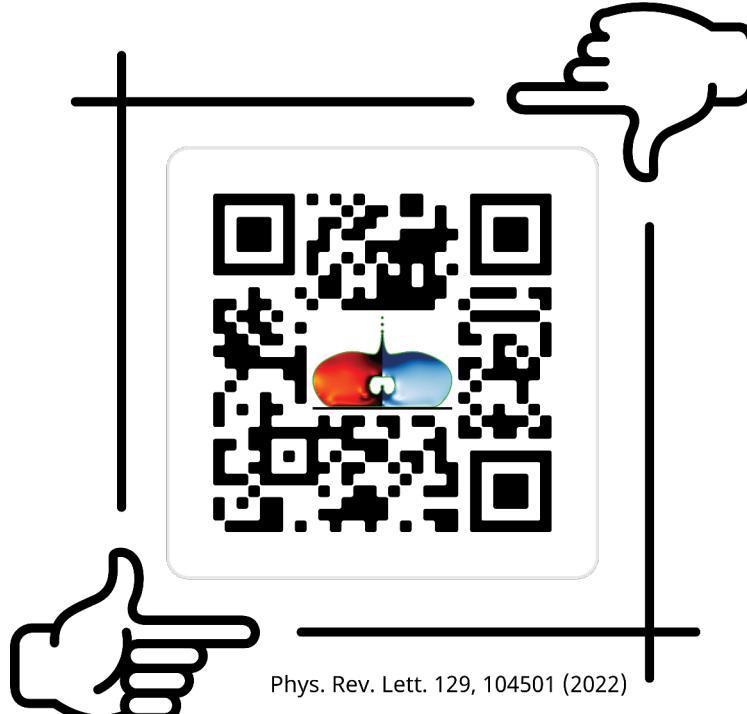
$D_0/2$



**Closure of air bubble leads
to singular jet!**

Bartolo, Josserand, & Bonn

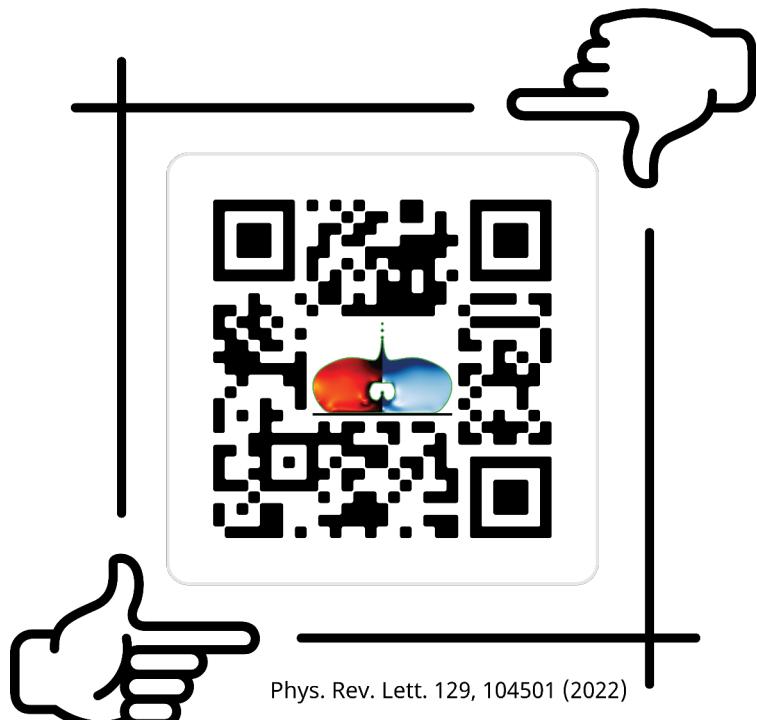
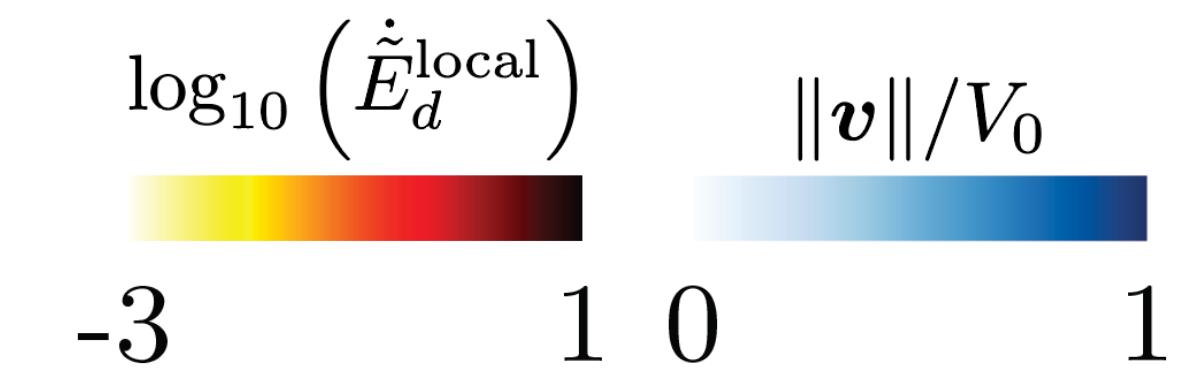
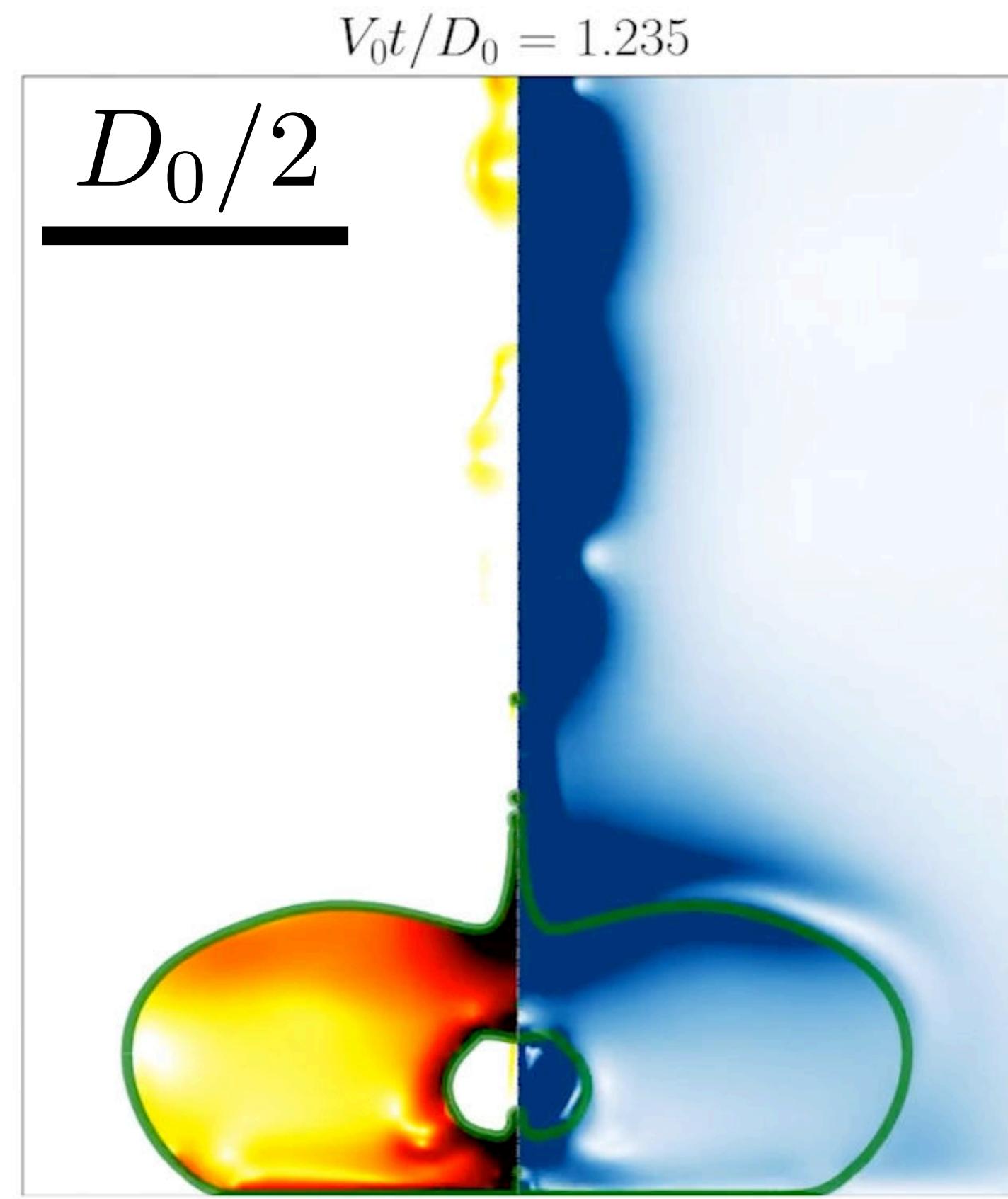
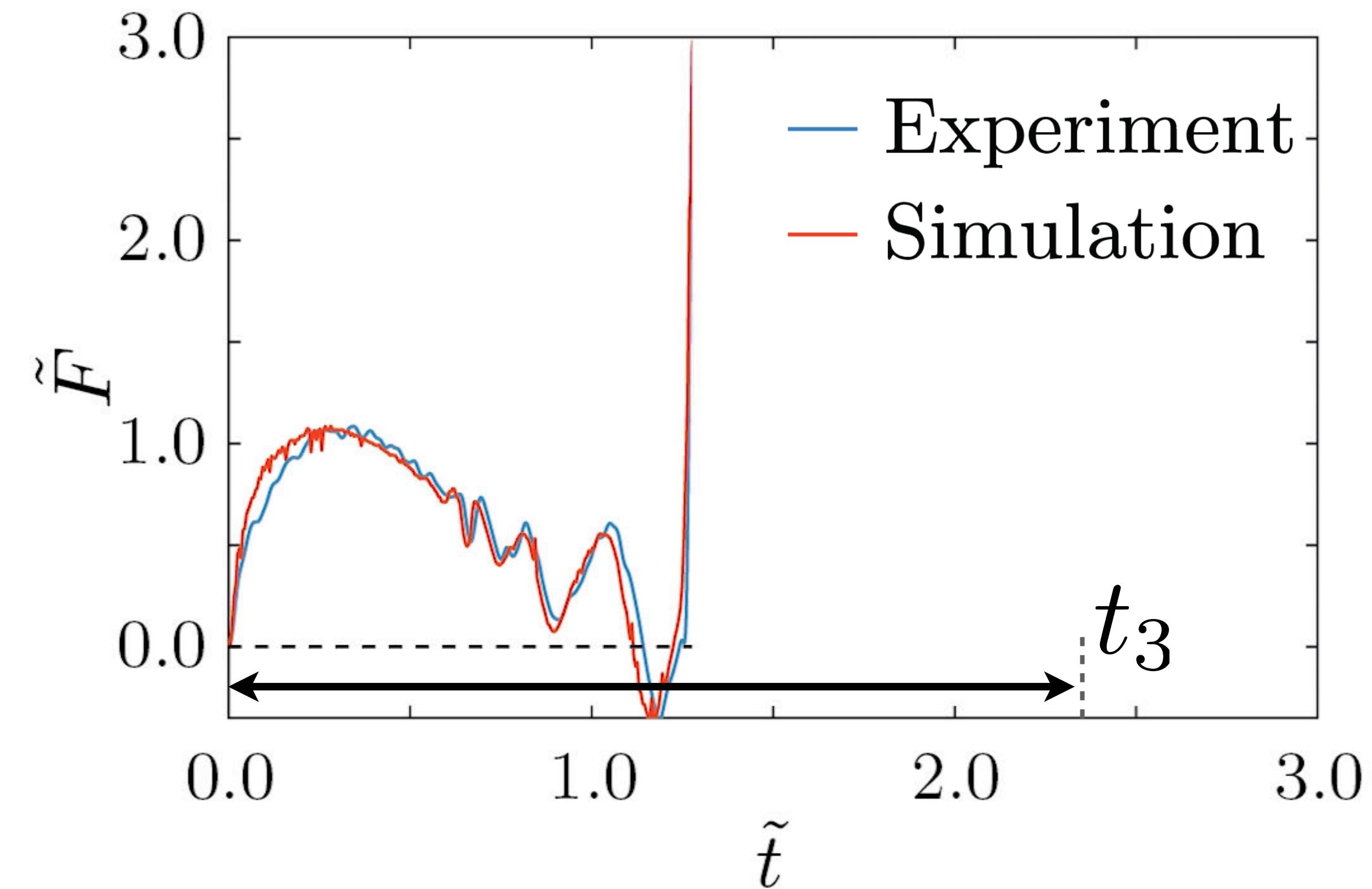
Phys. Rev. Lett. 96, 124501 (2006)



$We = 9$

$Oh = 0.0025$

$D_0/2$



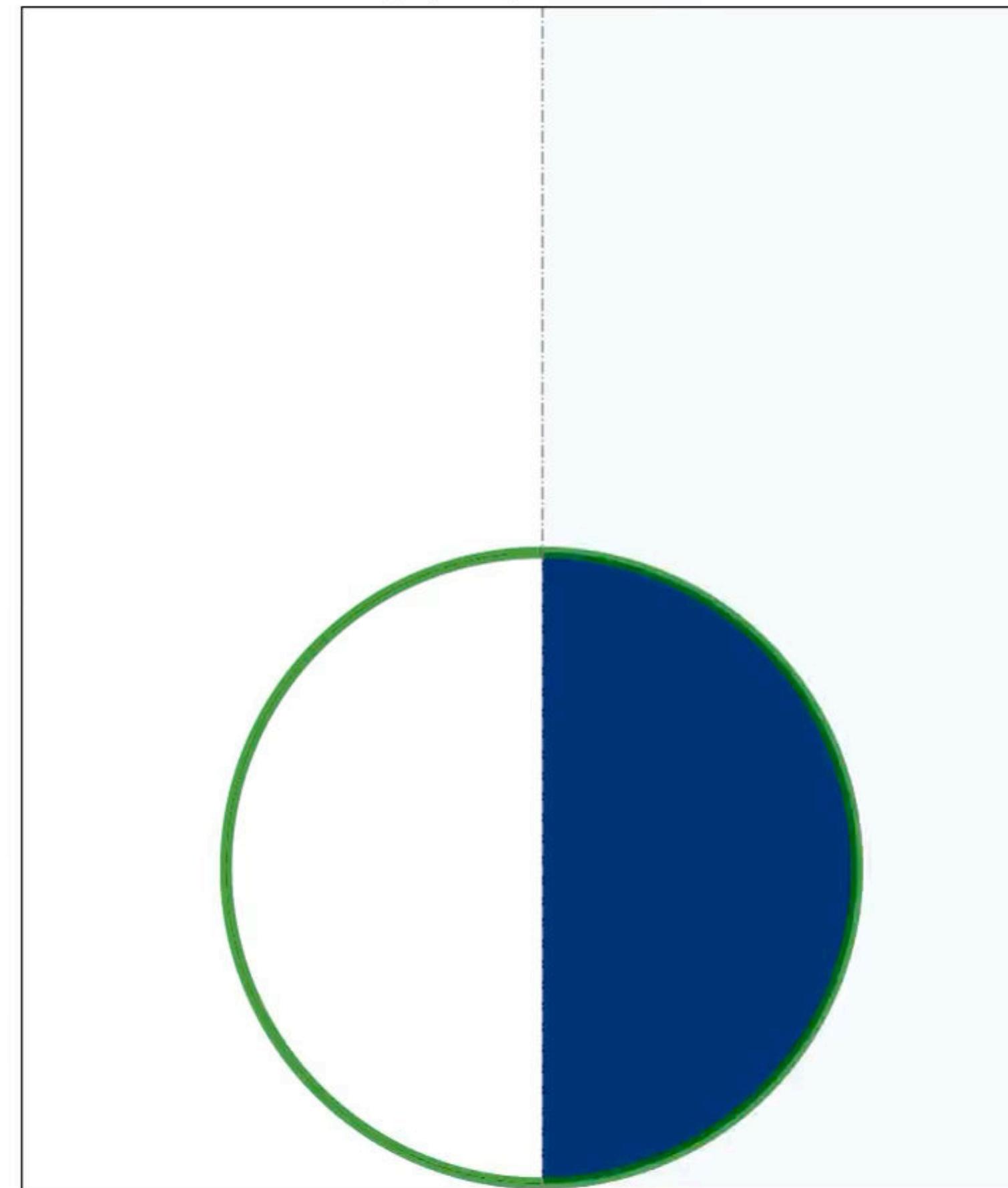
Ways to kill this ‘singularity’!

I. Viscous dissipation

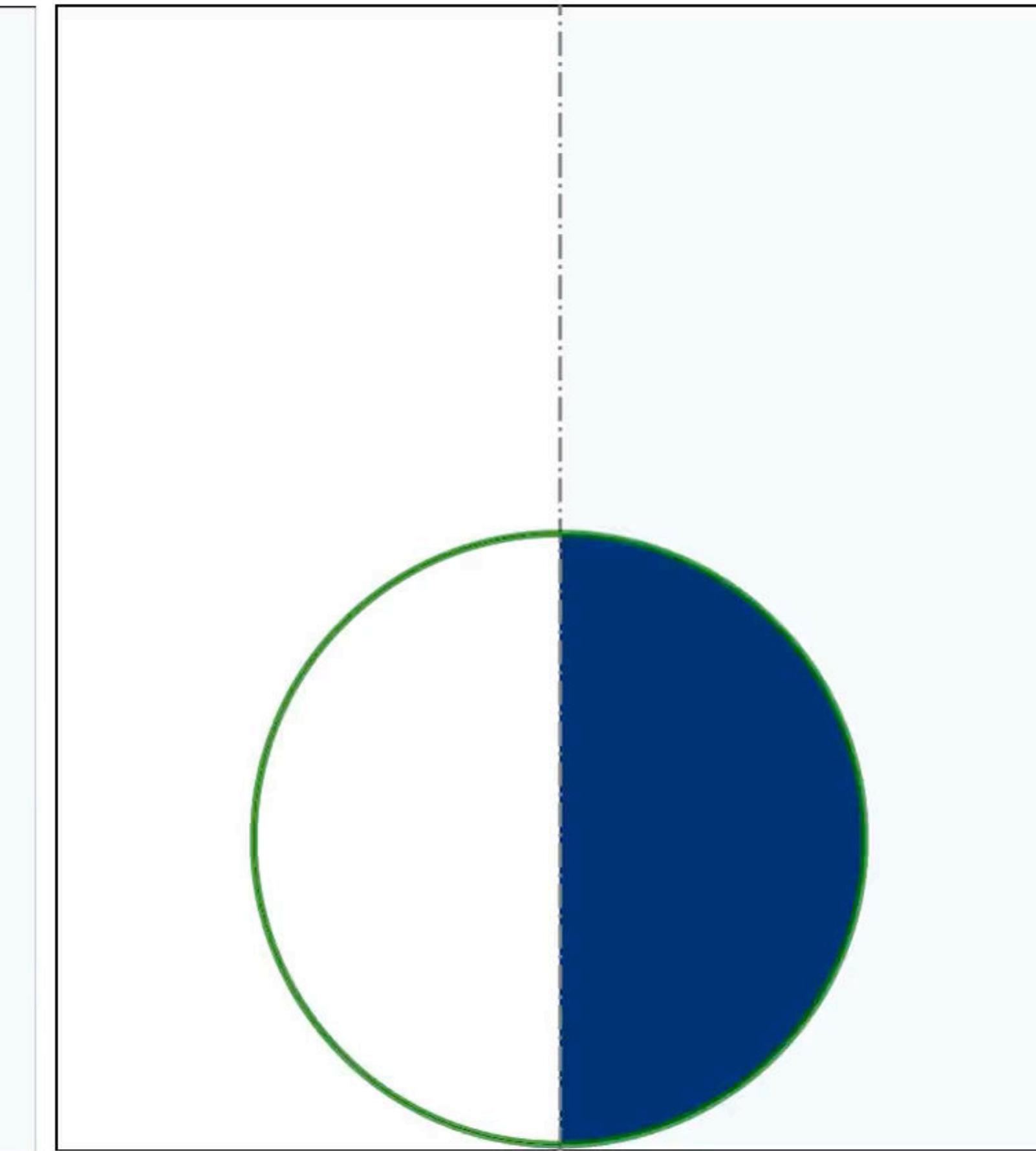
Jet & bubble

$We = 9$

$V_0 t / D_0 = 0.000$



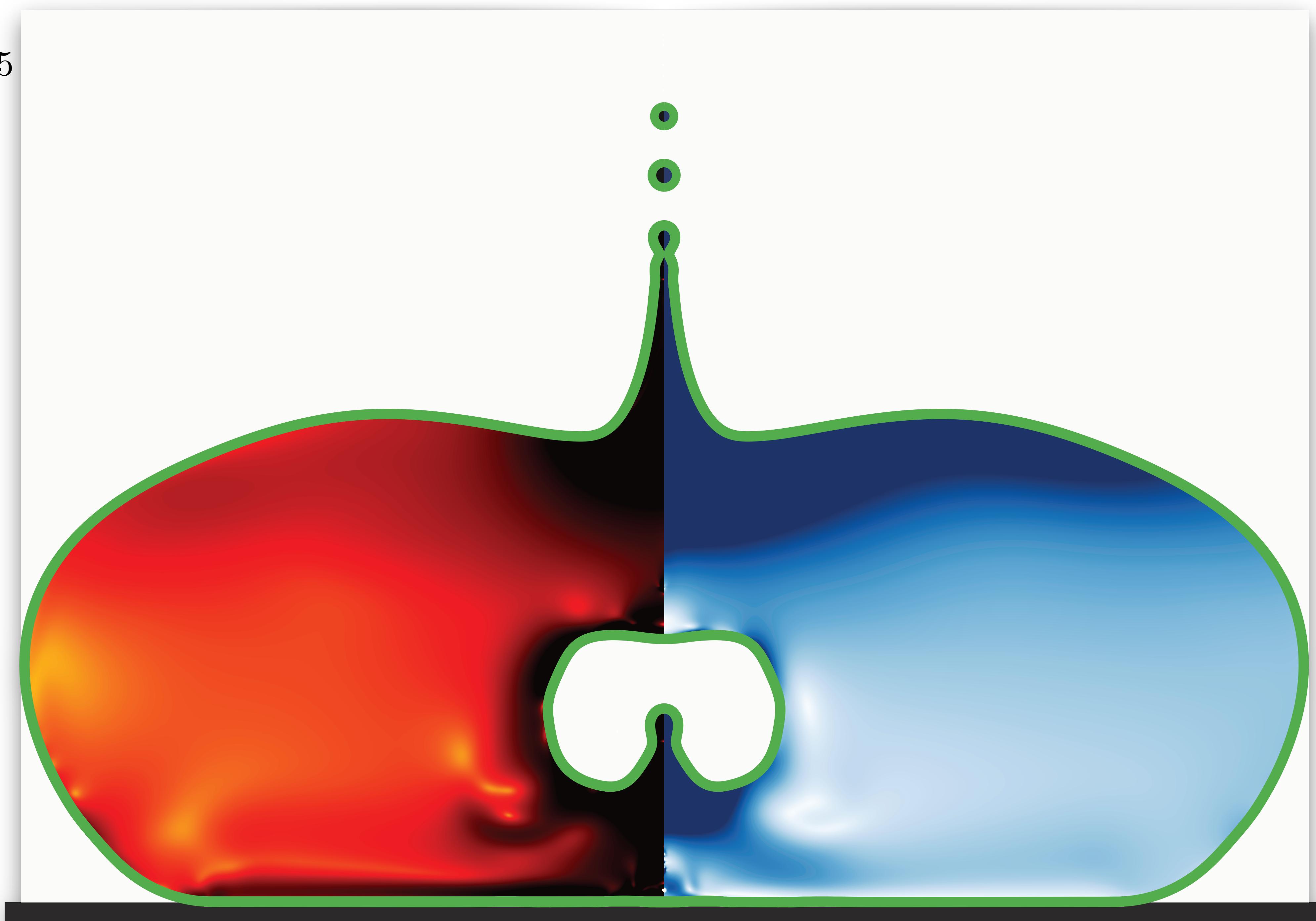
$Oh = 0.0025$



$Oh = 0.005$

$We = 9$

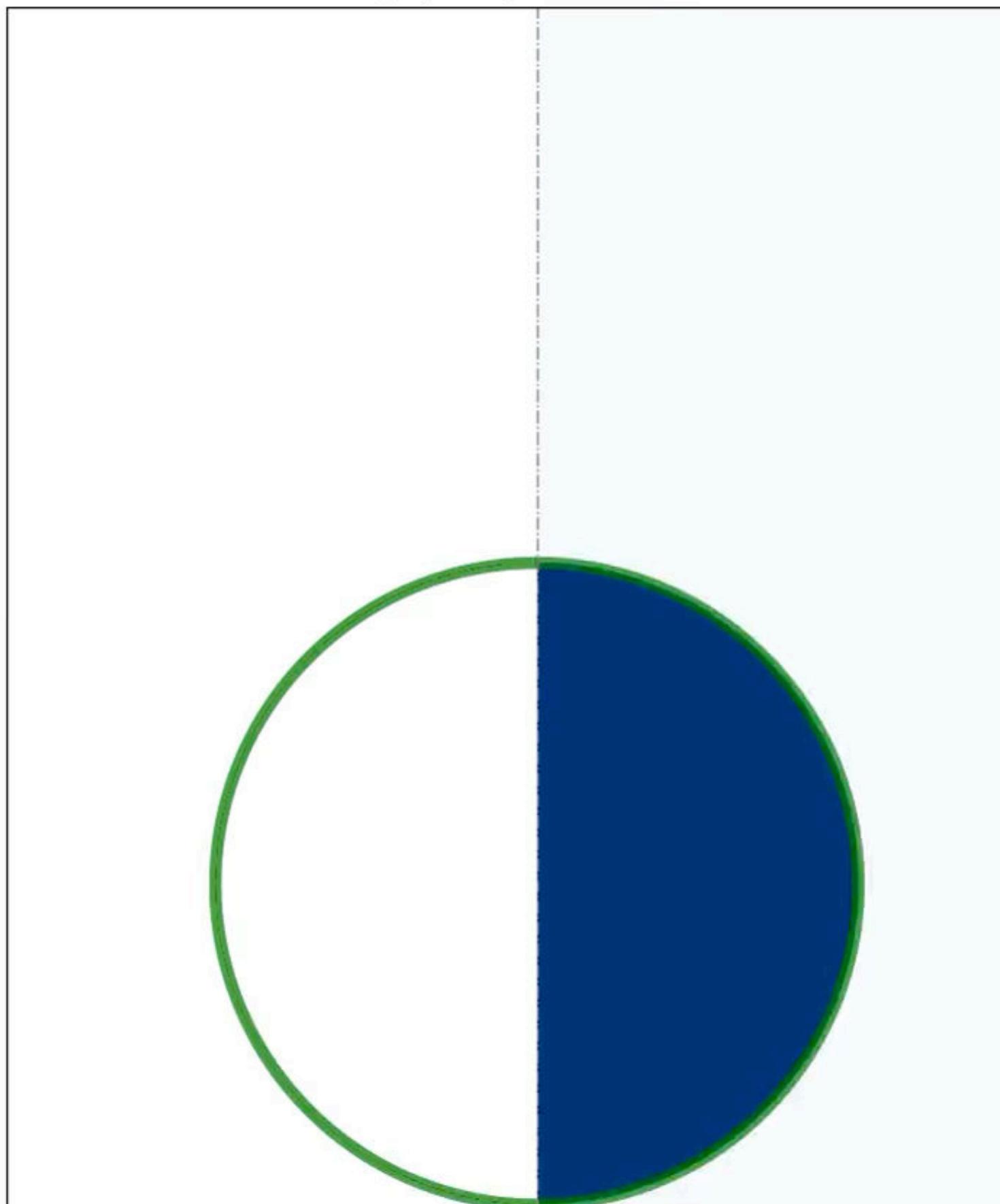
$Oh = 0.0025$



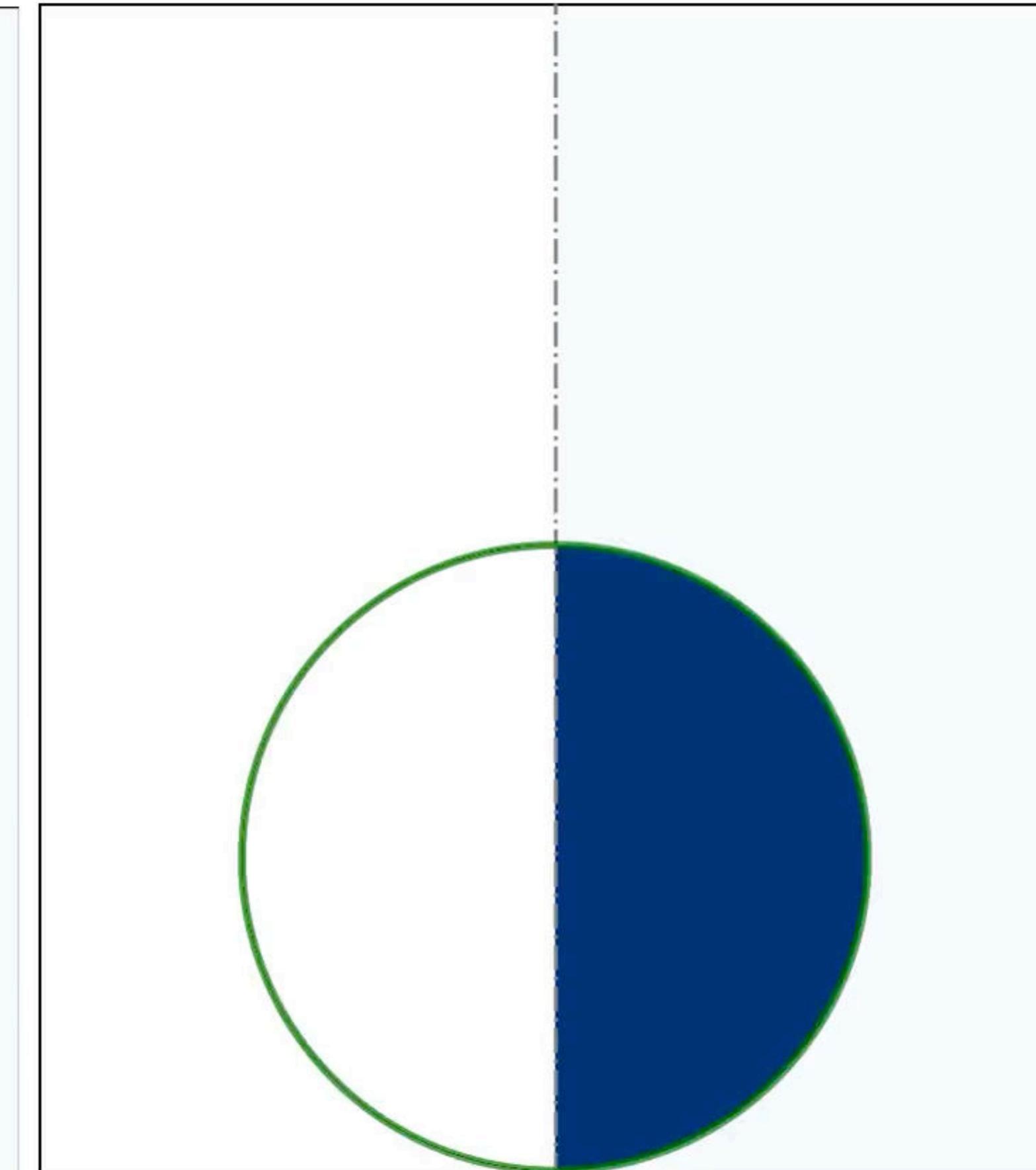
Singular jet & bubble

$We = 9$

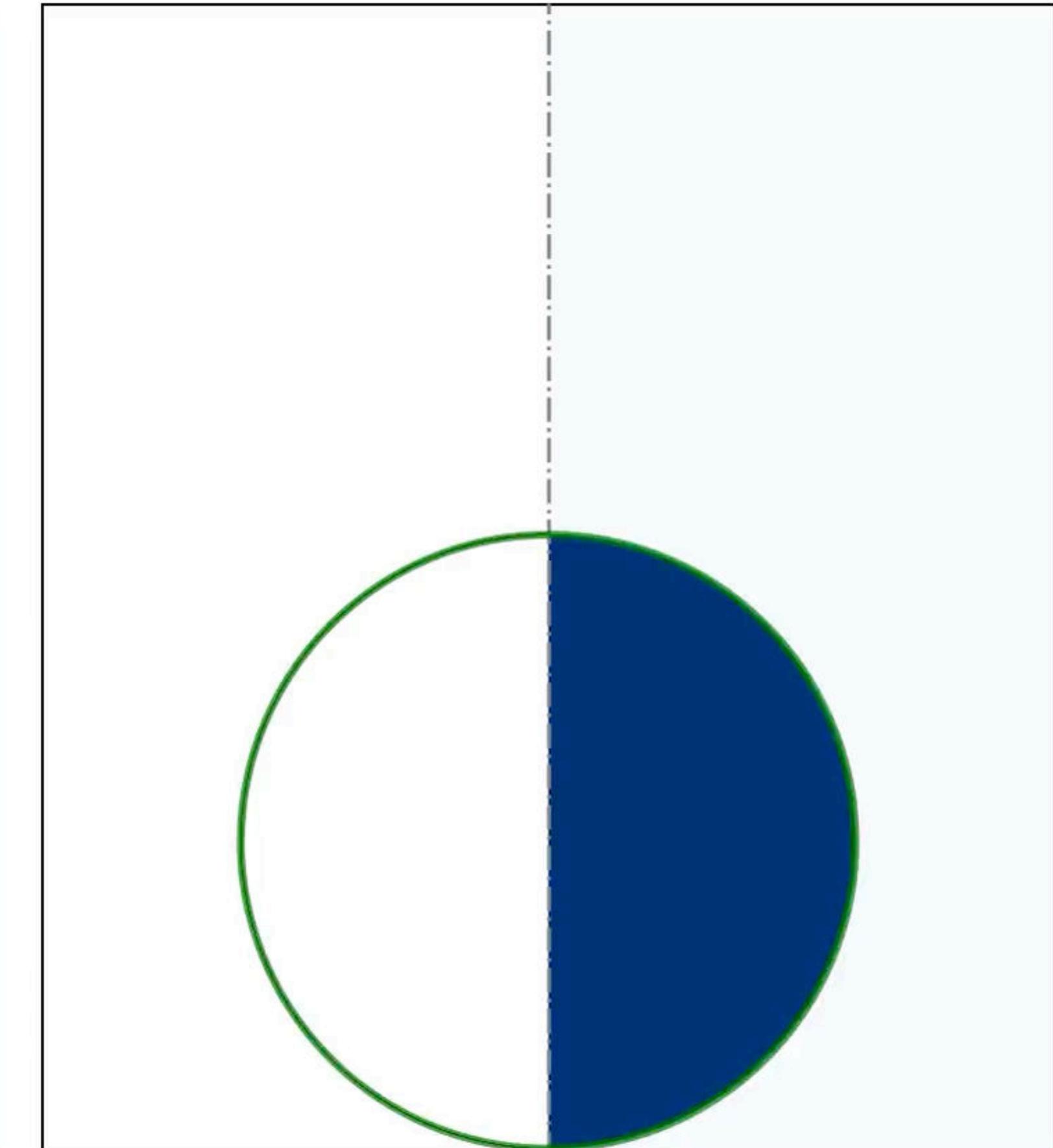
$V_0 t / D_0 = 0.000$



$Oh = 0.0025$



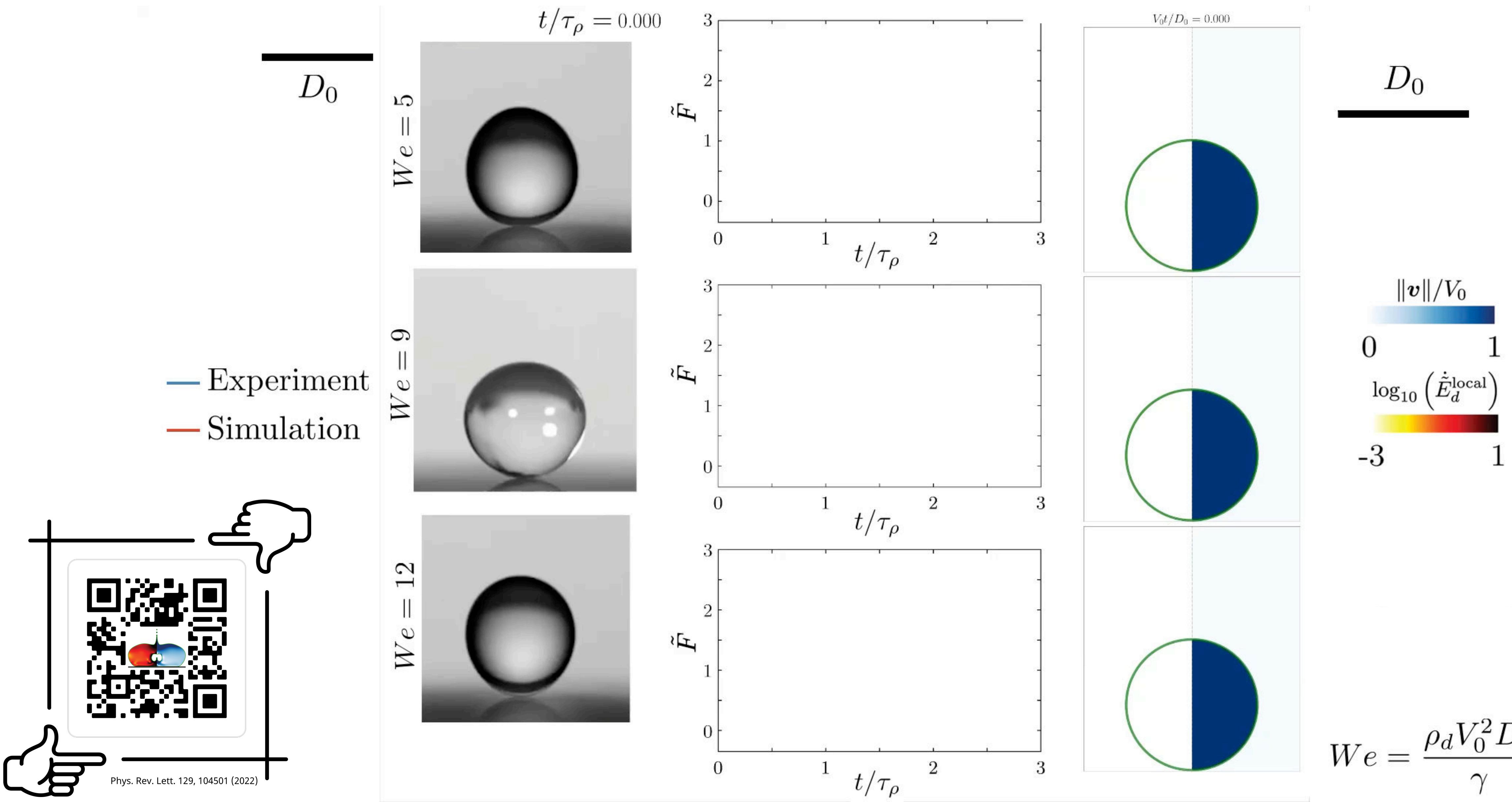
$Oh = 0.005$

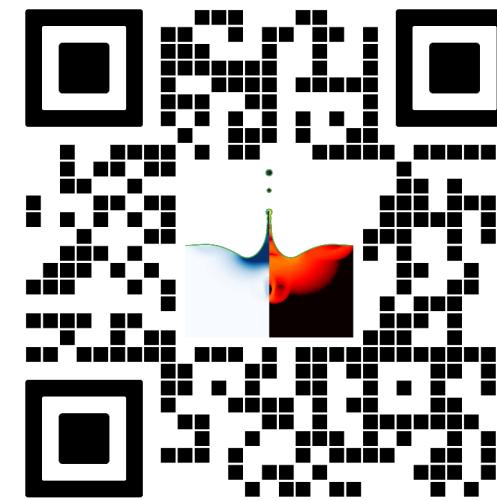


$Oh = 0.05$

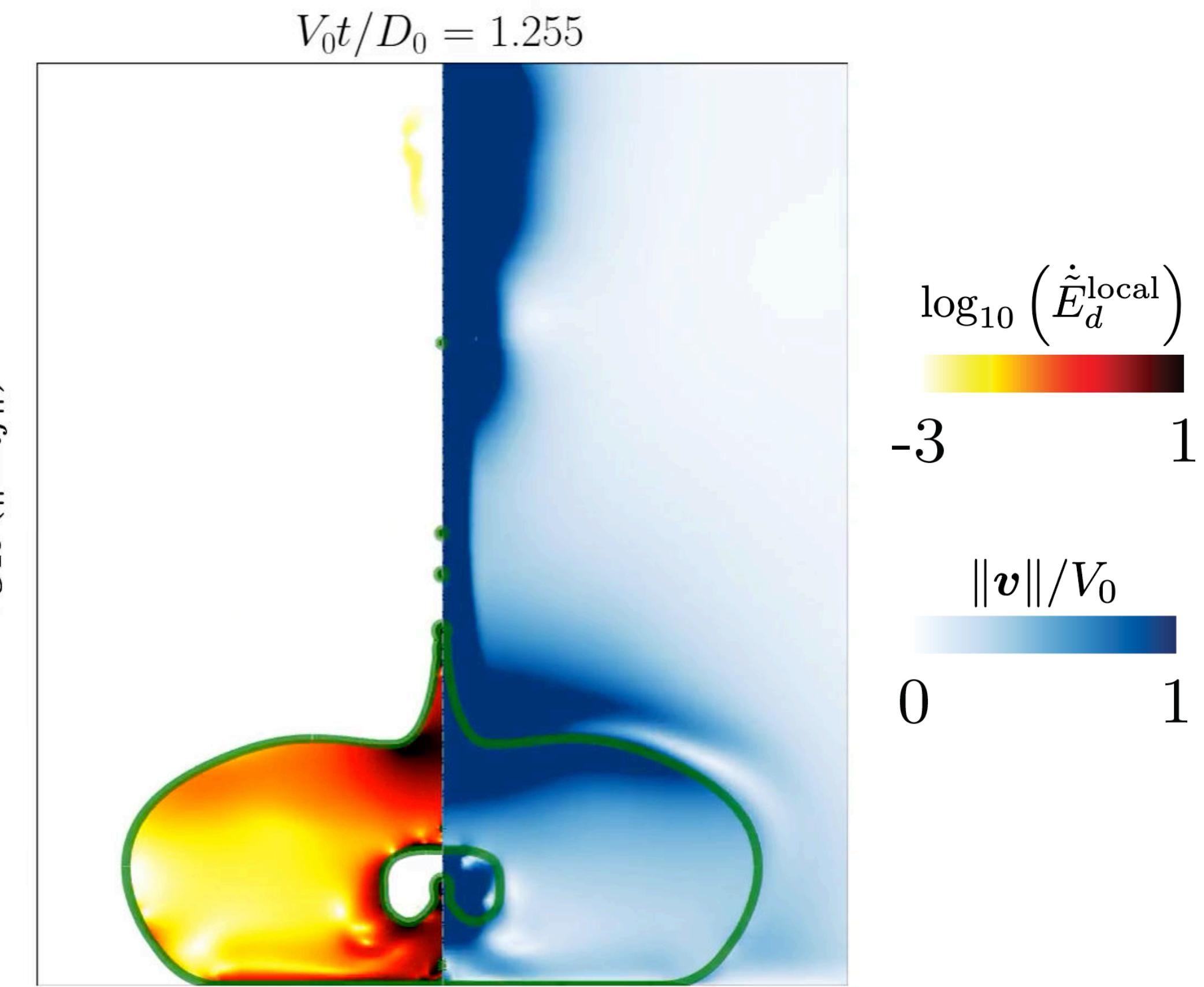
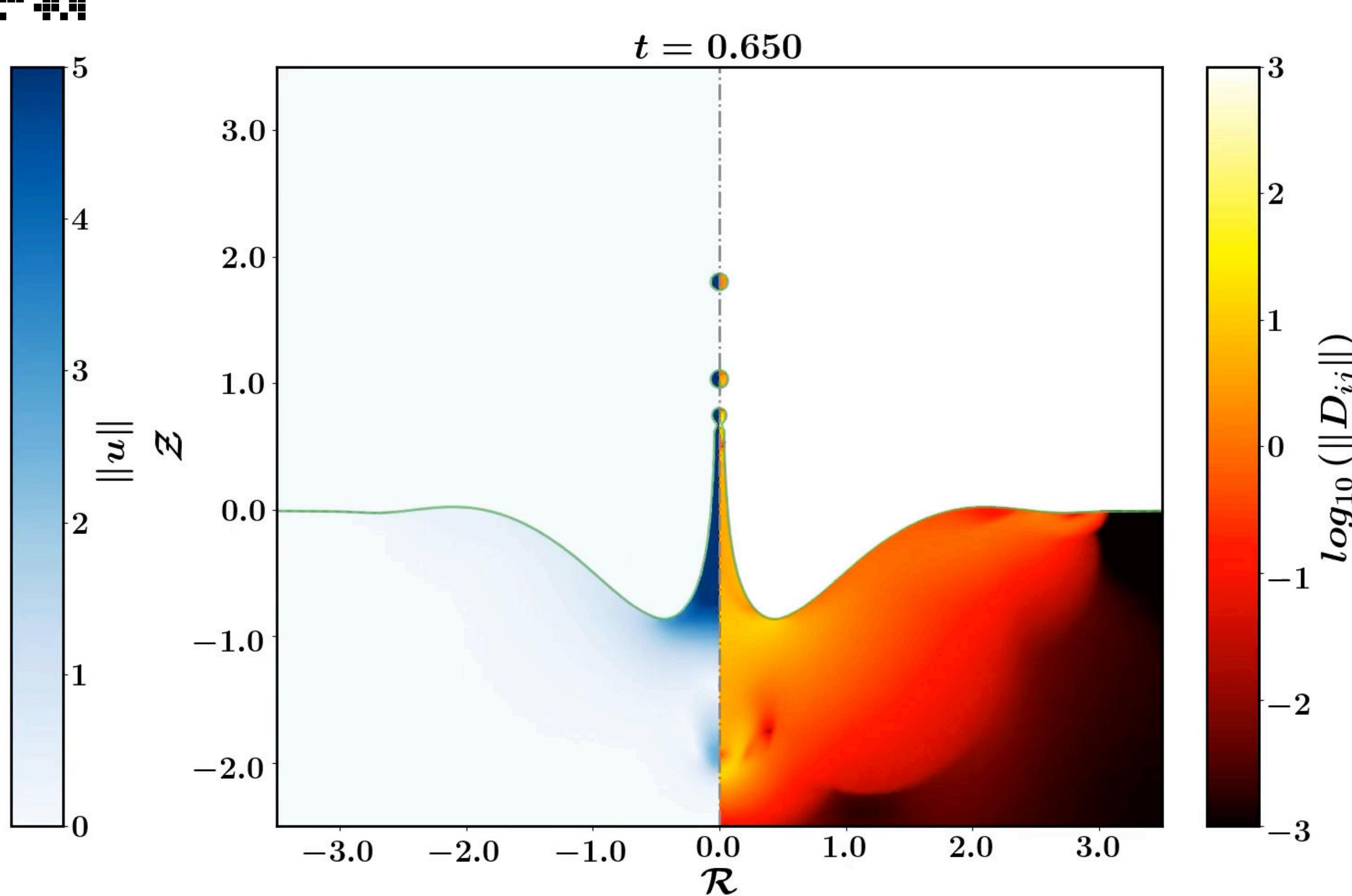
II. What about the impact conditions?

Bubble entrainment regime is very narrow $We \approx 9$





Throwback Friday: Worthington jets

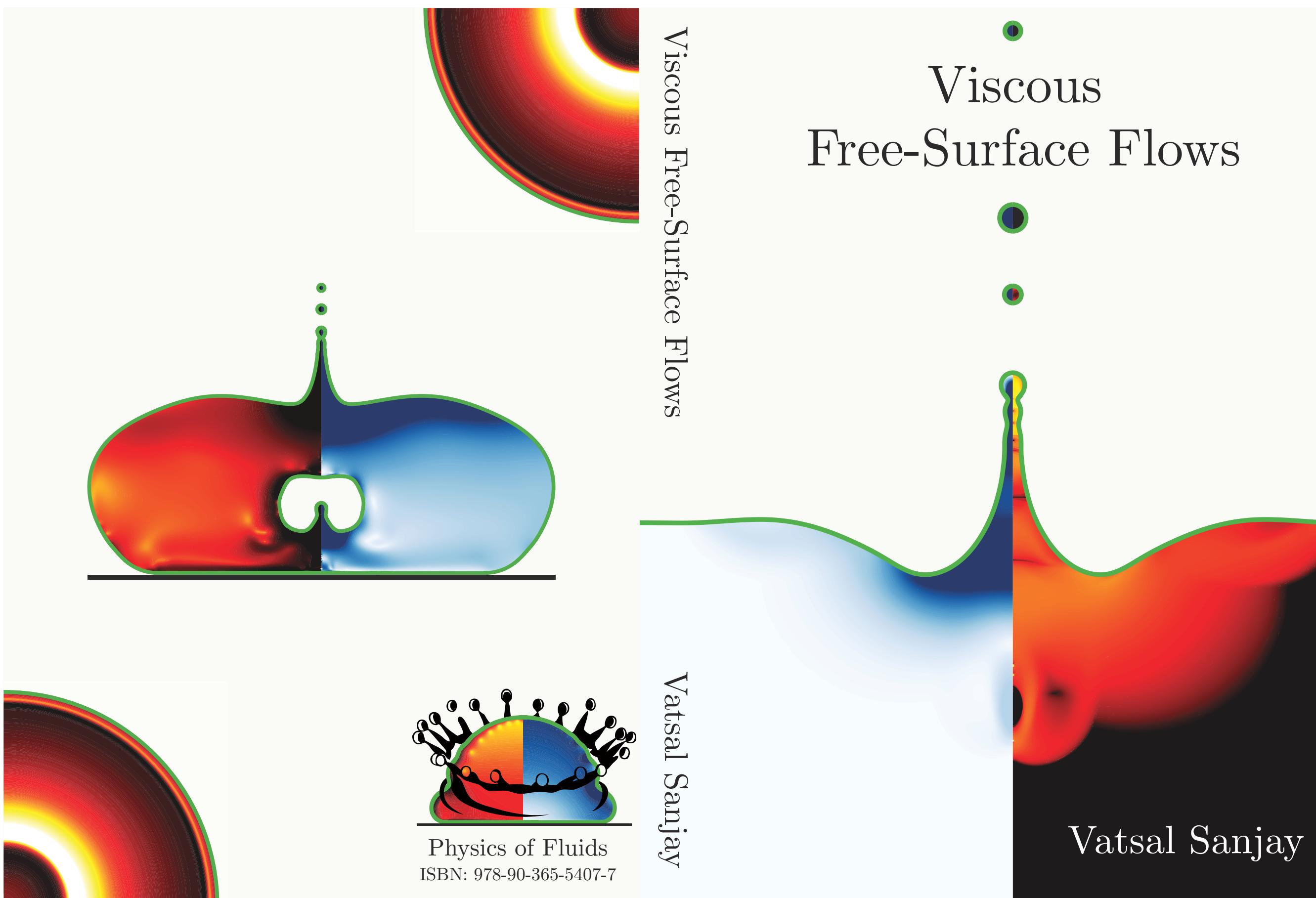


BGUM 2019

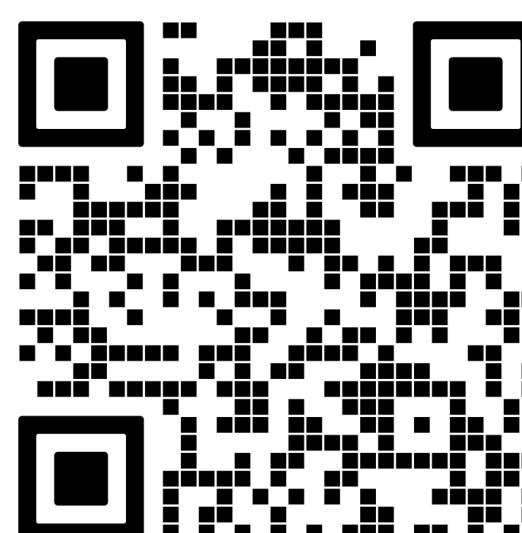
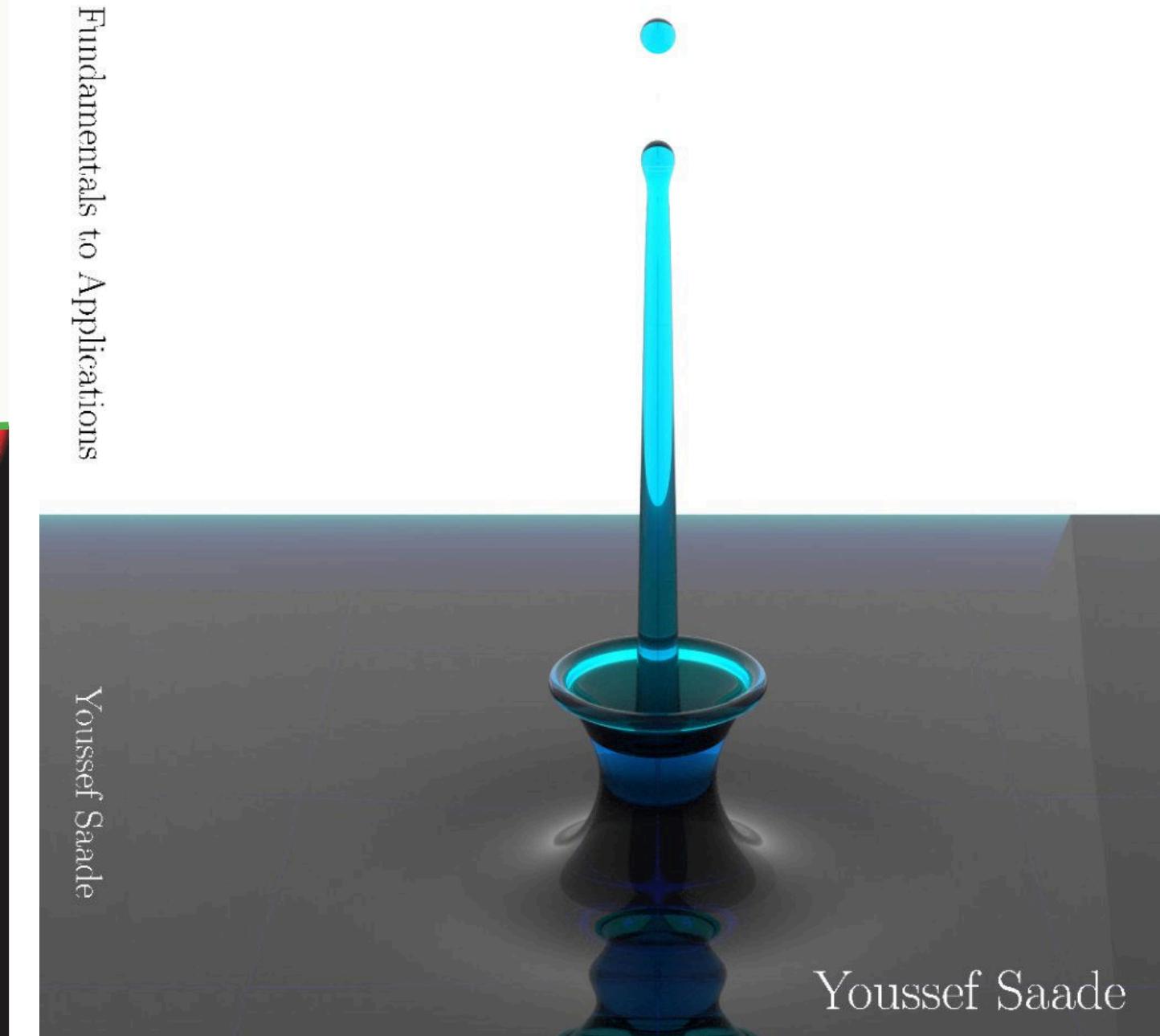
BGUM 2023



Worthington-type jets in the last 4 years

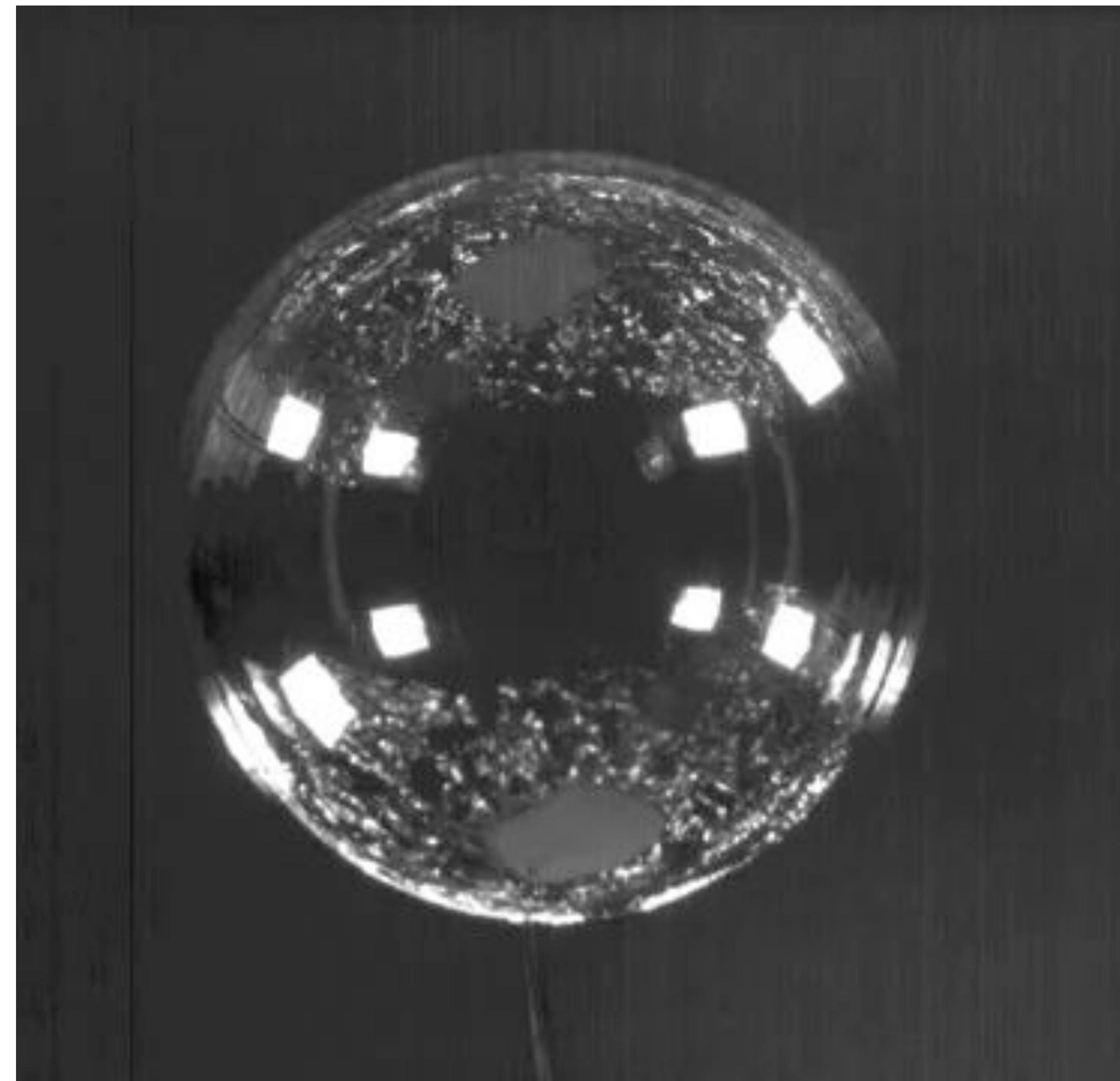


Drops & Bubbles:
From Fundamentals to Applications

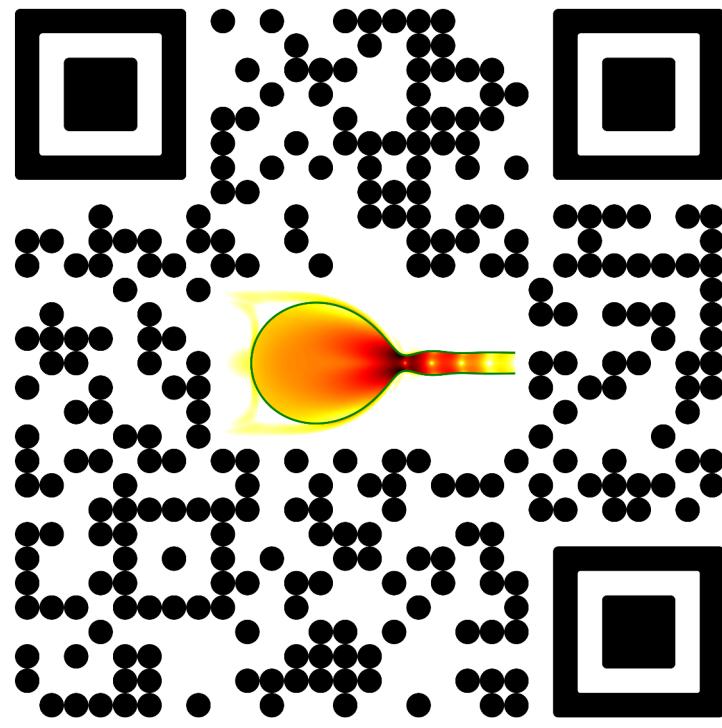


More free-surface flows

(Another) Real life examples



Video from <https://fyfluidynamics.com/2011/10/high-speed-video-of-a-soap-bubble-being-popped/>



Taylor-Culick Retractions

Detlef Lohse

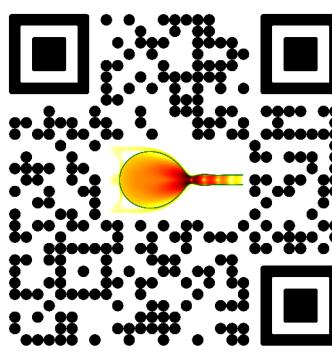


Udo Sen



Pallav Kant



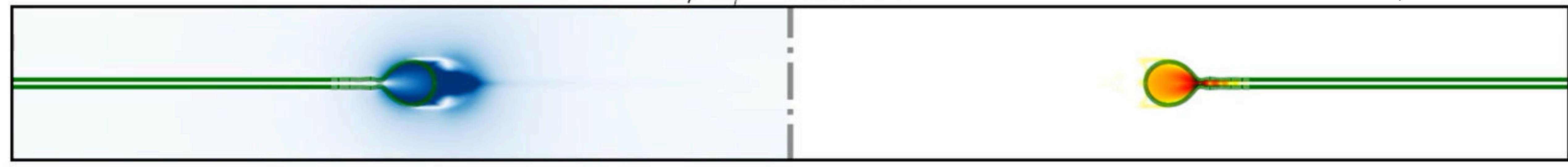


Classical Taylor-Culick retraction

$$Oh_f = 0.05$$

$$t/\tau_\gamma = 50.500$$

$$Oh = \frac{\eta}{\sqrt{\rho_f(2\gamma_{af})h_0}}$$



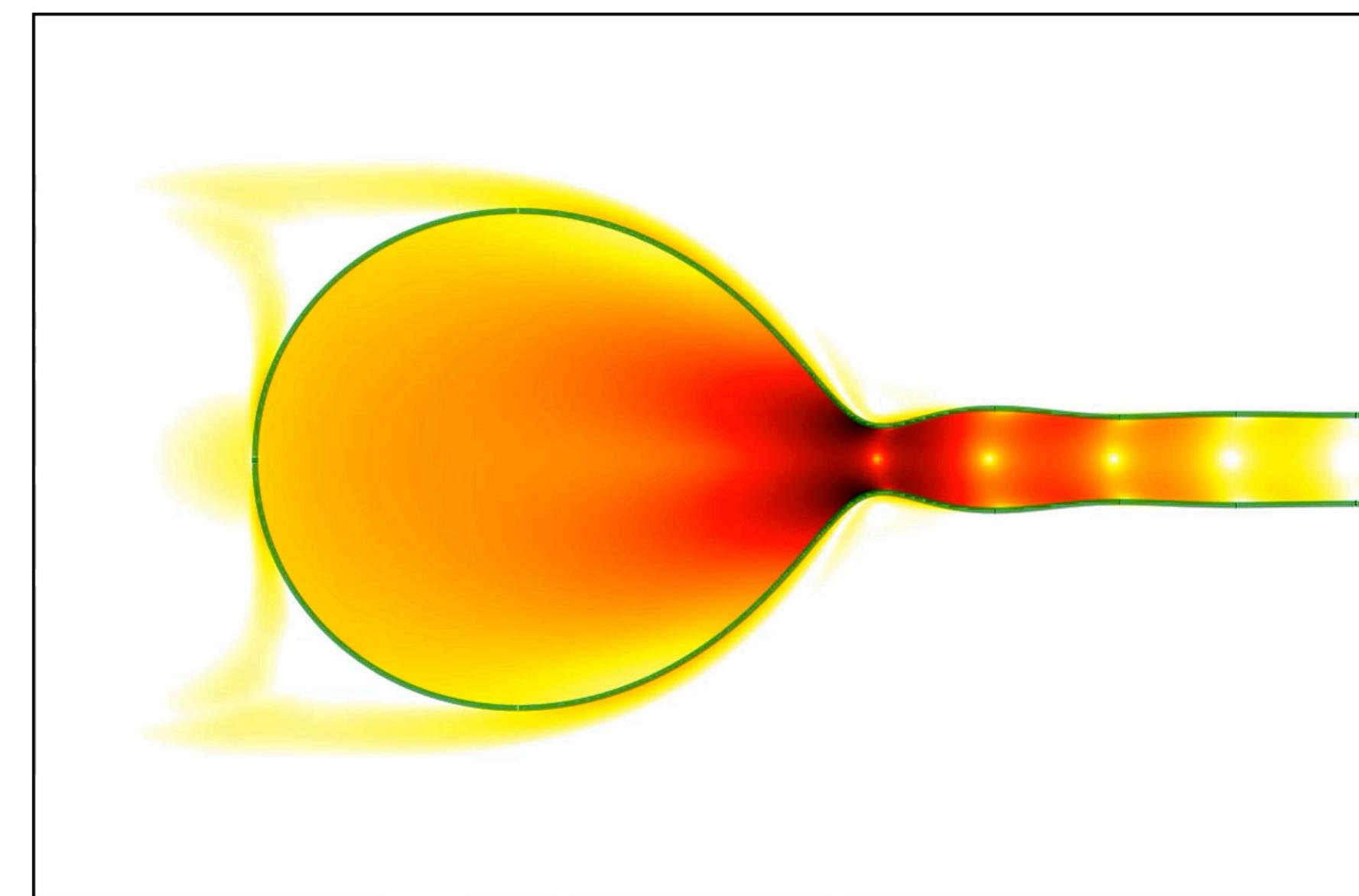
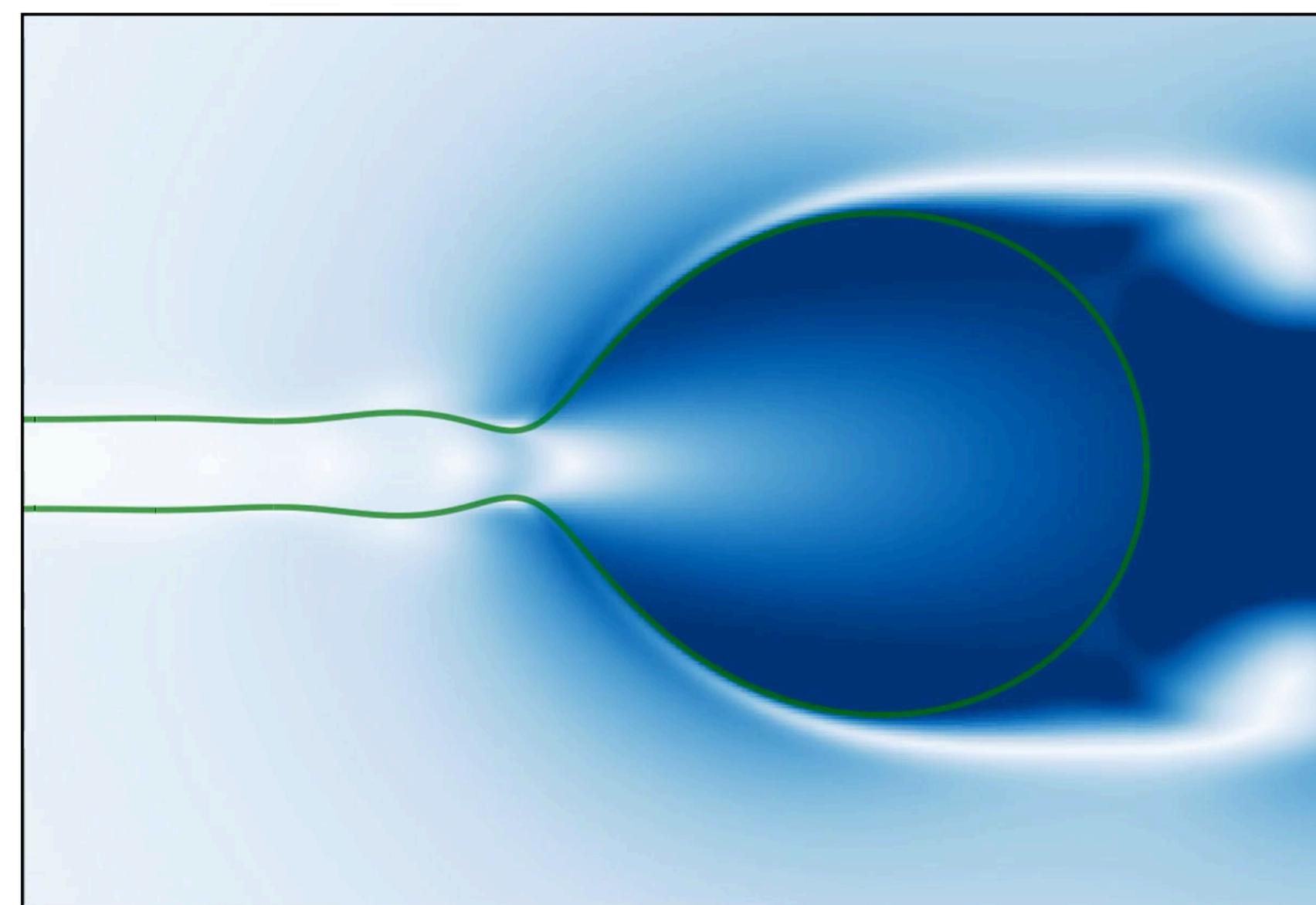
0 1

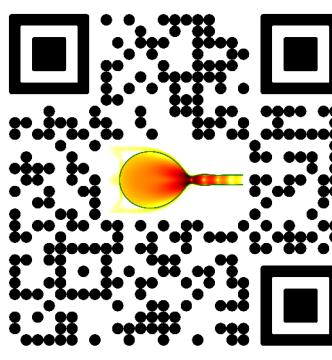
$$\|\boldsymbol{v}\|/v_\gamma$$

$$-\log_{10} (2Oh (\mathcal{D} : \mathcal{D}) \tau_\gamma^2)$$

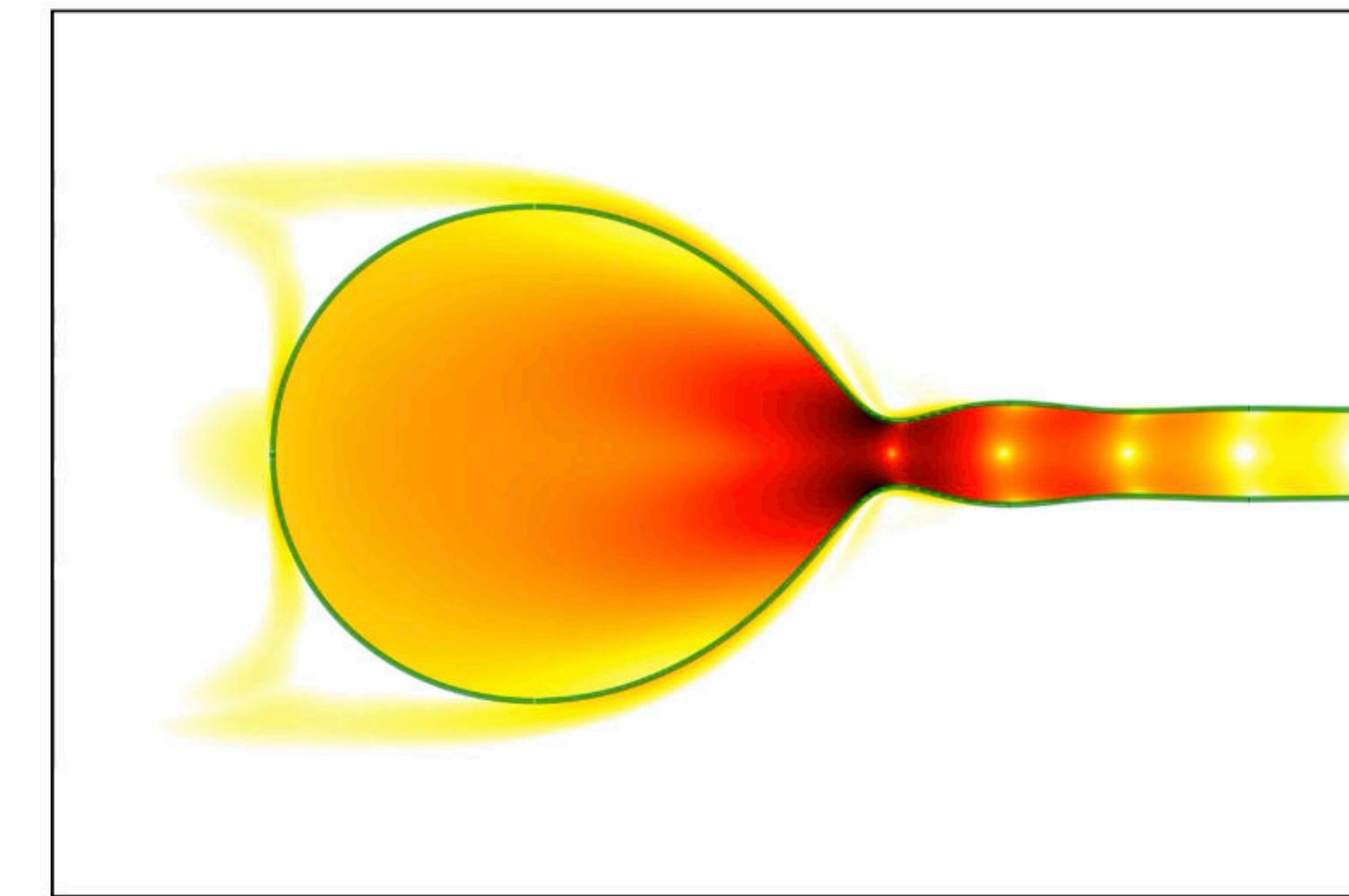
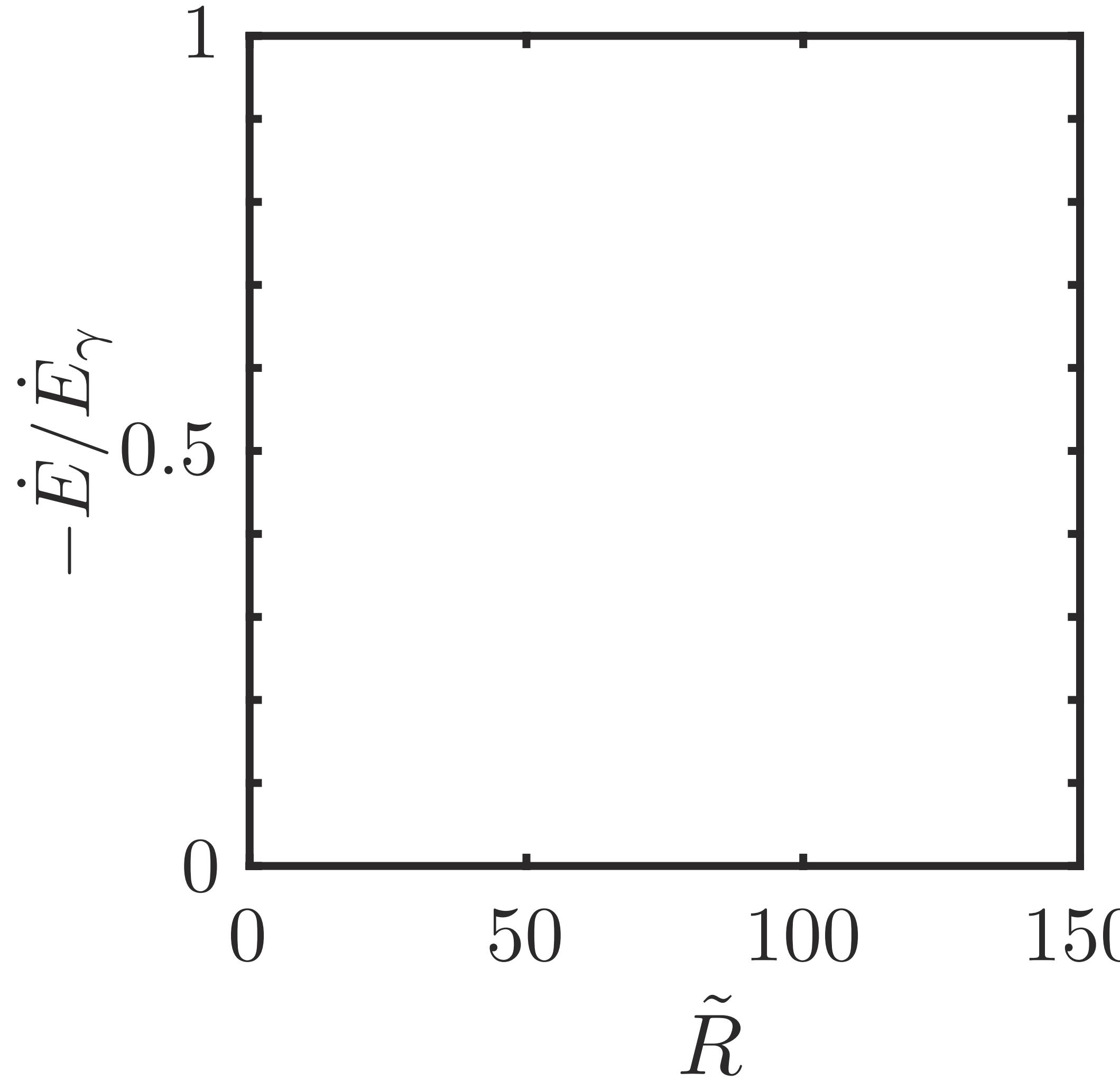
$$\mathcal{D} = \left(\nabla \boldsymbol{v} + (\nabla \boldsymbol{v})^T \right) / 2$$

$$\tau_\gamma = \sqrt{\frac{\rho_f h_0^3}{2\gamma_{af}}} \quad v_\gamma = \sqrt{\frac{2\gamma_{af}}{\rho_f h_0}}$$

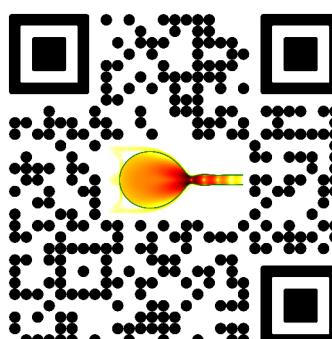




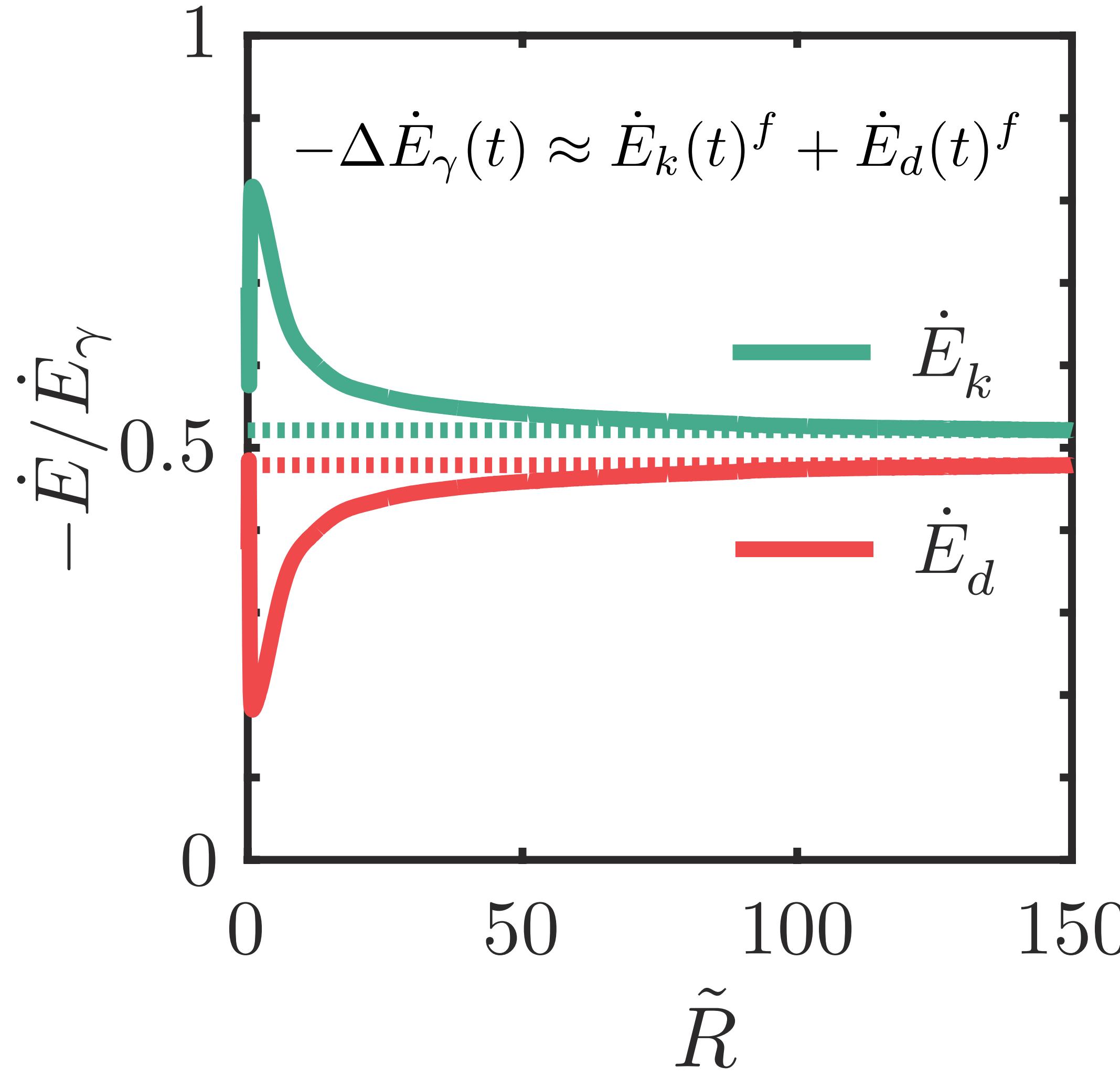
Energy Budget: Classical Taylor-Culick retraction



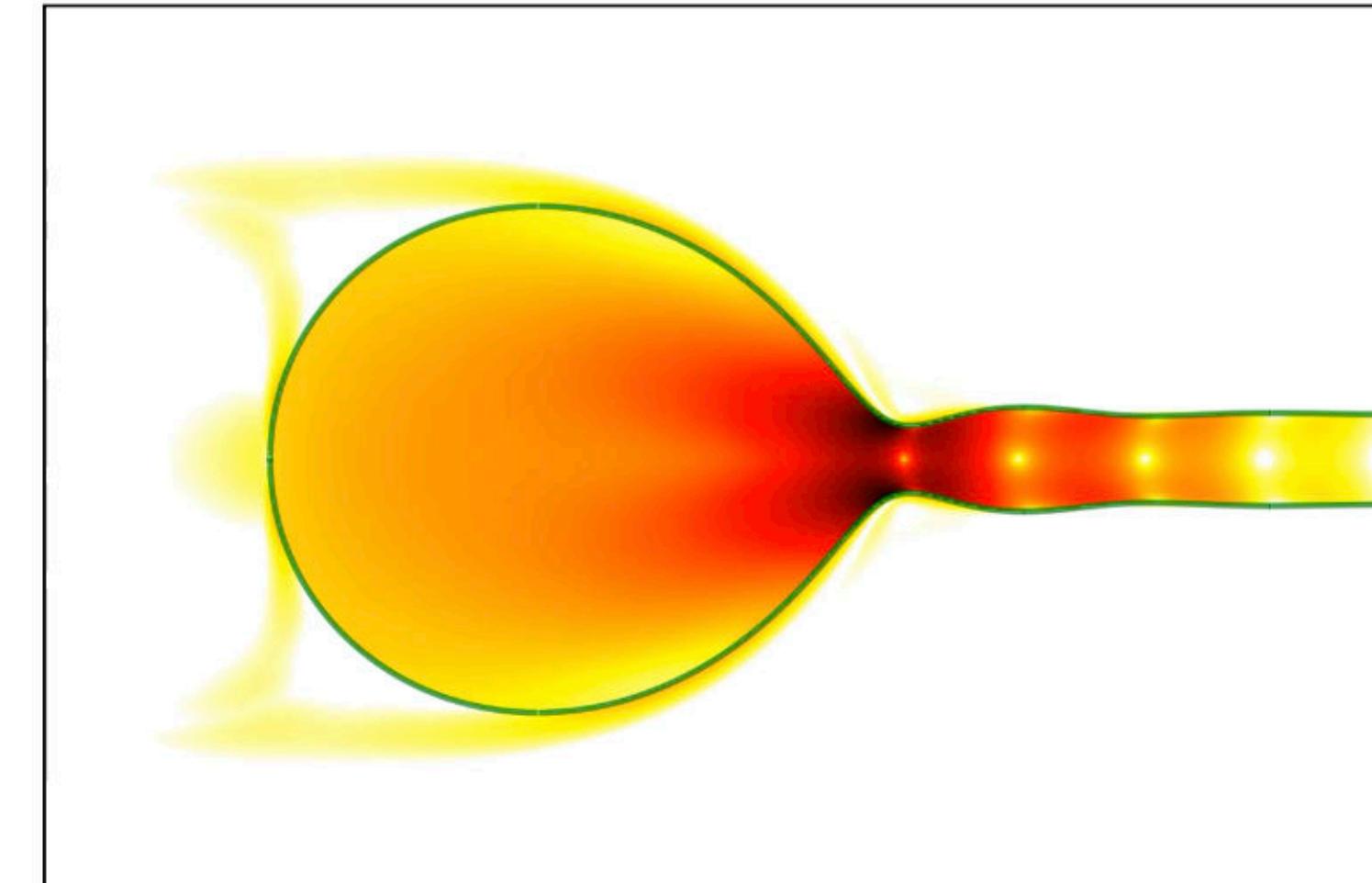
$$\log_{10} (2O \hbar (\mathcal{D} : \mathcal{D}) \tau_\gamma^2)$$



Energy Budget: Classical Taylor-Culick retraction



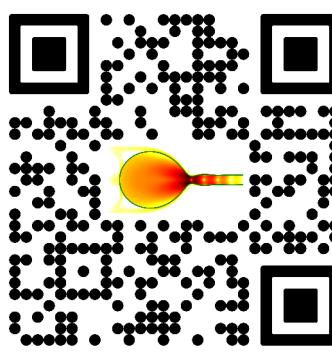
$$\dot{E}_d = \frac{1}{2} \frac{dm}{dt} v^2$$



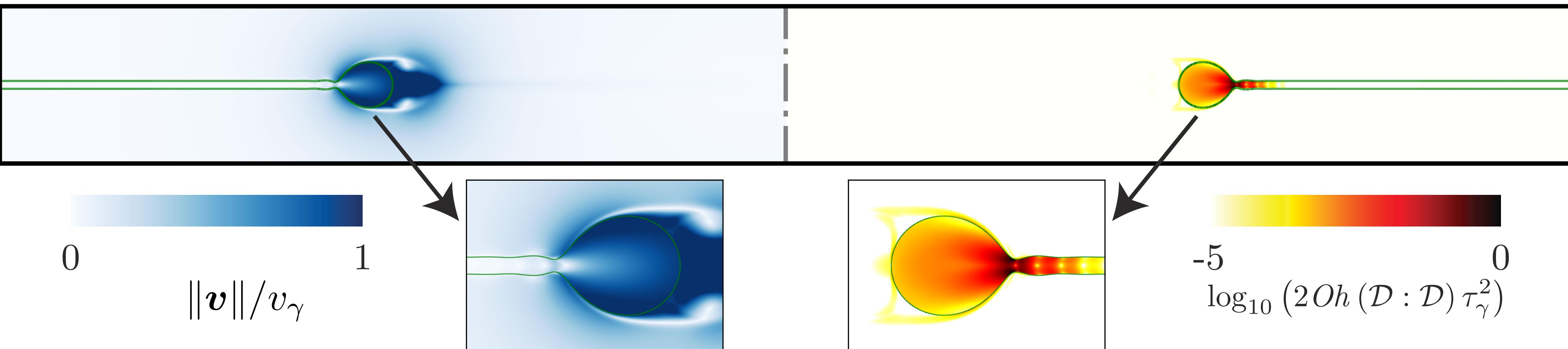
G. I. Taylor

F. E. C. Culick

P.-G. de Gennes



Synopsis of Classical Taylor-Culick retractions

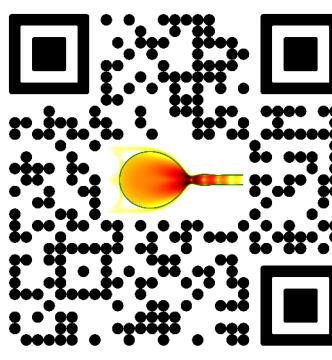


- Even in the inertial limit, cannot neglect viscous dissipation in the thin film
- Dissipation is independent of viscosity.

$$v_f = v_{TC} = \sqrt{\frac{(2\gamma_{fa})}{\rho_f h_0}}$$

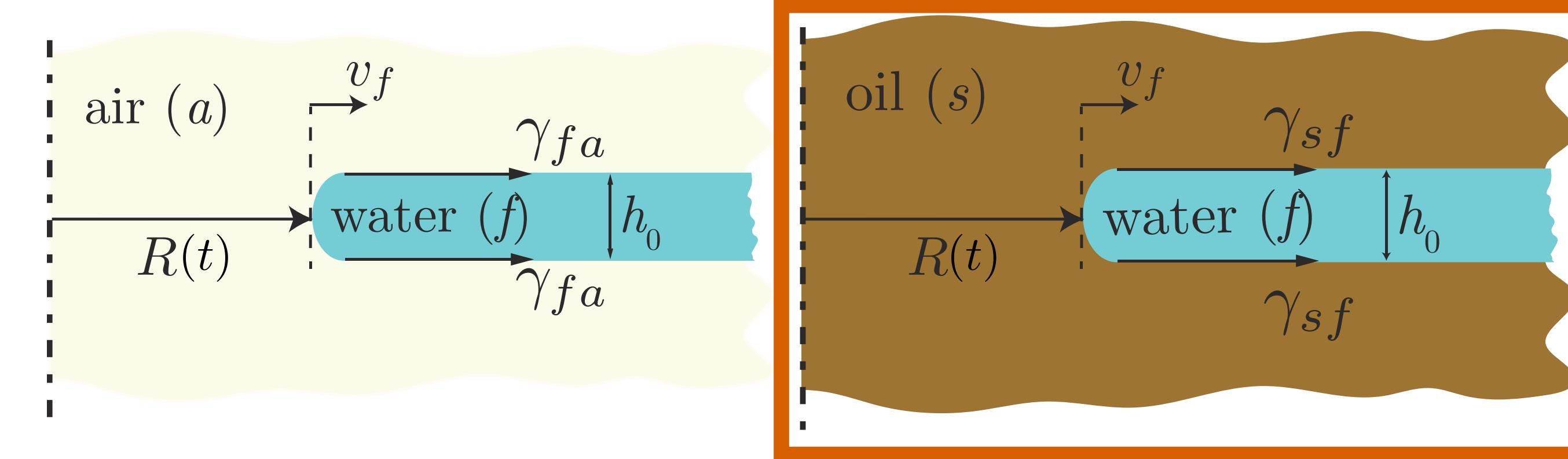
$$-\Delta \dot{E}_\gamma(t) \approx \dot{E}_k(t)^f + \dot{E}_d(t)^f$$

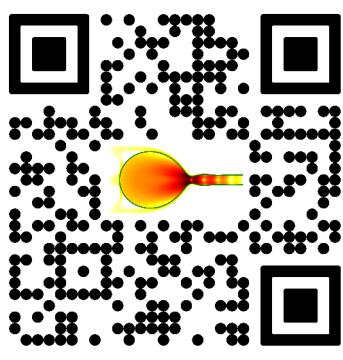
$$\dot{E}_d = \frac{1}{2} \frac{dm}{dt} v^2$$



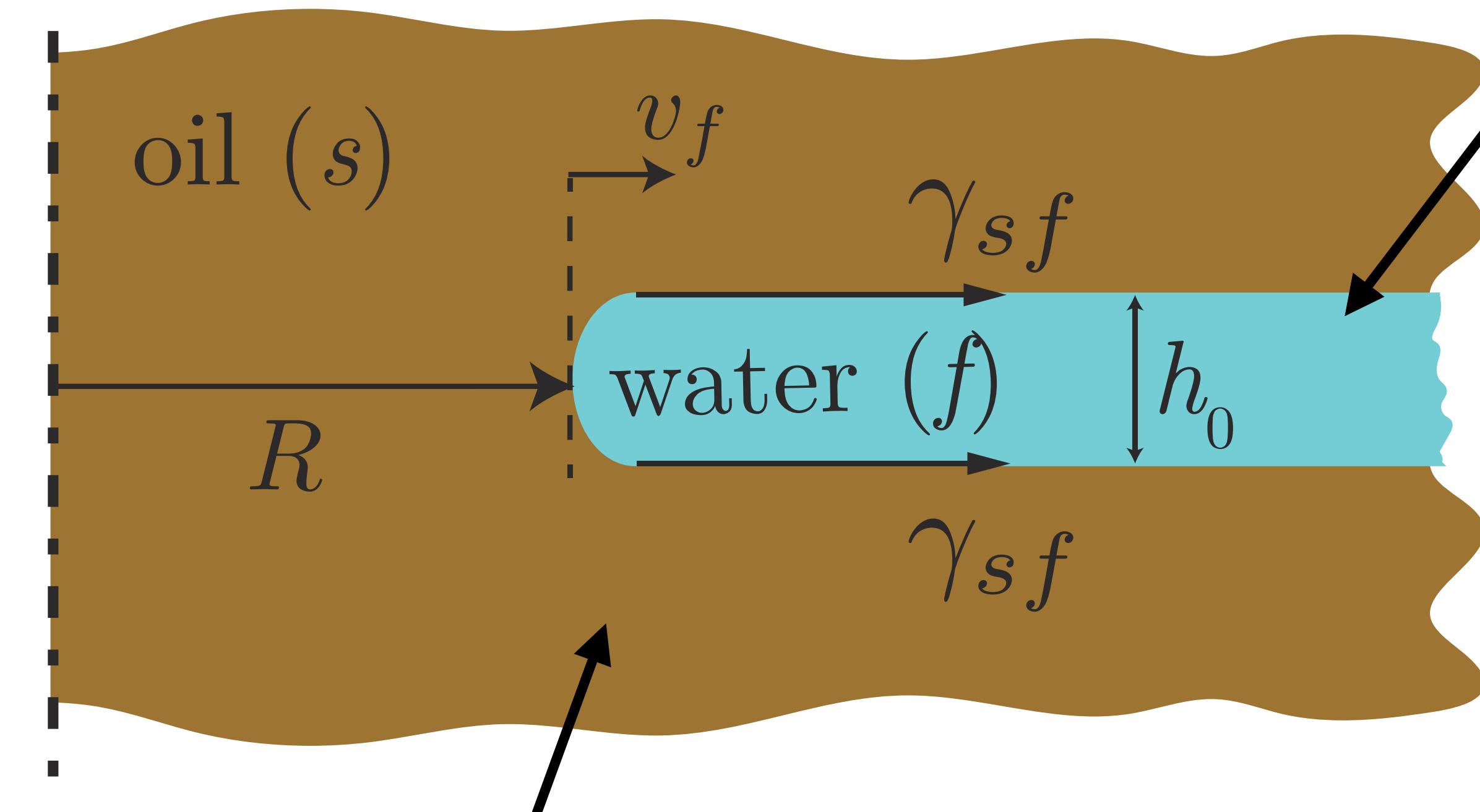
Beyond the free-surface ...

What happens if the surrounding medium is not air?





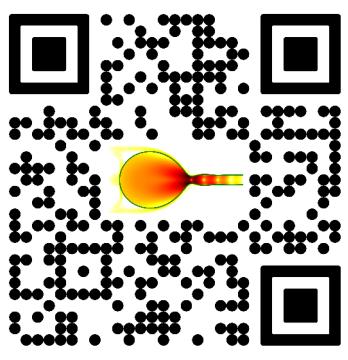
Problem Statement



$$Oh_s = \frac{\eta_s}{\sqrt{\rho_f (2\gamma_{fs}) h_0}}$$

$$Oh_f = \frac{\eta_f}{\sqrt{\rho_f (2\gamma_{fs}) h_0}}$$





Retraction in viscous environment: Inertial limit

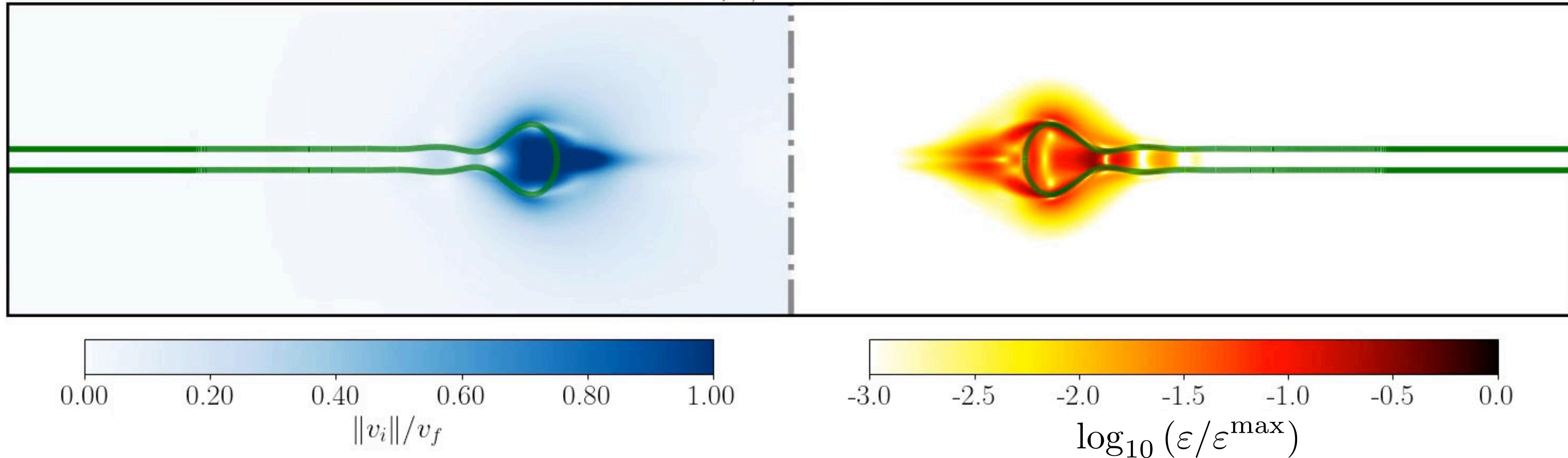
Control Parameters:

$$Oh_s = \frac{\eta_s}{\sqrt{\rho_f (2\gamma_{fs})} h_0}$$

$$Oh_f = \frac{\eta_f}{\sqrt{\rho_f (2\gamma_{fs})} h_0}$$

$$Oh_f = 0.03 \quad Oh_s = 0.01$$

$$t/t_\gamma = 20.500$$

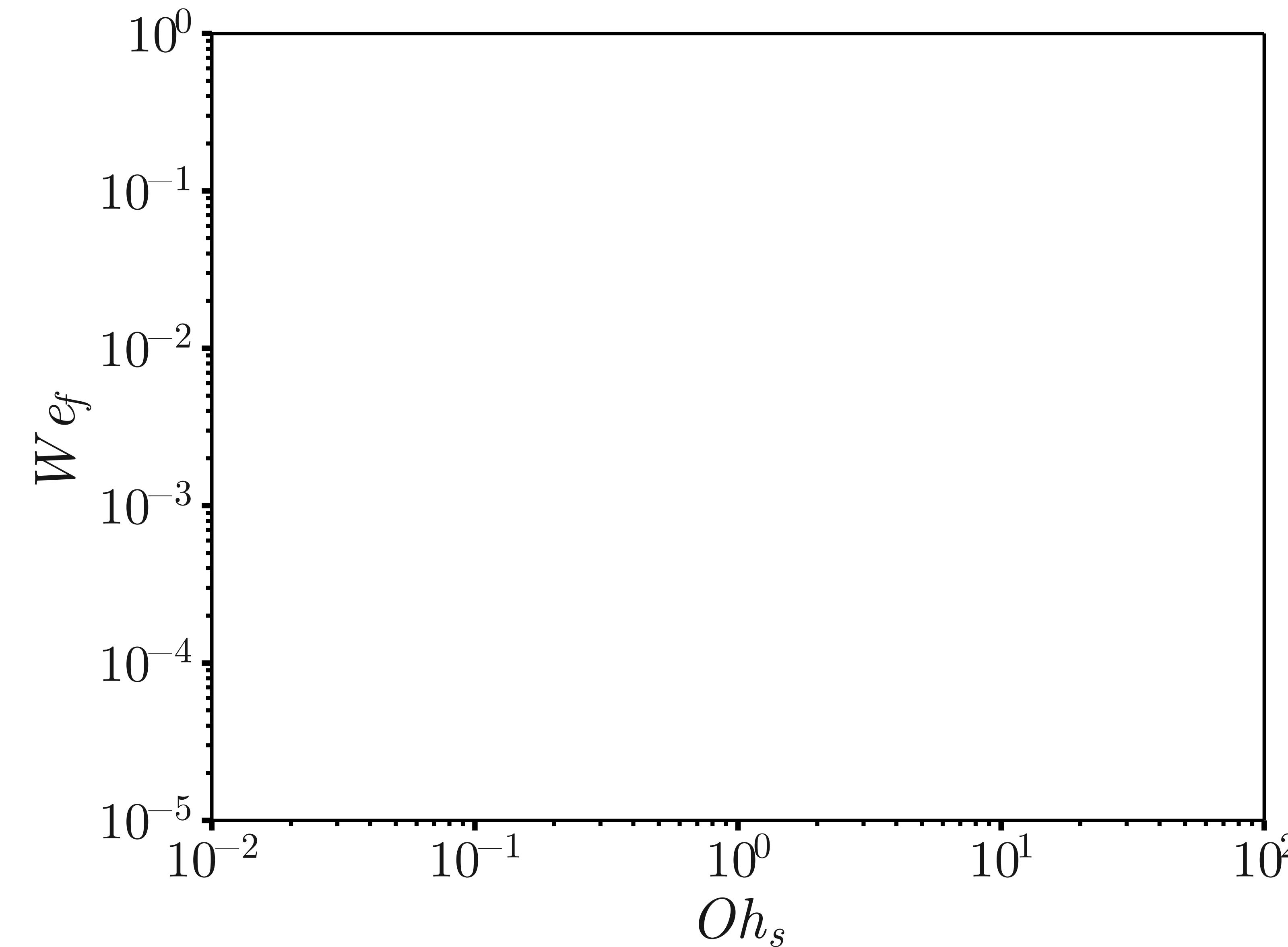
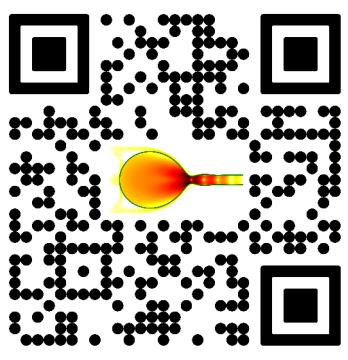


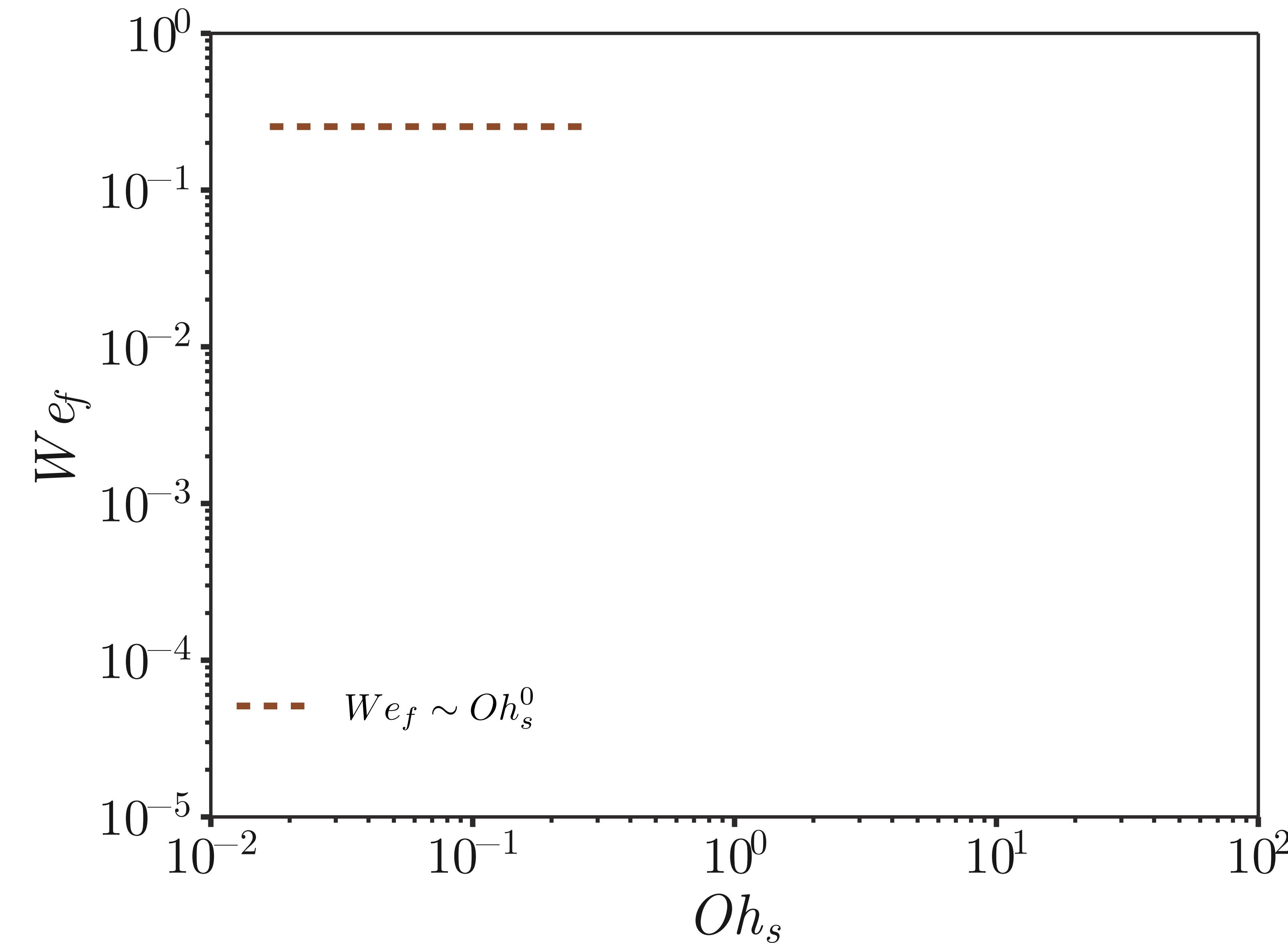
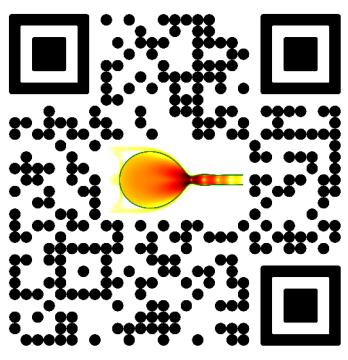
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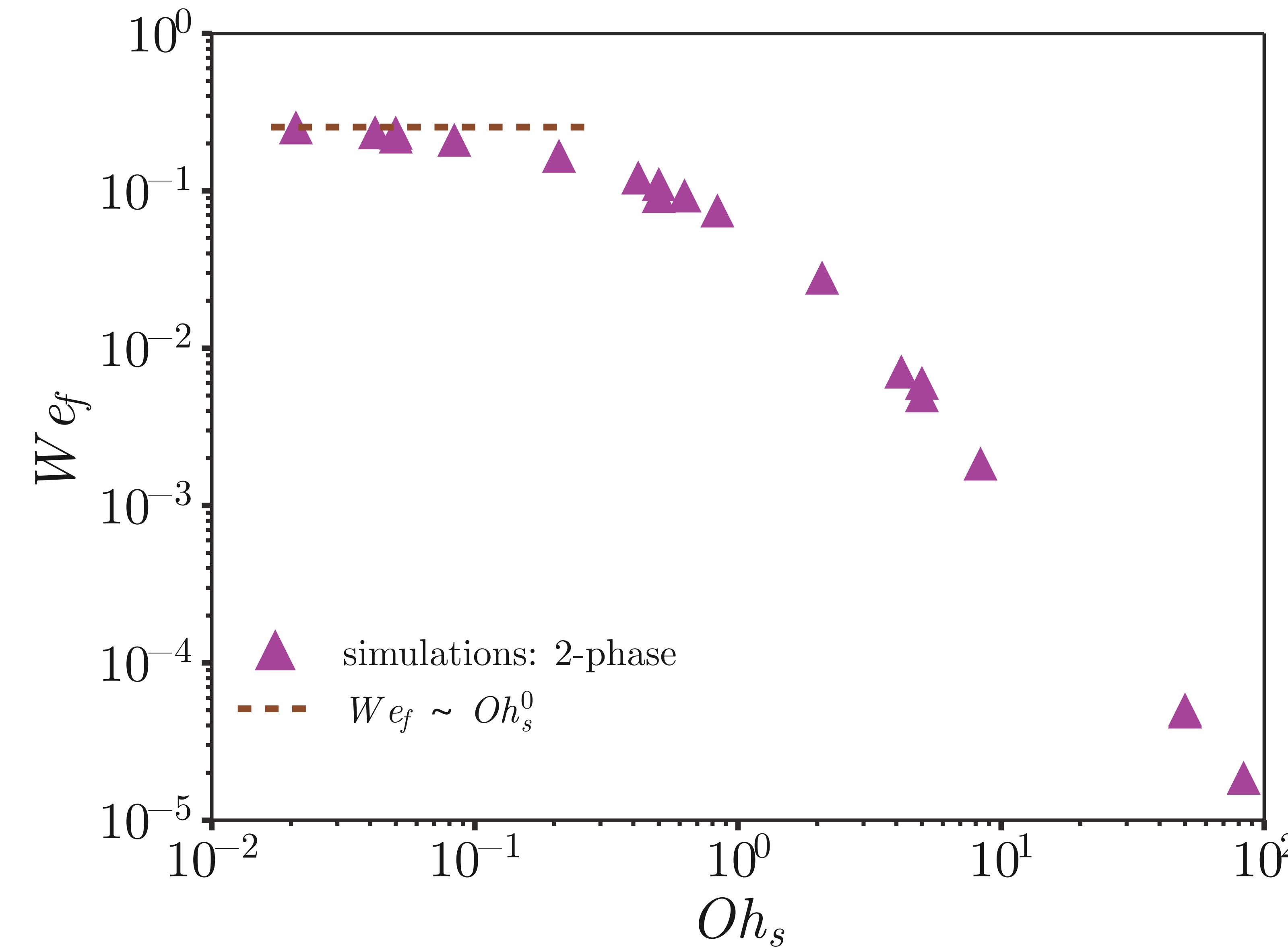
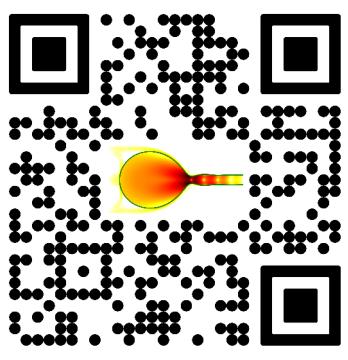
$$We_f = \frac{\rho_f v_f^2 h_0}{2\gamma_{fs}}$$

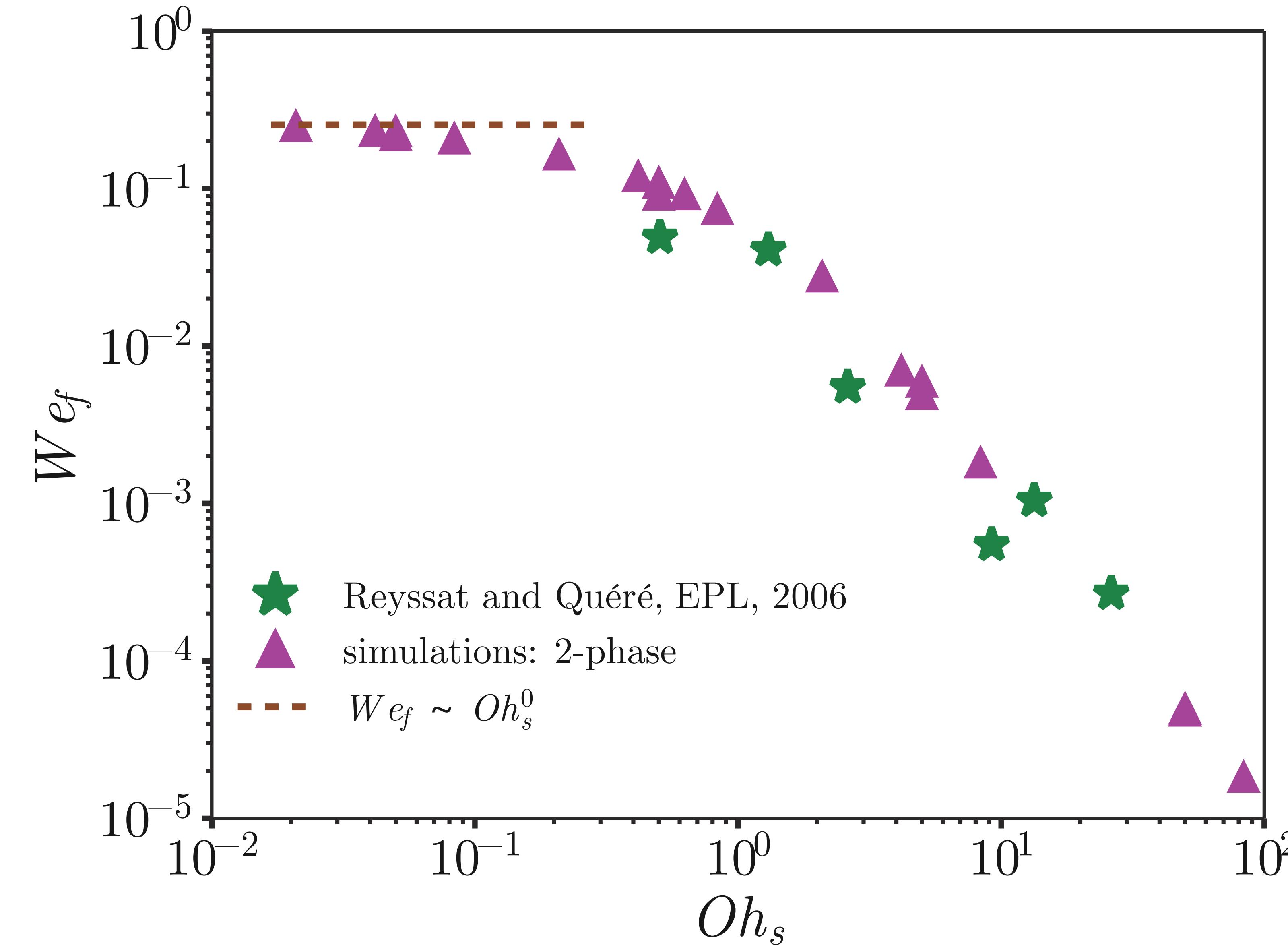
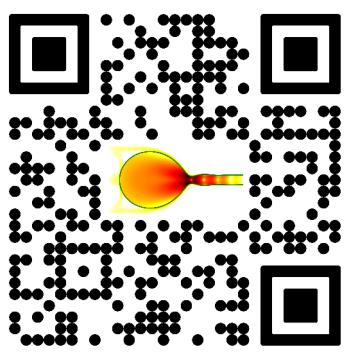
$$\varepsilon = 2\eta \mathcal{D}_{ij} \mathcal{D}_{ij}$$

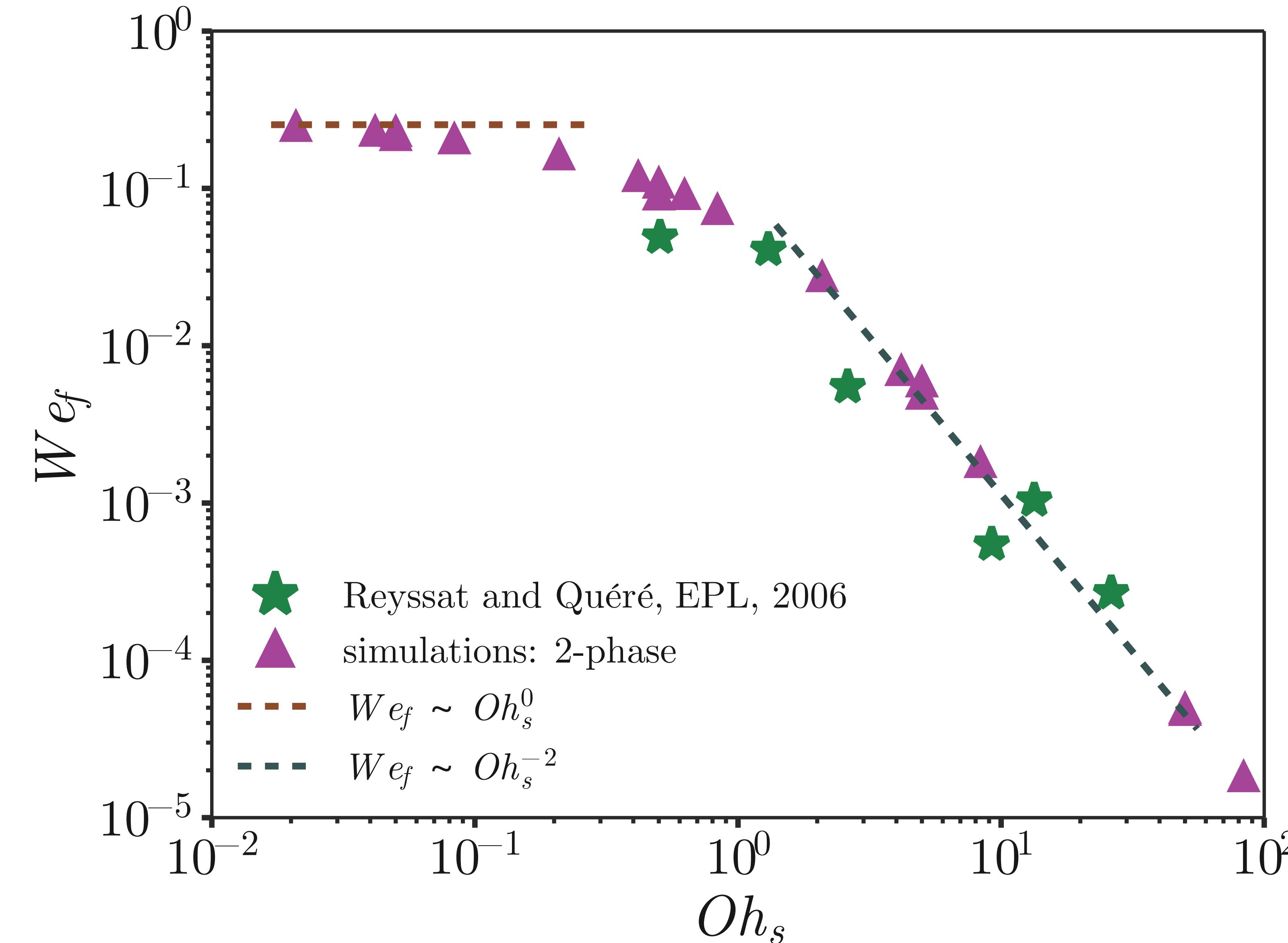
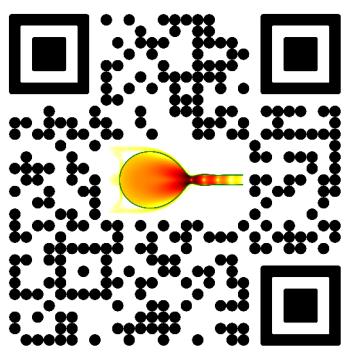
$$\mathcal{D}_{ij} = \frac{1}{2}(\partial_j V_i + \partial_i V_j)$$

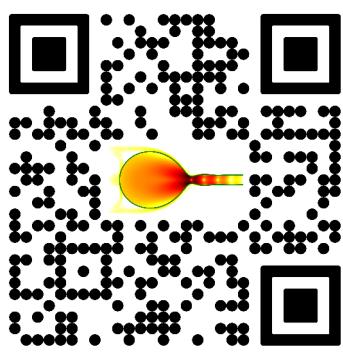










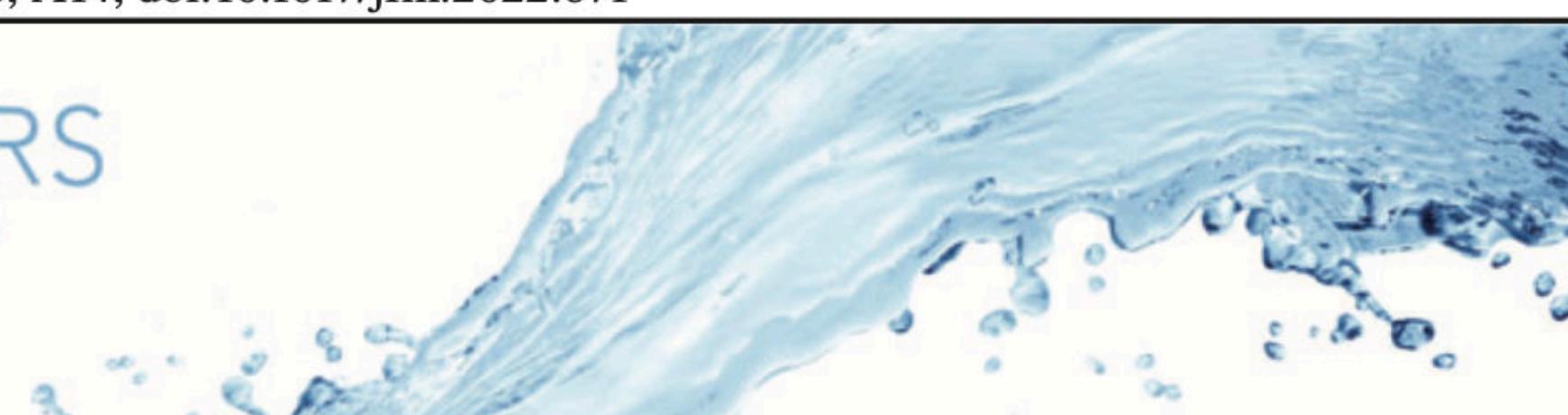


The story continues ...

The story continues ...

J. Fluid Mech. (2022), vol. 948, A14, doi:10.1017/jfm.2022.671

JFM PAPERS



Taylor–Culick retractions and the influence of the surroundings

Vatsal Sanjay^{1,†}, Uddalok Sen^{1,†}, Pallav Kant¹ and Detlef Lohse^{1,2,†}

¹Physics of Fluids Group, Max Planck Center for Complex Fluid Dynamics, Department of Science and Technology, and J. M. Burgers Centre for Fluid Dynamics, University of Twente, P. O. Box 217, 7500 AE Enschede, The Netherlands

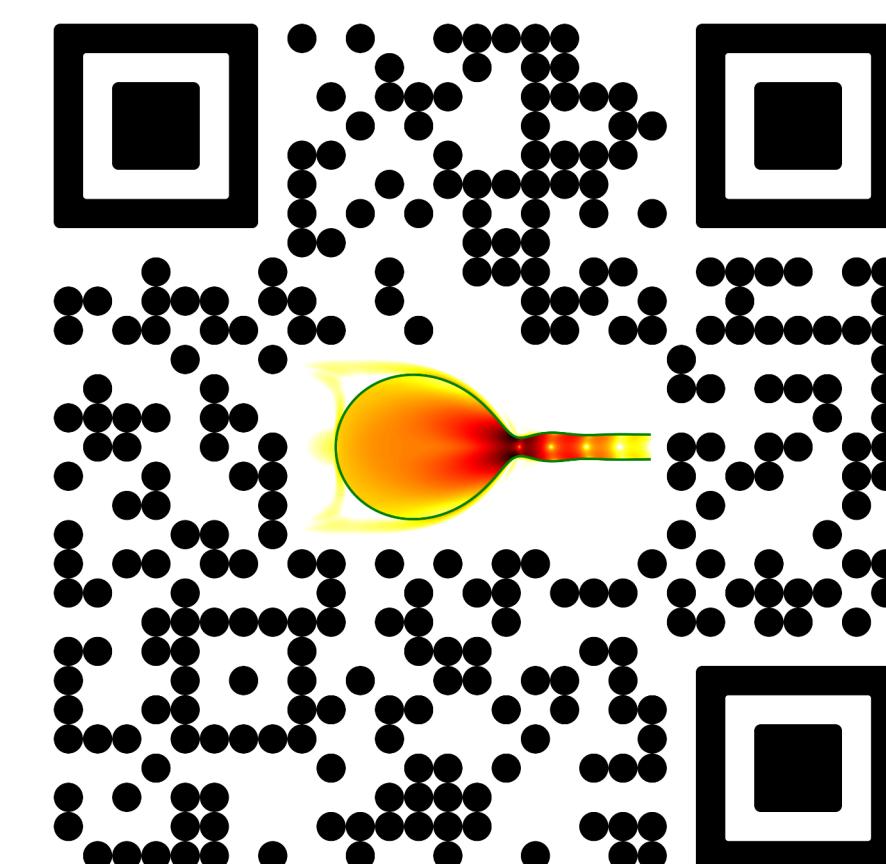
²Max Planck Institute for Dynamics and Self-Organization, Am Fassberg 17, 37077 Göttingen, Germany

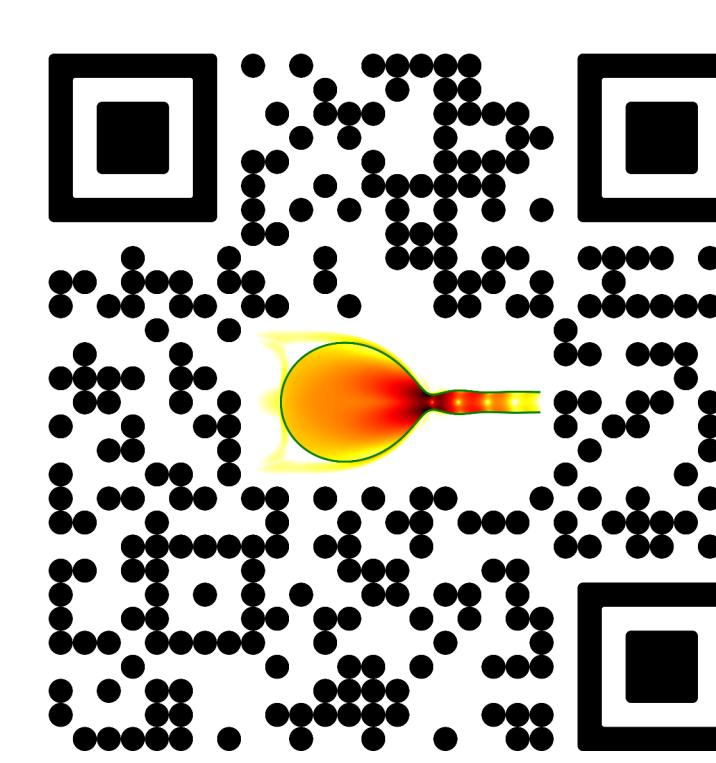
(Received 27 February 2022; revised 29 May 2022; accepted 18 July 2022)

Water films may rupture at the oil-water-air interface, thus dispersing oil droplets further.

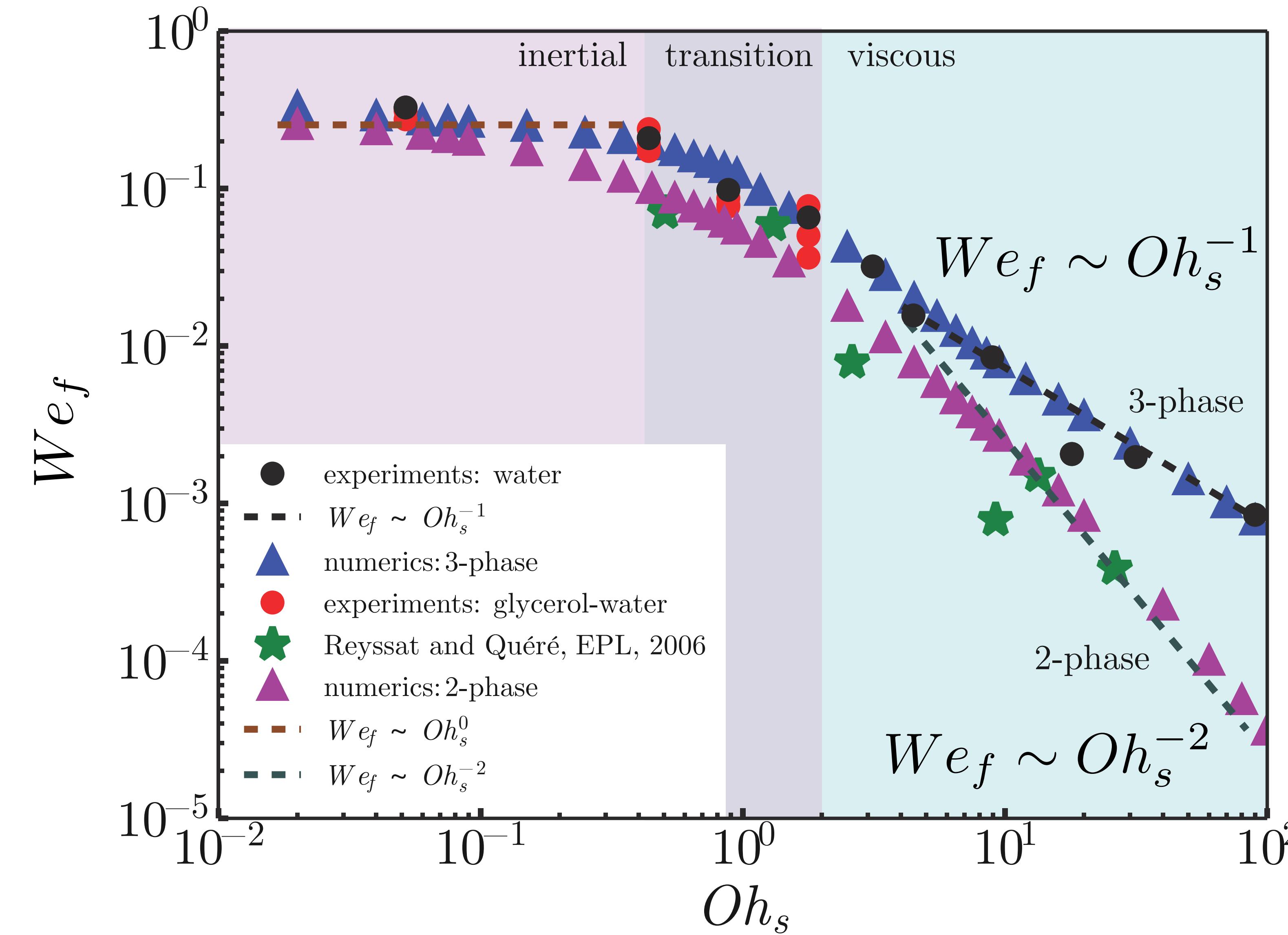


source: physics.stackexchange.com



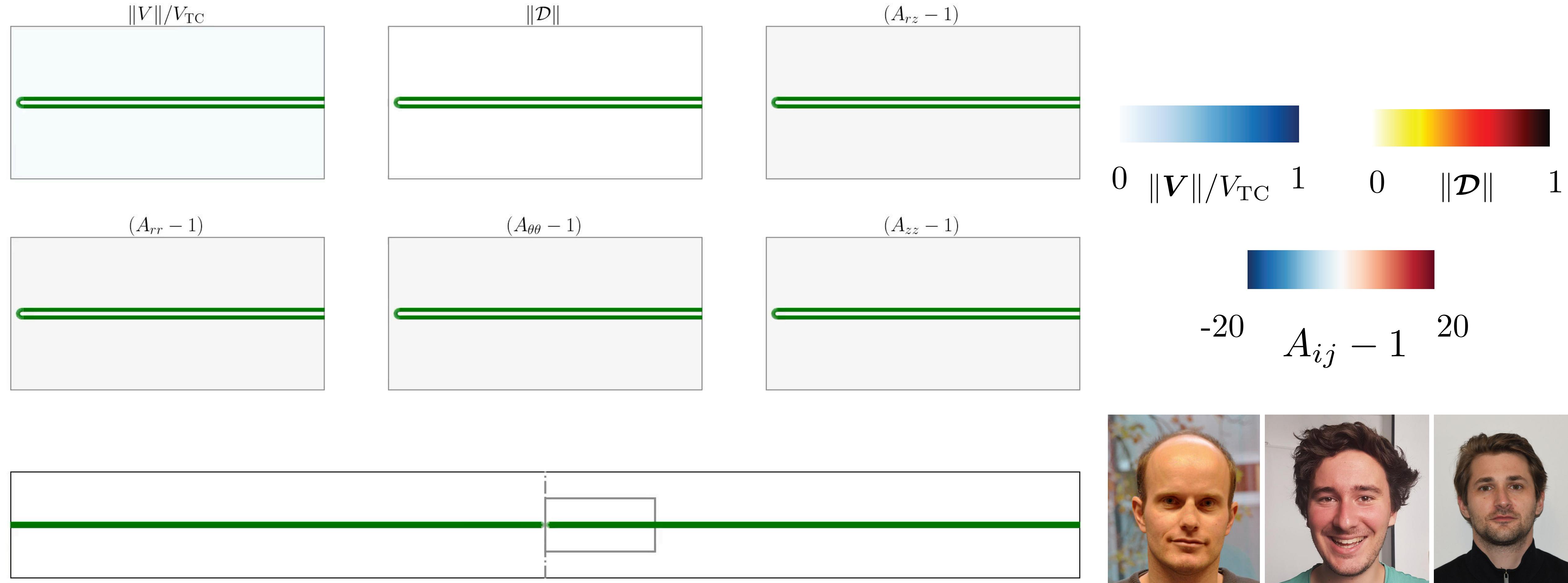


The story continues ...



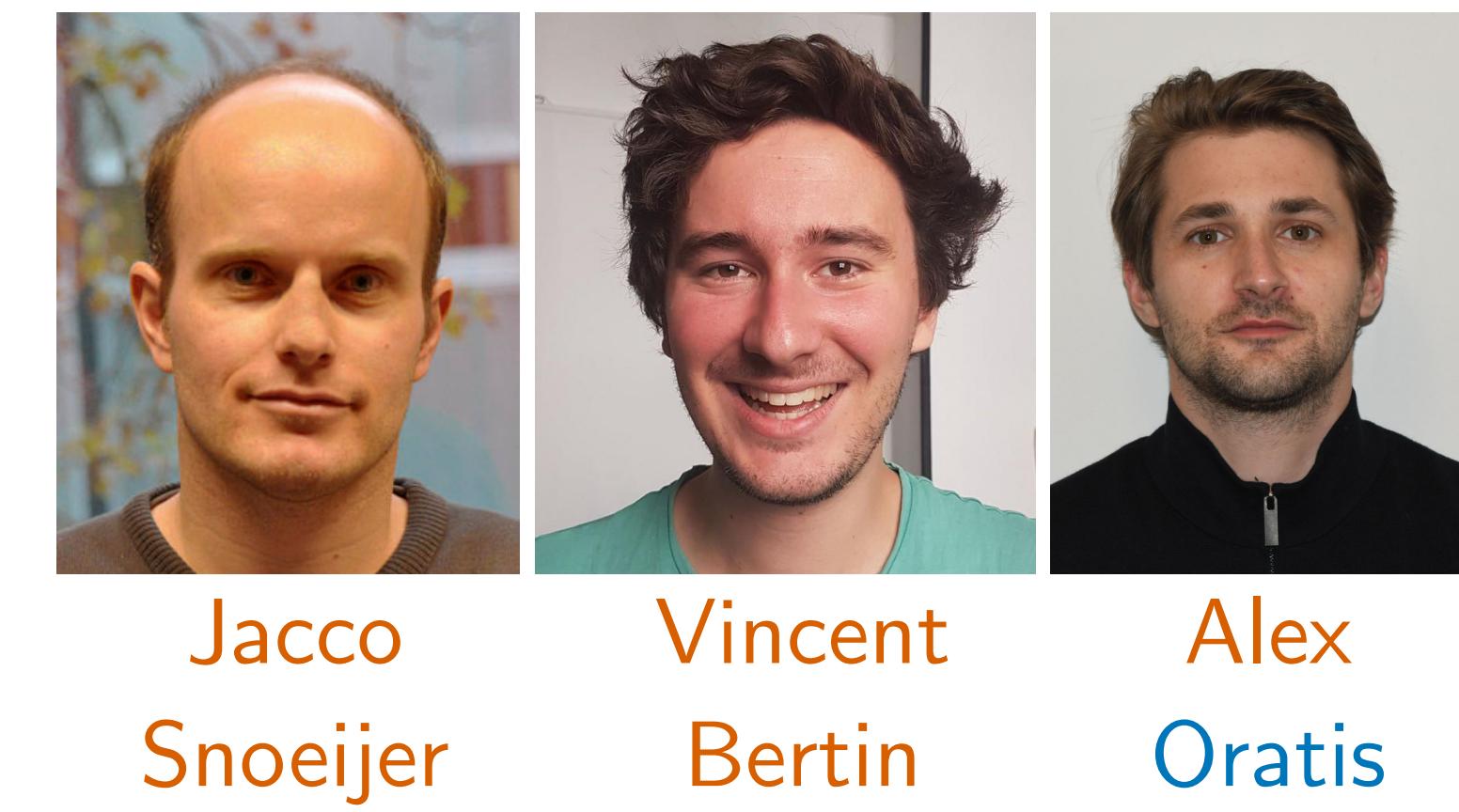
More to follow: Elastic Taylor-Culick

$t/t_\gamma = 0.00$



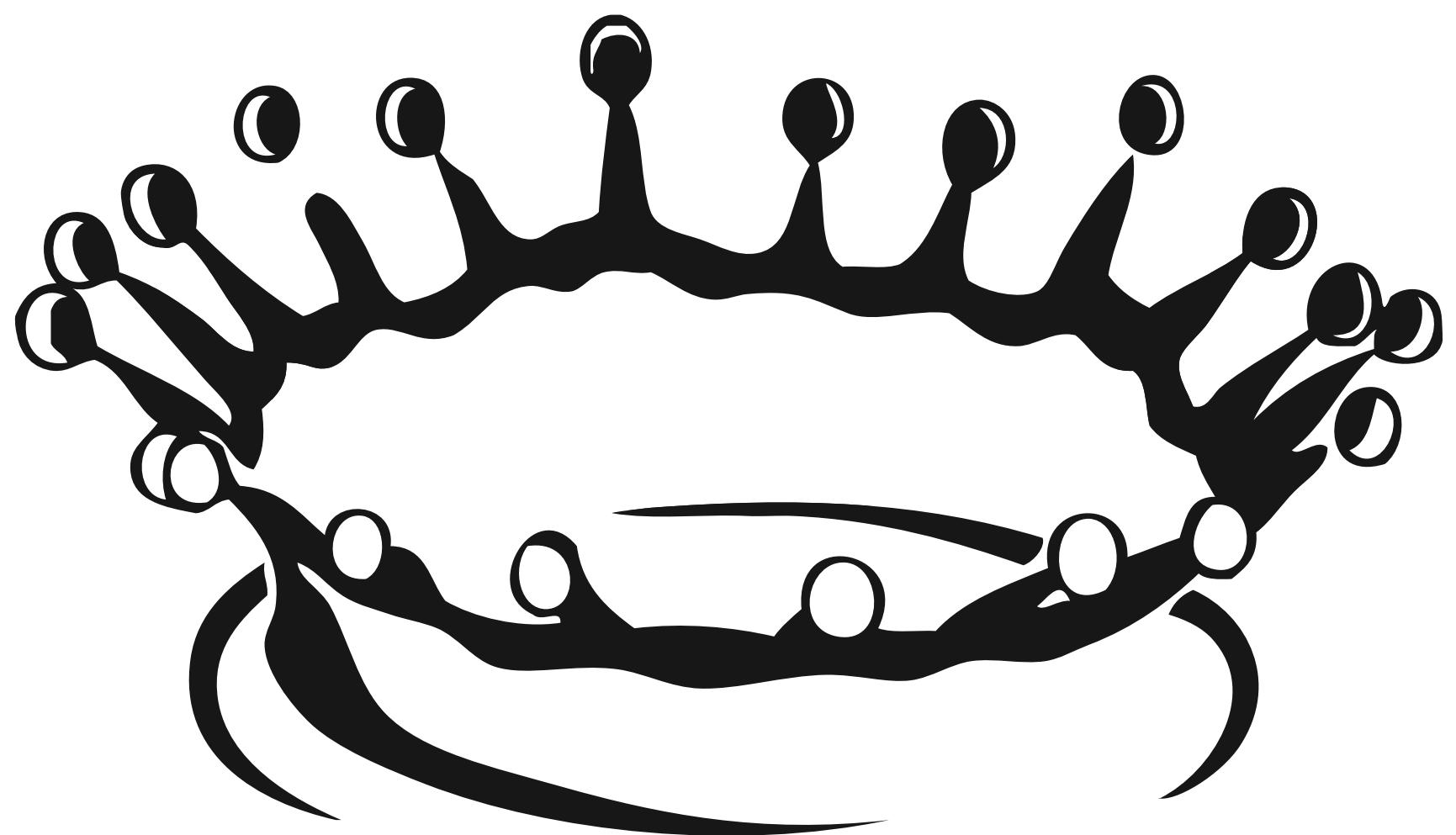
$$Ec = \frac{Gh_0}{\gamma} = 0.01$$

$$De = \lambda / \sqrt{\frac{\rho R_0^3}{\gamma}} \rightarrow \infty$$



One more thing...

Ph.D. positions across scales



Physics of Fluids



Ph.D. positions across scales



Physics of Fluids

Flow for future

Flow for Health

Flow for Climate

Flow for HighTech

Flow for Environment

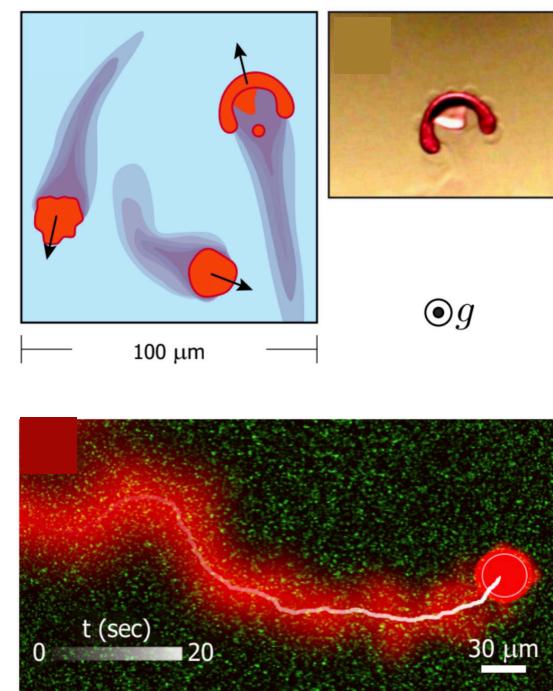
Flow for Energy Transitions

Flow for Agro & Food production

Ph.D. positions across scales

MultiMelt

Melting & Dissolution across scales



Physics of Fluids

Flow for future

Flow for Health

Flow for Climate

Flow for HighTech

Flow for Environment

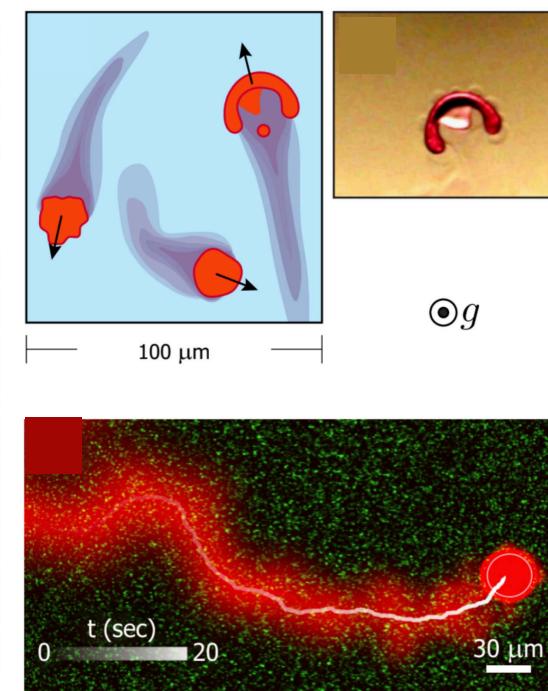
Flow for Energy Transitions

Flow for Agro & Food production

Ph.D. positions across scales

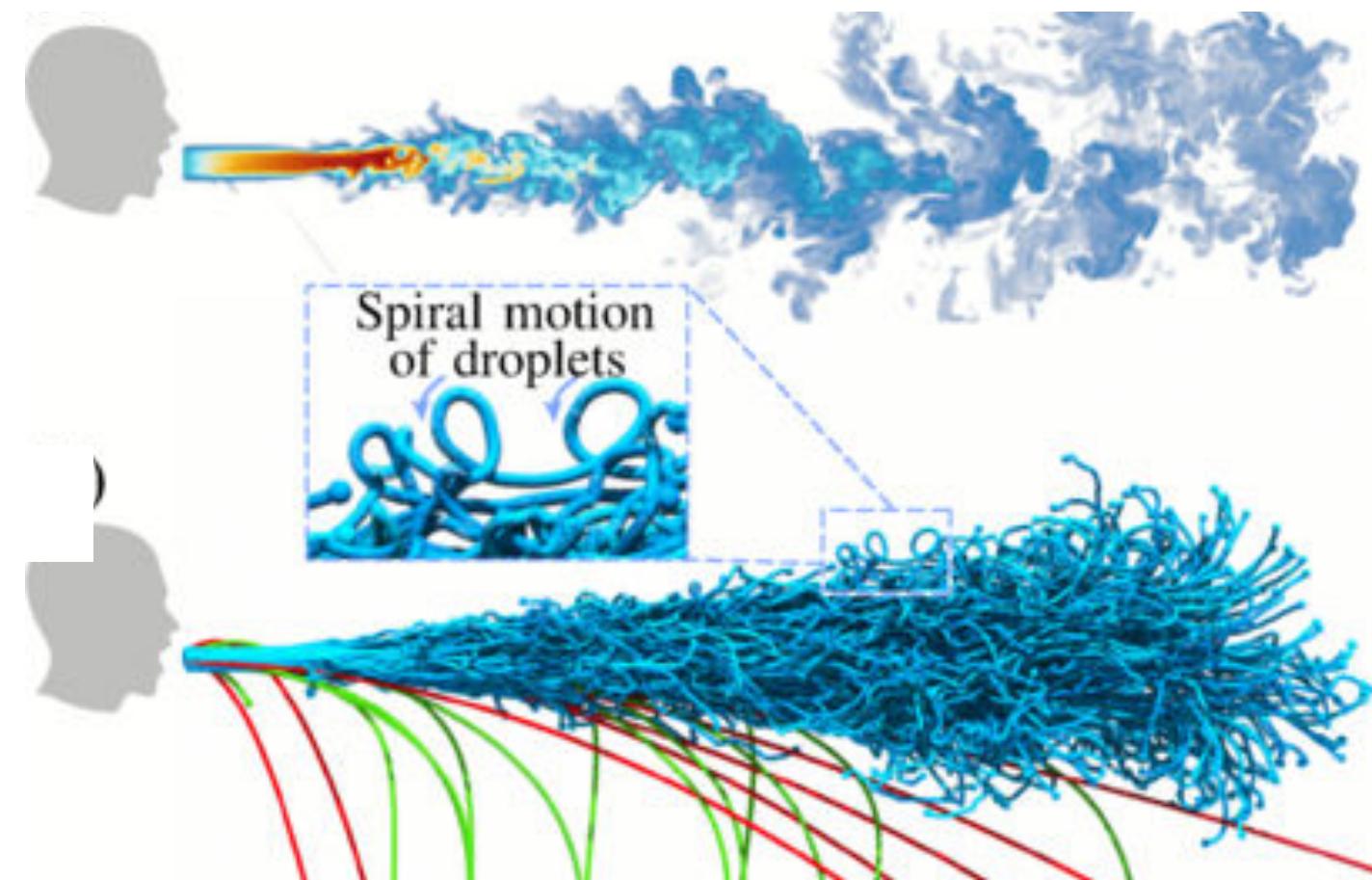
MultiMelt

Melting & Dissolution across scales



MIST

Mitigation Strategies for
Airborne Infection Control



Physics of Fluids

Flow for future

Flow for Health

Flow for Climate

Flow for HighTech

Flow for Environment

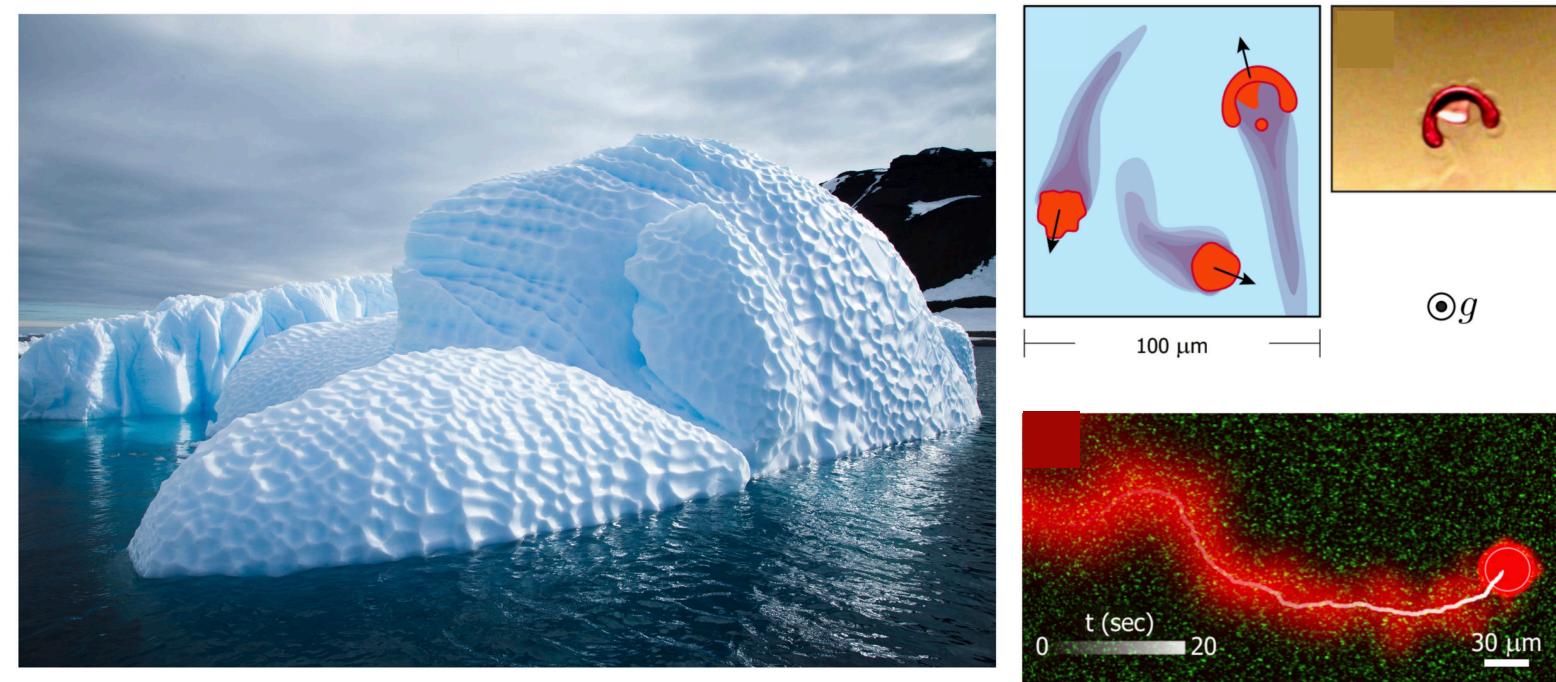
Flow for Energy Transitions

Flow for Agro & Food production

Ph.D. positions across scales

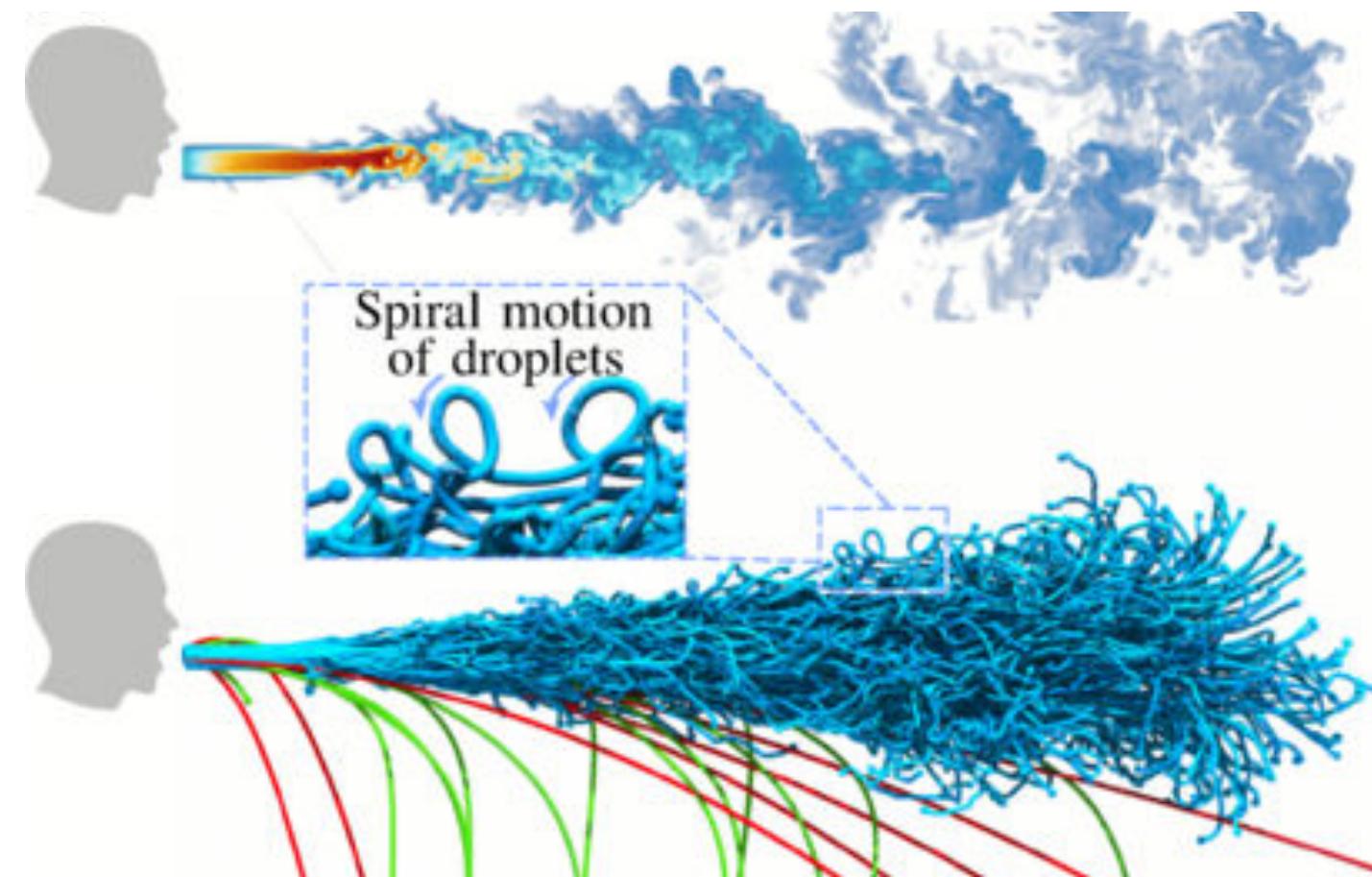
MulitMelt

Melting & Dissolution across scales



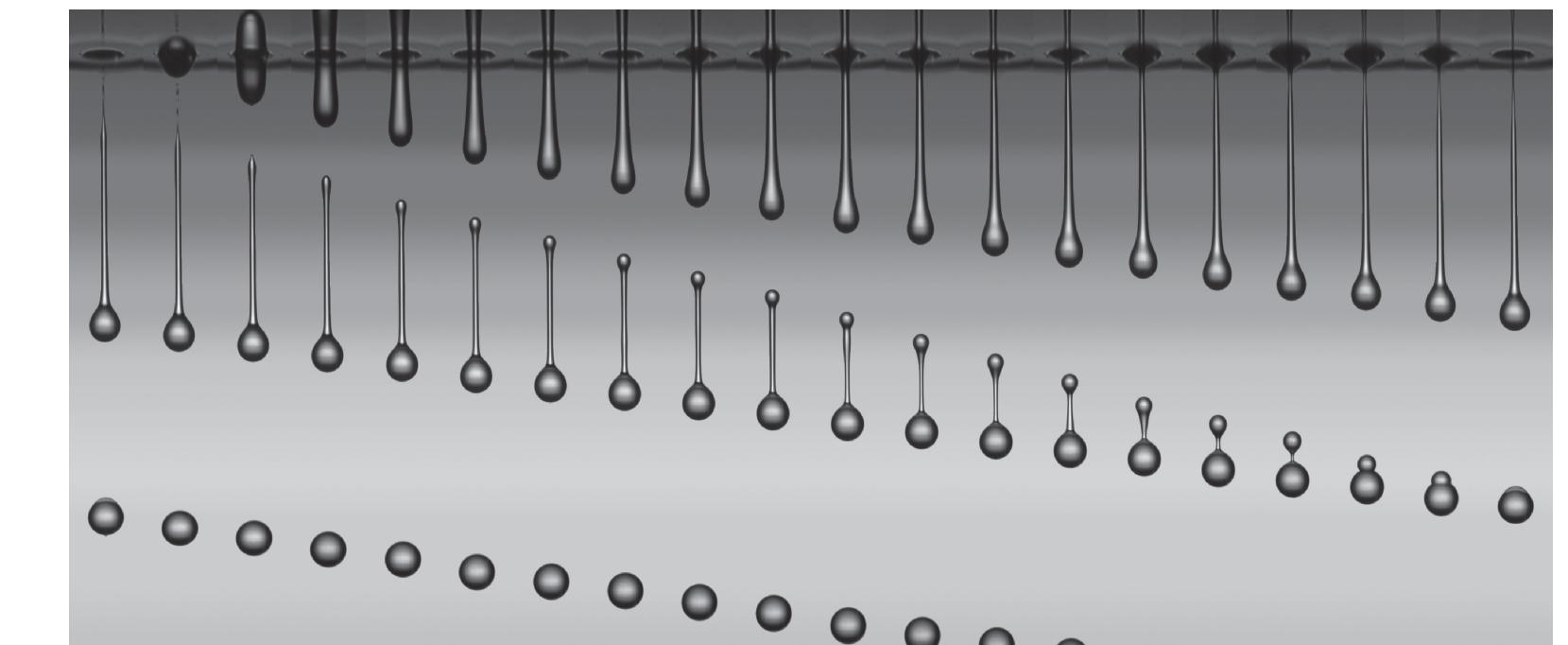
MIST

Mitigation Strategies for Airborne Infection Control



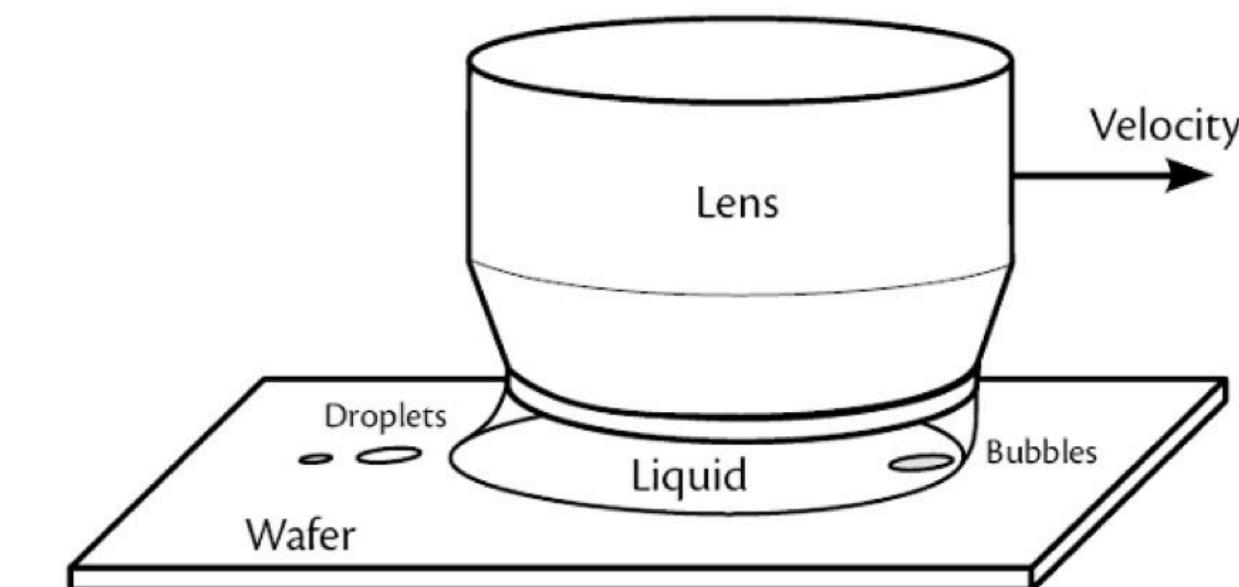
Fundamentals of Inkjet printing-II

Physicochemical Hydrodynamics of Droplets



Canon ASML

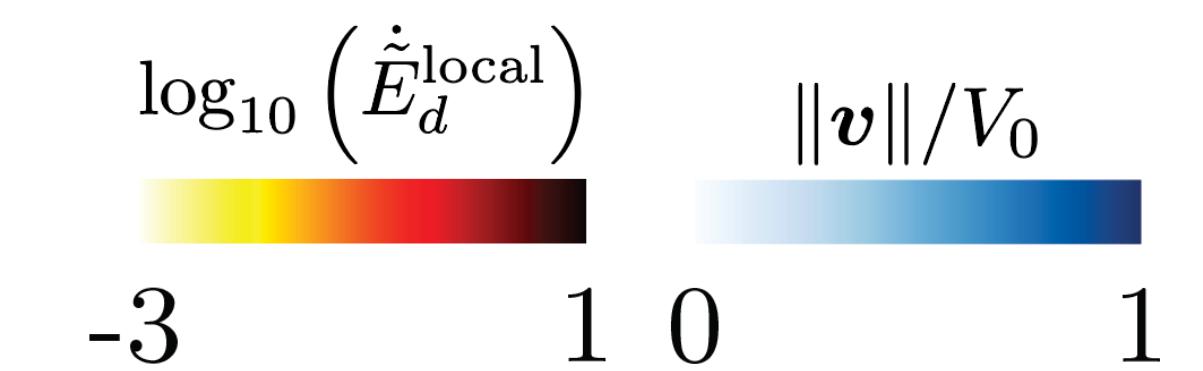
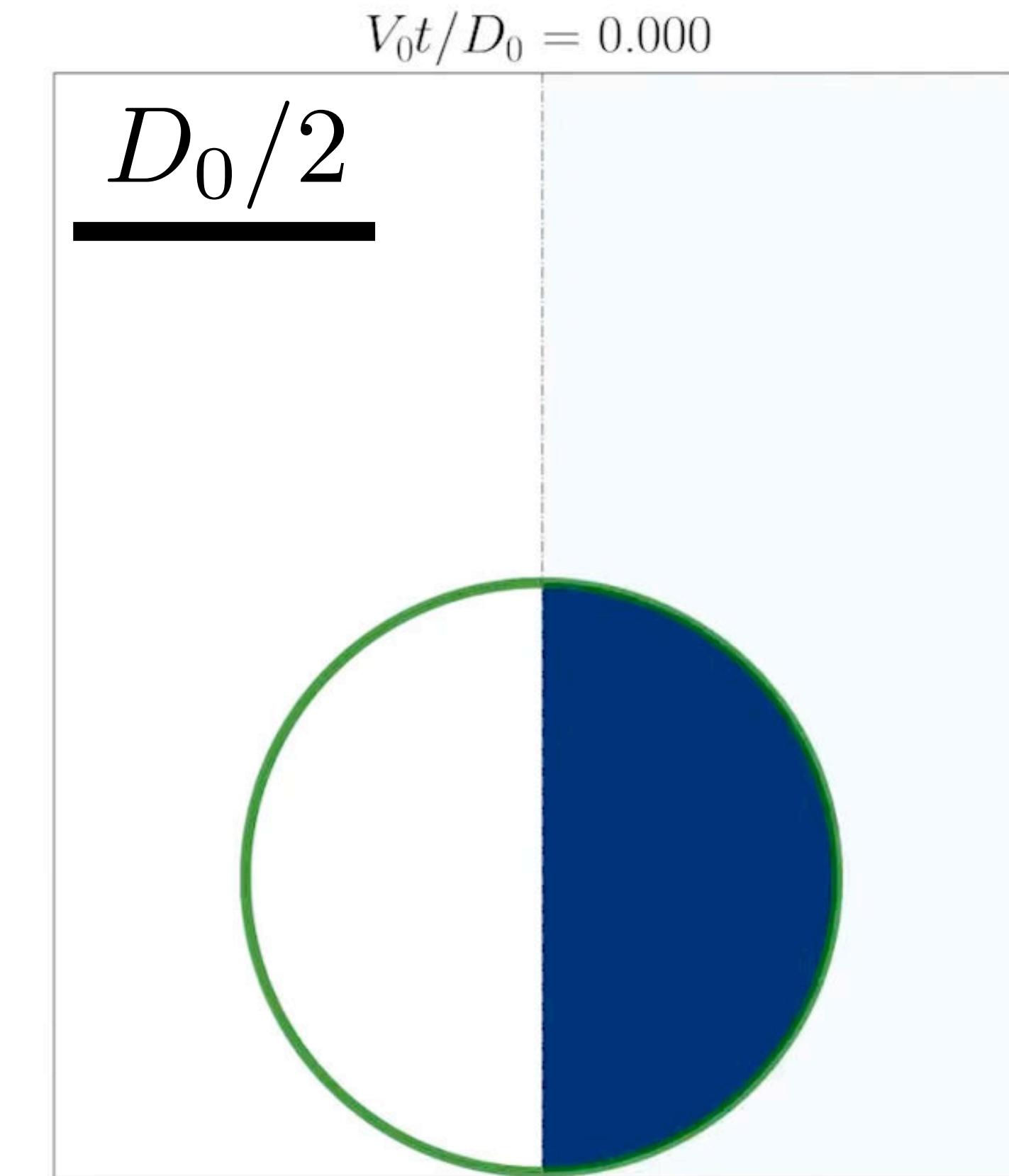
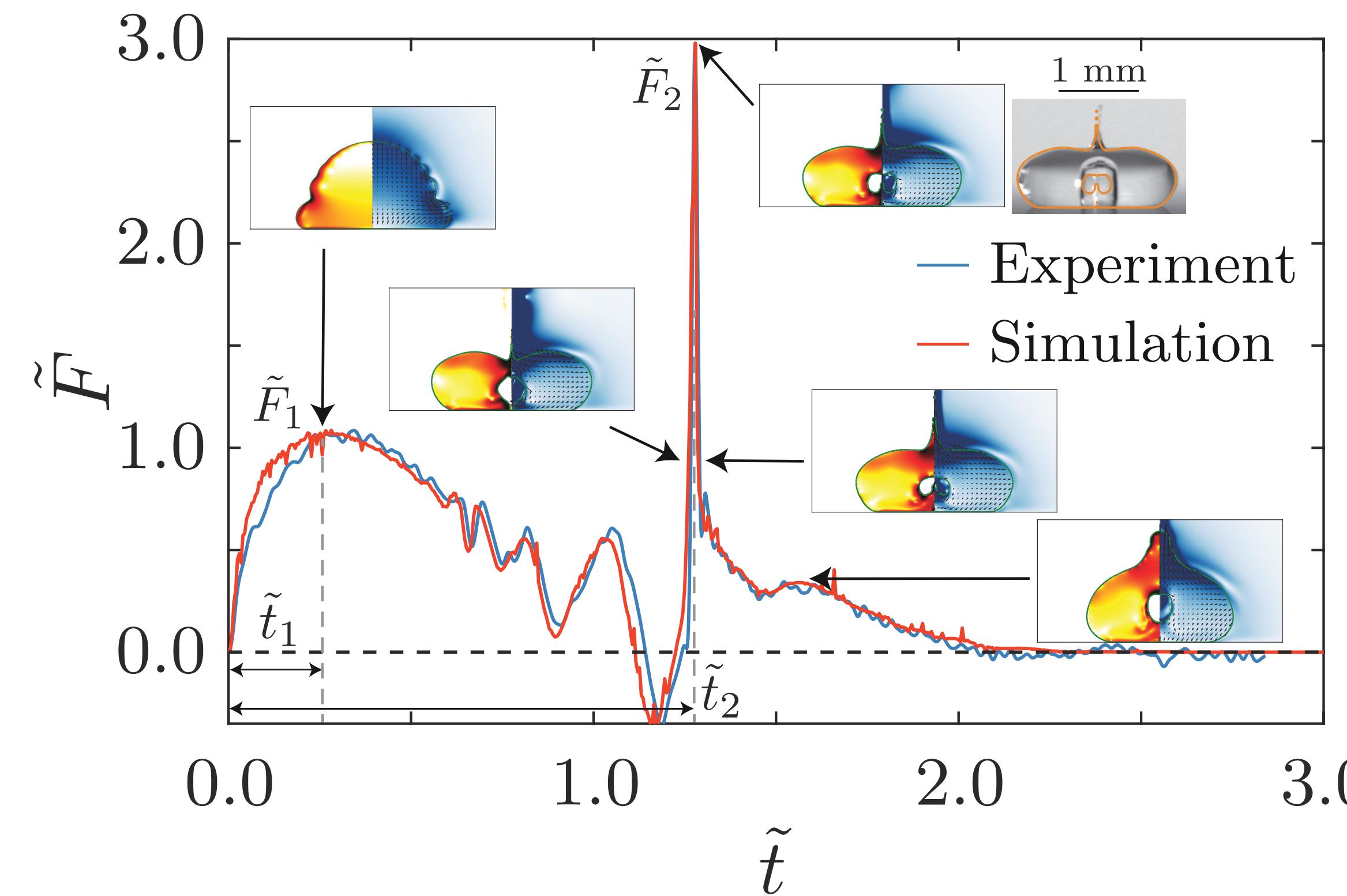
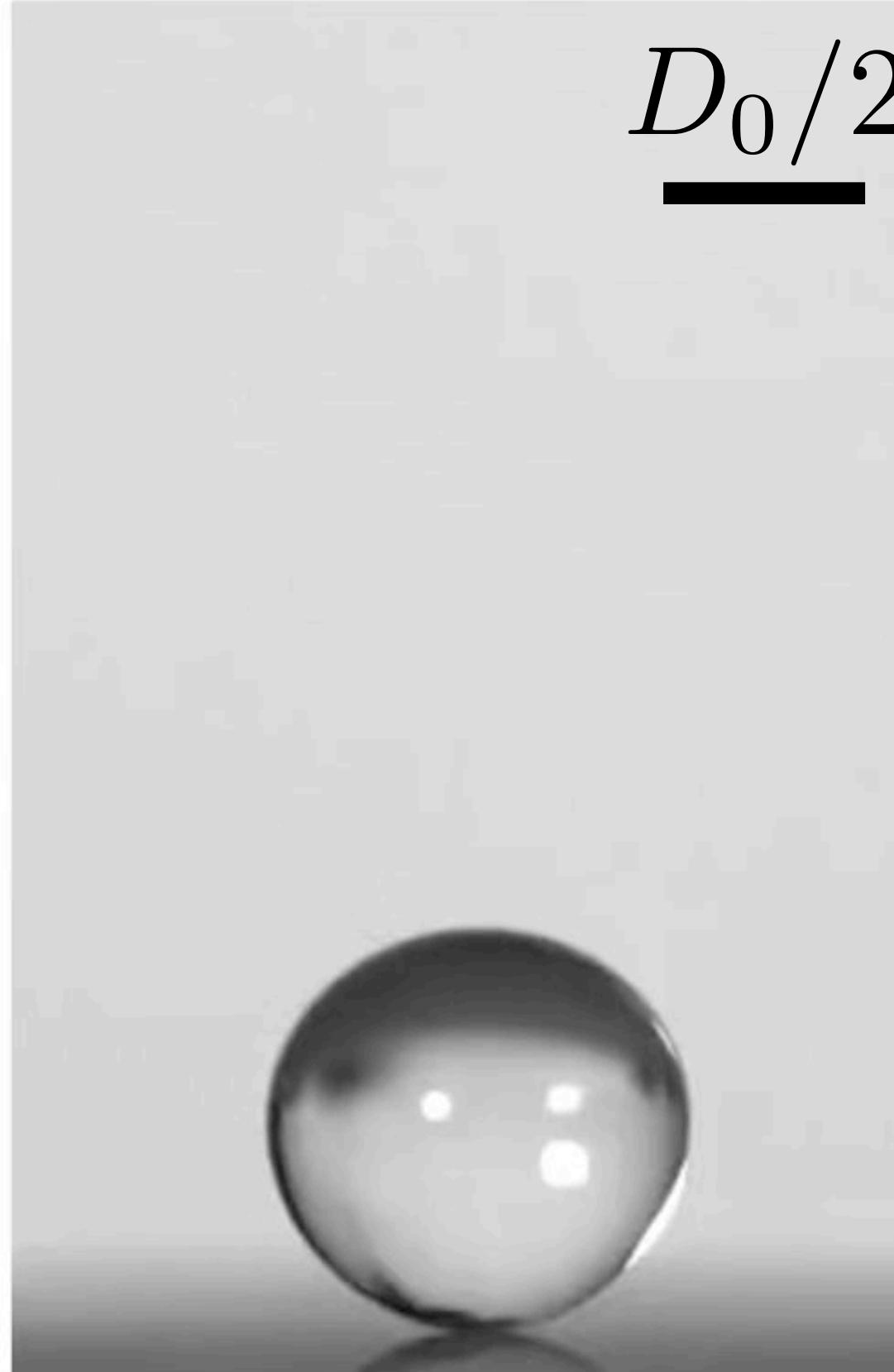
Contact lines
Inertial instability



Physics of Fluids

Flow for future

- Flow for Health
- Flow for Climate
- Flow for HighTech
- Flow for Environment
- Flow for Energy Transitions
- Flow for Agro & Food production



Thank you!

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basilisk.fr/sandbox/vatsal/

Resources



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- **Vincent Bertin**
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- Mandeep Saini*
- **Pallav Kant (Univ. of Cambridge)**
- Jonathan Pham (Univ. of Kentucky)
- Doris Vollmer (MPI-Mainz)

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Physics of Fluids



European Research Council

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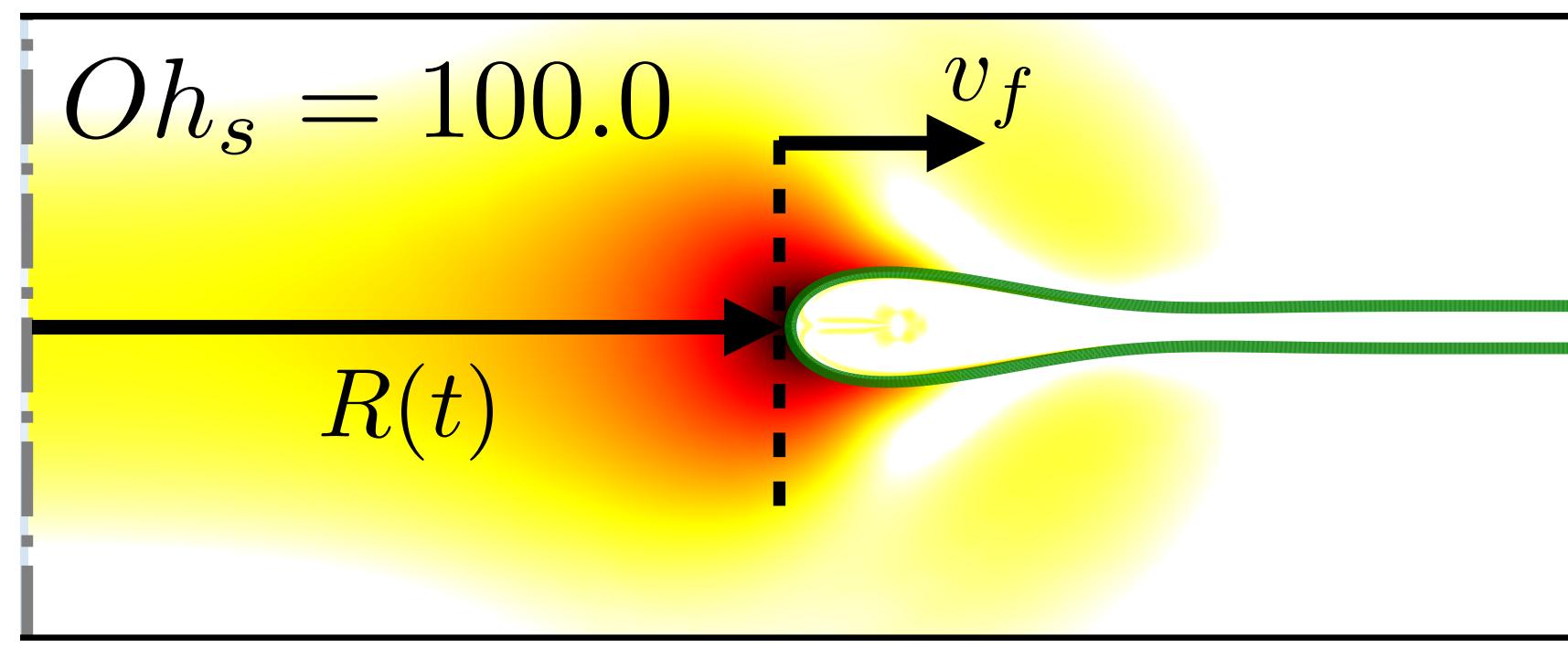


How can we understand the scaling for retraction velocity?

$$We_f \sim Oh_s^{-2}$$

Dynamics: 2 phase

Capillary force during retraction vs. Viscous resistance



$$F_\gamma \sim F_\eta$$

Stokes flow/Oseen approximation

$$2\gamma_{fs} \sim \eta_s v_f$$

$$Oh_s = \frac{\eta_s}{\sqrt{\rho_f (2\gamma_{fs}) h_0}}$$

$$Ca_s = \frac{\eta_s v_s}{2\gamma_{fs}}$$

$$We_f = \frac{\rho_f v_f^2 h_0}{2\gamma_{fs}}$$

$$Ca_s \sim Oh_s^0$$

$$v_f = v_s$$

$$We_f \sim Oh_s^{-2}$$

Fraaije and Cazabat, JCIS 133, 1989
Reddy et al., PRF 5, 2020

2-phase Taylor-Culick retraction

$$Oh_f = \frac{\eta_f}{\sqrt{\rho_f (2\gamma_{fs})} h_0} \text{ independent}$$

